



Aalto University  
School of Chemical  
Engineering

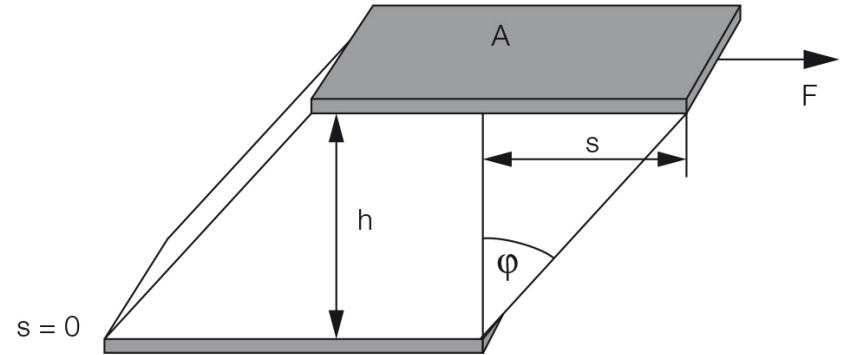
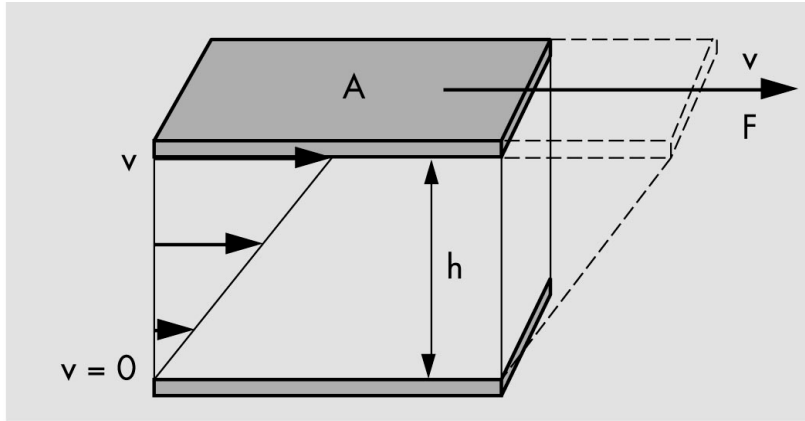
# Rheology of cellulose solutions

*Theory and Practice of Wet Spinning of Cellulose  
Solutions*

# Fundamentals

- Anton Paar, Basics of Rheology. Course number: IARBA001
- Gebhard Schramm, A practical approach to rheology and rheometry, Gebrueder Haake GmbH, Karlsruhe (ASIN: B000BWY1WA)
- Thomas G. Mezger, Applied Rheology – With Joe Flow on Rheology Road (ISBN: 978-3-9504016-0-8)

# Steady shear tests



h ... plate distance  
A ... area of upper plate  
F ... force displacing upper plate sideways  
v ... velocity of upper plate (bottom one is fixed)

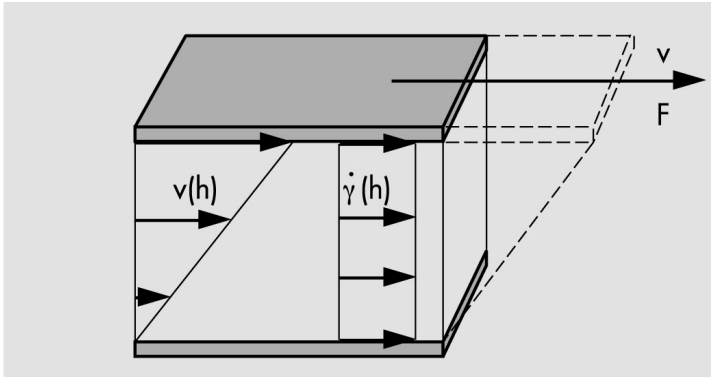
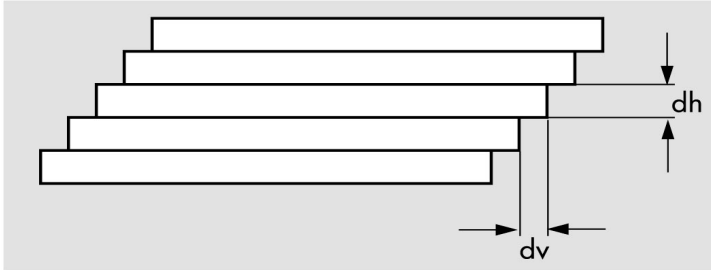
s ... deflection path  
 $\varphi$  ... deflection angle

