# HYDROCYCLONE

\_\_\_\_/ \_\_\_ 200\_\_\_\_

Made by

Student number

#### **MARKINGS:**

Given in:	/ 200	
Examined:	/ 200	 <b>RET / PASSED</b>
	/ 200	 RET / PASSED
	/ 200	 RET / PASSED
	/ 200	 RET / PASSED
Passed:	/ 200	

## **1. GENERAL**

Thickening of a fluid with a hydrocyclone was studied in this laboratory work. Feed flow rate, pressure difference, and the solids concentration of the exiting flows was measured in this work, and the feed flow rate was the altered variable.

Only simple mass and energy balances were are used when calculating the efficiencies and energy losses.

Finally, a rough estimate for cut size of the process is calculated.

## 2. SOLIDS CONCENTRATIONS

Solids concentrations were determined by weighting the samples before and after evaporation. A summary of calculations of solids concentrations is shown on sheet 13-cycl-en.xls.Concentrations in appendix 1.

Mass fraction of solids is calculated from the measuring data as follows (experiment #\_\_\_\_\_ as an example):

 $w_F =$ 

#### **3. MASS BALANCE**

The following calculations are done by using experiment #\_\_\_\_\_ as an example.

The volume flow rate of the feed was measured and it is converted to mass flow rate:

 $\mathbf{F} =$ 

Now, the unknown mass flows O and U can be calculated:

O =

U =

A summary of the calculations is shown on sheet 13-cycl-en.xls.Balance-and-Eff in appendix 2.

## 4. SEPARATION EFFICIENCIES

The following calculations are done by using experiment #\_\_\_\_\_ as an example.

Hydrocyclone, with which given slurry is handled, can be controlled only by controlling the flow rate. So, the results of the calculations are given as a function of either flow velocity or flow rate.

Diameter of the inlet pipe is  $D_i =$ 

Then the velocity of feed flow is:

 $u_i =$ 

Diameter of the piping system is D =

So, the flow rate in the piping system is:

u =

Separation efficiency can be calculated in many ways from the flow rates and concentrations. A summary of calculations is shown on sheet 13-cycl-en.xls.Balance-and-Eff in appendix 2.

In appendix \_\_\_\_\_ is shown  $E_1 = w_0$ , in appendix \_\_\_\_\_ is shown  $E_2 = w_U$ , and in appendix \_\_\_\_\_

is shown  $E_7 = O/U$  as a function of \_\_\_\_\_\_.

Also, in appendix \_\_\_\_\_\_ is shown \_\_\_\_\_, which with the previous describes the best the change of

separation efficiency as a function of \_\_\_\_\_\_.

# **5. CUT SIZE**

The following calculations are done by using experiment #\_\_\_\_\_ as an example.

# **5.1 RESIDENCE TIME**

The cross-sectional area of the flow **is assumed** to be an annulus constrained by diameters D and  $D_o$  and the distance which the fluid flows in the cyclone, is the length L of the cyclone.

The cross-sectional area of the flow is

 $A_{\rm A} =$ 

The axial velocity is

 $u_{\rm A} =$ 

Then the residence time of the fluid in the cyclone is:

 $\tau =$ 

# 5.2 SINKING TIME OF A PARTICLE THROUGH THE WHOLE FLOW LAYER

The depth of the whole flow layer is:

S =

The sinking speed of a particle, which diameter is  $d_p = \_$  m, obtained from the Stokes law is:

 $u_p =$ 

Sinking time of the particle through the whole flow layer is:

 $t_n =$ 

Since the sinking time of the particle is greater/smaller than the residence time of the fluid in the cyclone, the particle has time/does not have time to sink through the whole layer.

#### 5.3 SINKING SPEED OF CUT SIZE

Next, the cut size  $d_{50}$  is considered. If a particle has time to sink 50 % of the depth of the flow layer during the residence time  $\tau$ , it has a 50 % probability to end up in the underflow. In such case, the velocity of the particle has to be:

 $u_{\rm p} =$ 

# 5.4 CUT SIZE

Normal acceleration based on the inlet velocity in the top of the hydrocyclone is

a =

Assuming that particle sinks with a constant speed obtained from the Stokes law, can the cut size  $d_{50}$  be calculated as follows:

 $d_{50} =$ 

A summary of the cut size calculations is shown on sheet 13-cyclo-en.xls.Cut-size in appendix 3. In appendix \_\_\_\_\_ are shown cut sizes  $d_1$ ,  $d_{50}$ , and  $d_{100}$  as a function of \_\_\_\_\_.

#### 6. ENERGY LOSSES

The following calculations are done by using experiment #\_\_\_\_\_ as an example.

#### **6.1 LOSSES IN CYCLONE**

Loss of mechanical energy in the cyclone is (assumed that flow is turbulent, so  $\alpha=1$ ):

 $P_{\rm h} =$ 

#### 6.2 LOSSES IN PIPING SYSTEM

Flow velocity in the piping is u = Reynolds number (for water) Re = Friction factor inside pipe (smooth pipe)  $\xi$ = Length of piping system L = Diameter of piping system D = Sum of friction factors due to fittings and valves  $\sum \zeta_i$  = Loss of mechanical energy in the piping system is:

 $P_{\rm h} =$ 

#### **6.3 LOSSES IN PUMP**

Electrical power of motor of the pump  $P_{\rm E}$  = Efficiency of the motor  $\eta_{\rm E}$  = Brake power  $P_{\rm B}$  = Mechanical efficiency  $\eta_{\rm P}$  = Loss of mechanical energy in the pump is  $P_{\rm h}$  =

#### 6.4 TOTAL LOSSES AND TEMPERATURE RISE

Total rate of loss of mechanical energy in the system is:

#### $P_{\rm h} =$

Generation power of heat energy is:

 $P_{\rm H,GEN} =$ 

 $\frac{dT}{dt} =$ 

Due to this temperature rise rate, the temperature of the system would increase

 $\Delta T =$ 

in 10 minutes.

A summary of losses and temperature rise is on sheet 13-cycl-en.xls.Losses is shown in appendix 4.

# 7. INCORRECT ESTIMATE AND CONCLUSIONS

# 8. APPENDICES