$$\text{Shear stress: } \tau = F/A \text{ [Pa]}$$

$$\text{Shear strain: } \gamma = s/h$$

**A!**

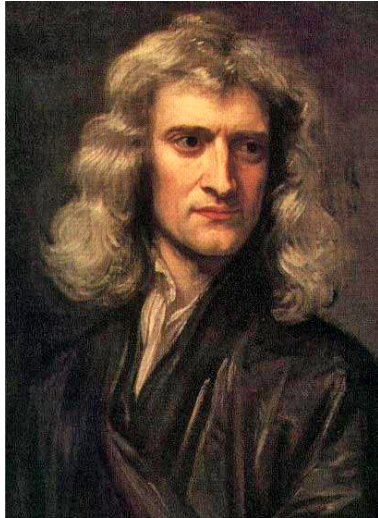
# Steady shear tests



$$\text{Shear rate: } \dot{\gamma} = \frac{dv}{dh} \quad [\text{s}^{-1}]$$

$$\dot{\gamma} = \frac{d\gamma}{dt} = \frac{ds/dh}{dt} = \frac{ds/dt}{dh} = \frac{dv}{dh}$$

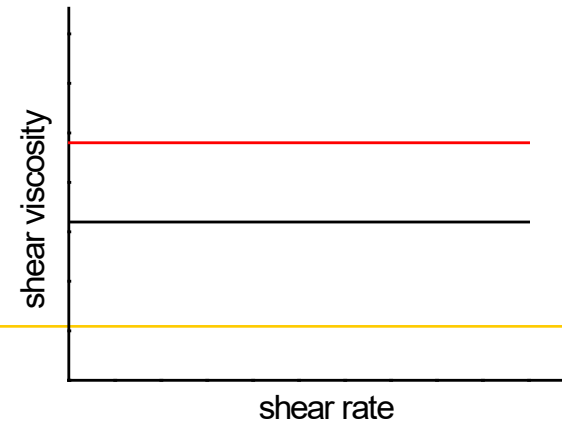
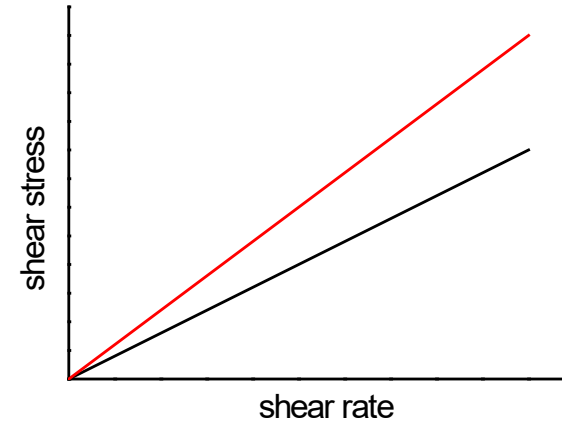
# Newton's law



Isaac Newton (1642 to 1727); he writes about the flow resistance of fluids (e.g. of air and water).

However, this later so-called “Viscosity Law of Newton” was formulated not before the 19 century (e.g. by G.G. Stokes in 1845).

$$\tau = \eta * \dot{\gamma}$$

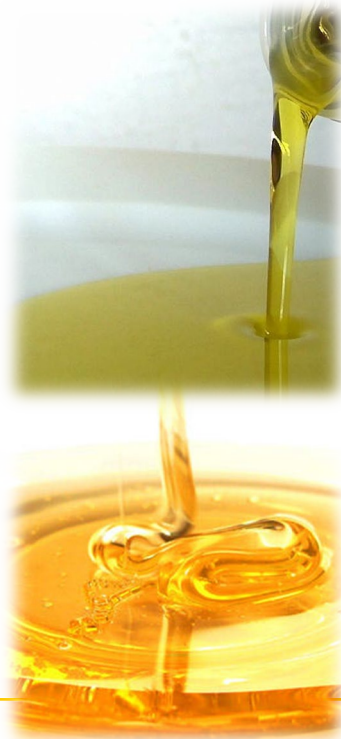


# Viscosity values

$$\tau = \eta * \dot{\gamma}$$

SI-unit: [Pa s]

old unit: "poise" [P]



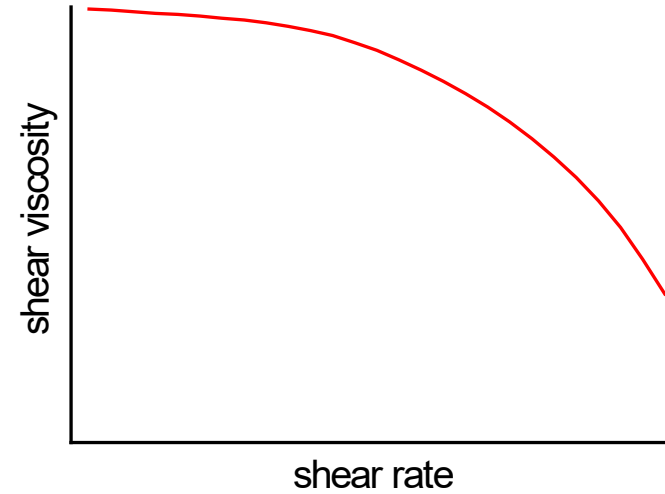
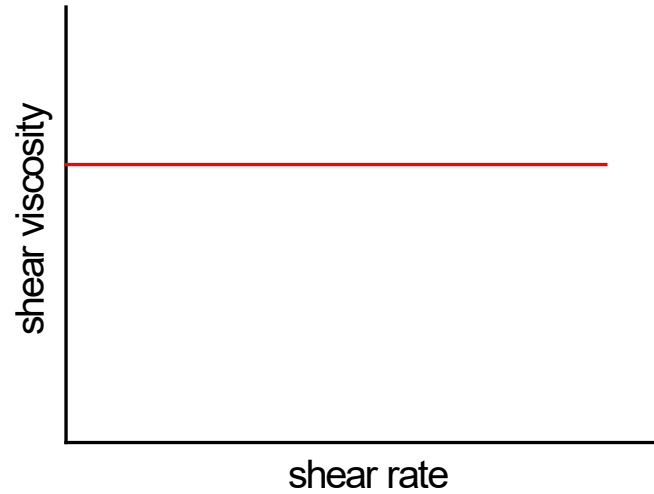
viscosity = flow resistance of fluids in motion

Material	Shear viscosity $\eta$ / mPas (20 °C)
air	0.018
water	1.00
ethanol	1.20
olive oil	100
motor oils	50-1000
honey	10000

# Typical shear rate ranges

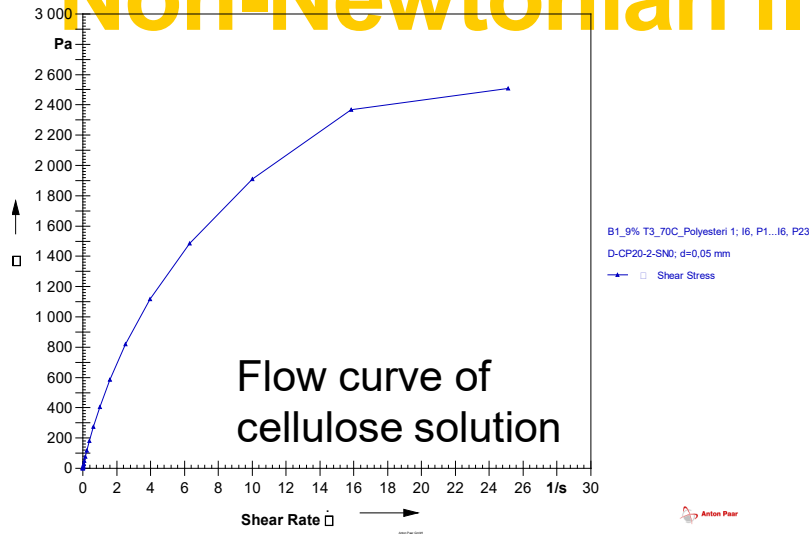
Process	Shear rates (s <sup>-1</sup> )
Sedimentation	< 0.001 to 0.01
Surface leveling	0.01 to 0.1
Sagging	0.01 to 1
Dip coating	1 to 100
Pipe flow, pumping, filling into containers	10 to 10,000
Mixing, stirring	10 to 10,000
Spinning	10 to 10,000
Coating, painting, brushing	100 to 10,000
Spraying	1000 to 10,000
(High-speed) coating, blade coating	100,000 to 1 mio.

# Non-Newtonian fluid

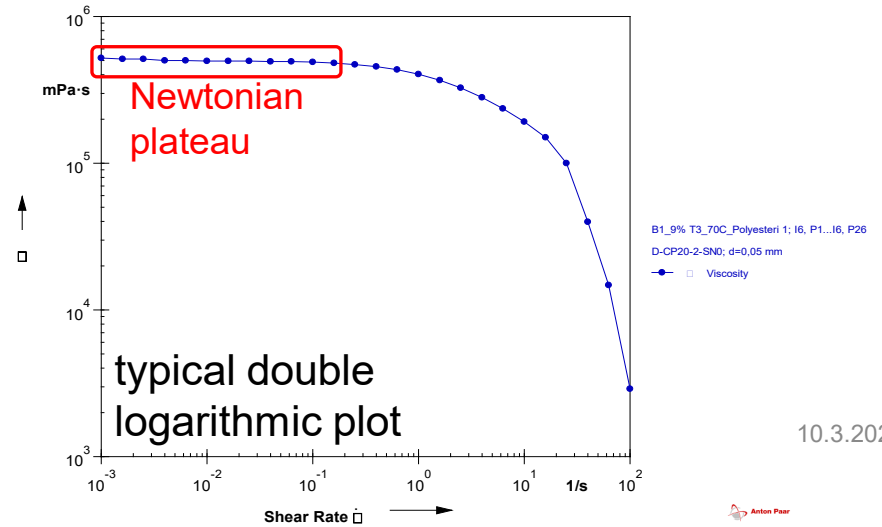
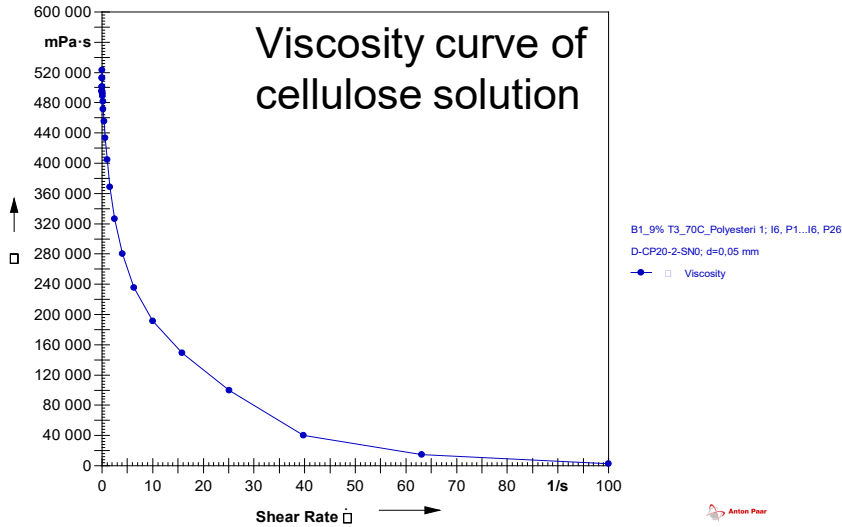




# Non-Newtonian fluid

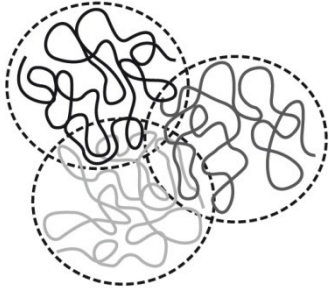


Polymer melts or solutions show reduced viscosity at high shear rates. This phenomenon is called *shear thinning*



# Non-Newtonian fluid

## 1. Liquids at rest

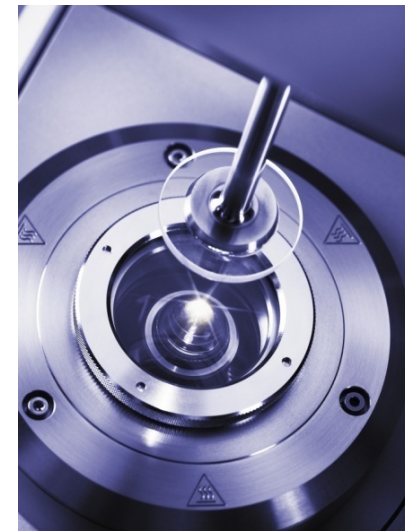
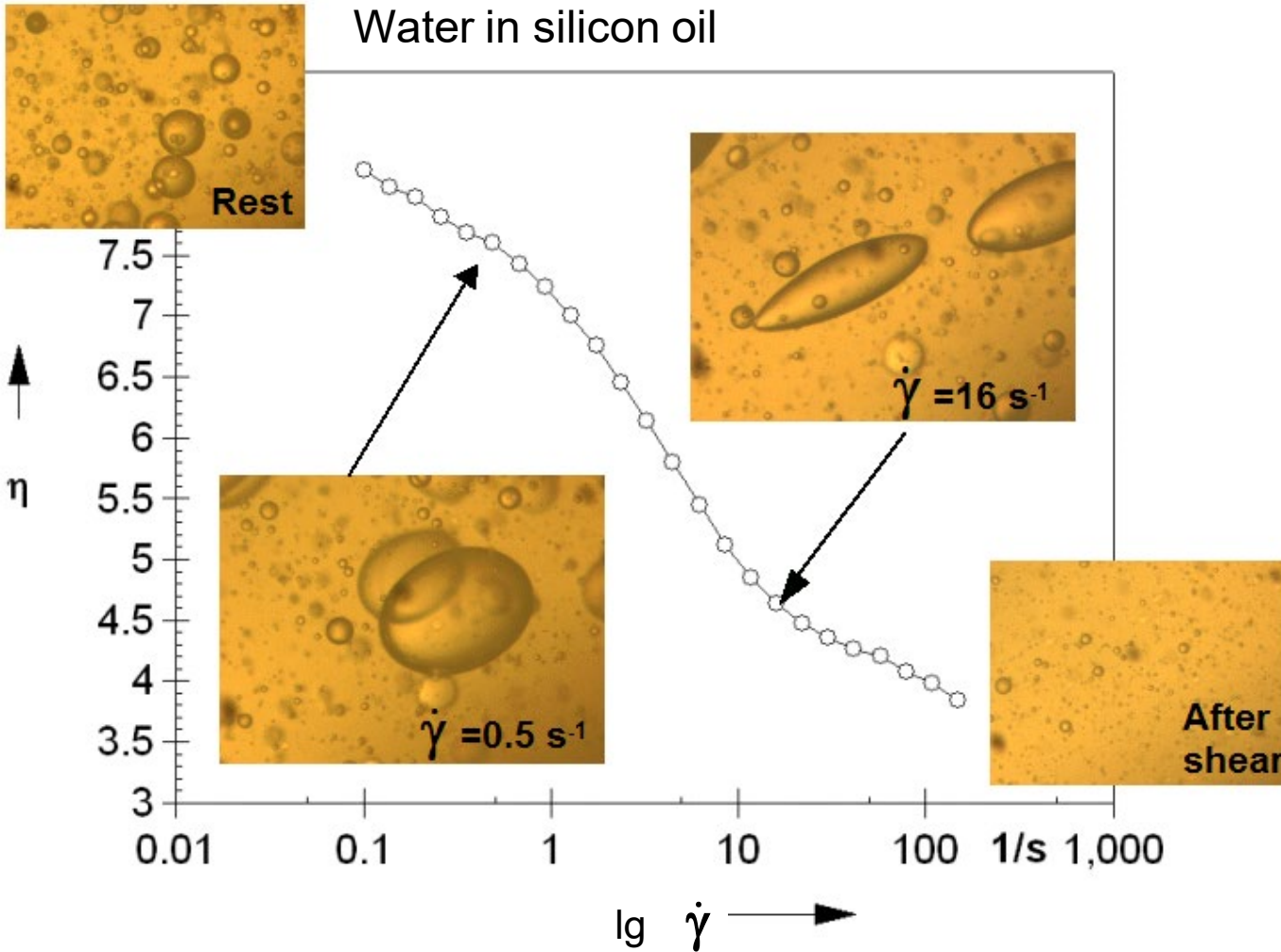


## 2. Liquids flowing in the direction of the arrows

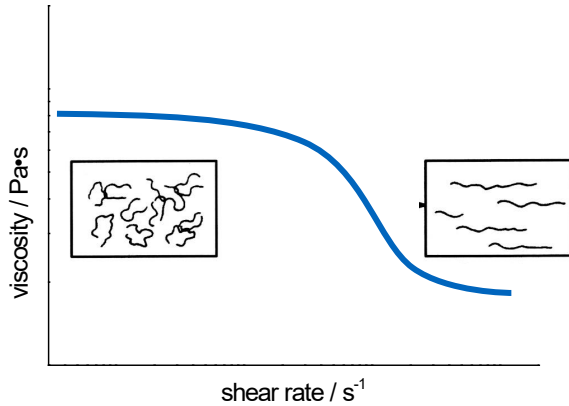


stretching

# Non-Newtonian fluid



# Zero shear viscosity $\eta_0$



The viscosity of polymer solutions and melts is dependent on the shear rate. Extrapolation of the viscosity curve to  $\dot{\gamma} = 0$  affords the so called *zero shear viscosity*  $\eta_0$

Suitable model functions for concentrated polymer solutions and melts to determine  $\eta_0$ :

$$\eta(\dot{\gamma}) = \frac{\eta_0}{1 + (c * \dot{\gamma})^p}$$

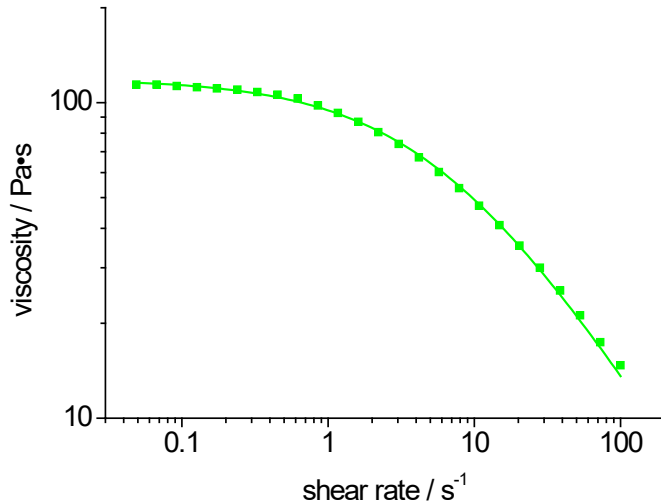
Cross

$$\eta(\dot{\gamma}) = (c * \dot{\gamma})^p$$

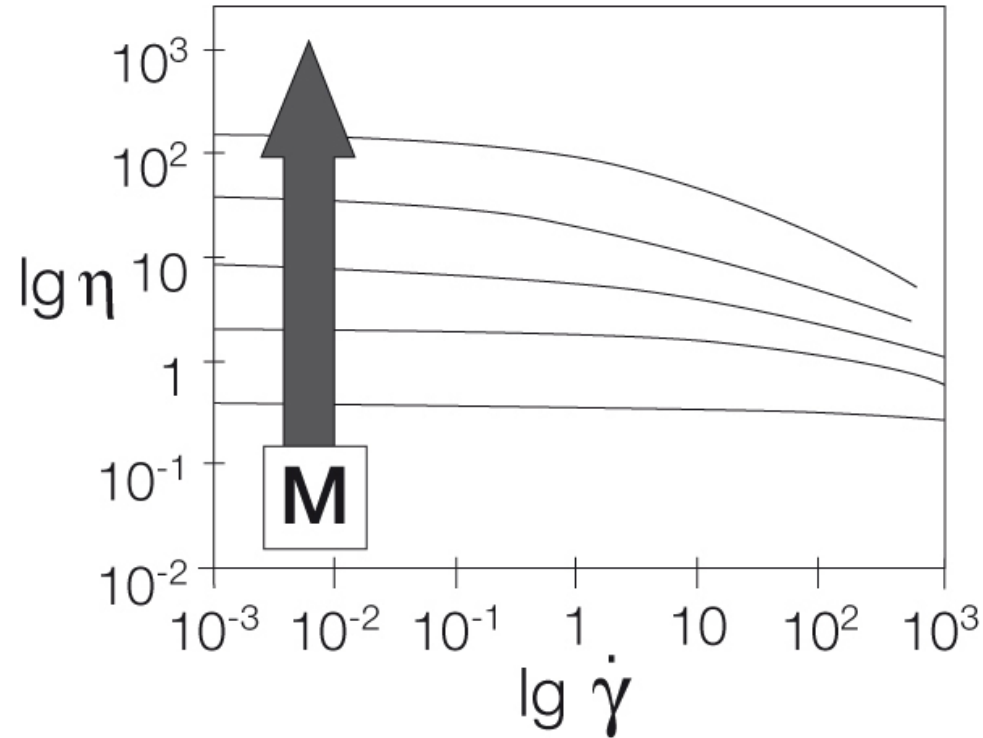
Power law (for  $\eta(\dot{\gamma}) \ll \eta_0$ )

$$\eta(\dot{\gamma}) = \frac{\eta_0}{(1 + (c * \dot{\gamma})^{p_1})^p}$$

Carreau/Gahleitner



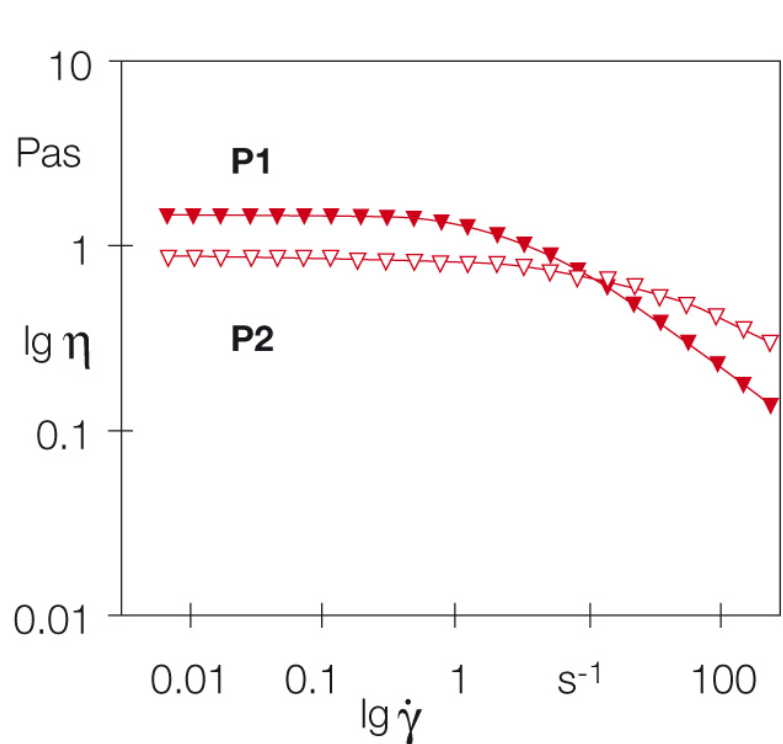
# Polymer solution



## For solutions containing unlinked polymers

An increasing average molar mass  $M$  results in a higher zero shear viscosity value (for a constant polymer concentration)

# Polymer solution



## Polymer solutions

Unlinked polymers and zero shear viscosity

**P1:** narrower MMD, with a steeper decrease of the curve

**P2:** wider MMD

# Non-Newtonian behaviors

Phenomenon*	Description
Shear thinning	Viscosity decrease upon shear rate increase
Shear thickening	Viscosity increase upon shear rate increase
Thixotropic behavior	<b>Time dependent</b> viscosity decrease upon constant shear load
Rheopectic behavior	<b>Time dependent</b> viscosity increase upon constant shear load

\*these terms are only applicable if the solute (molecules) are not degraded, i.e. the fluid displays the initial viscosity level after a certain rest phase.

# Shear test – Continuous rotation

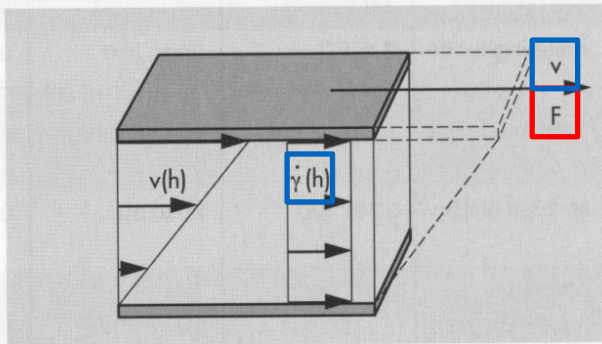
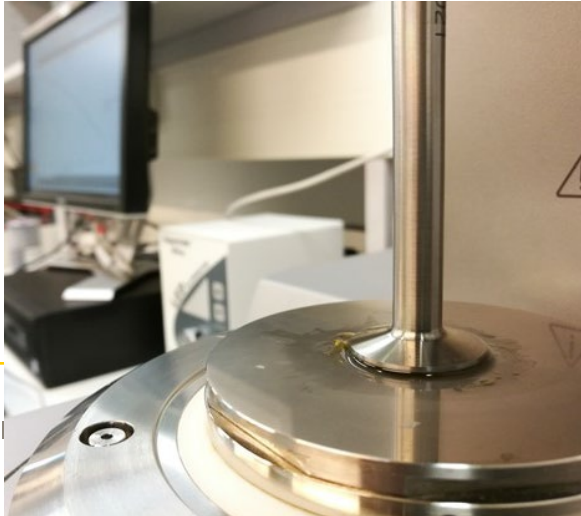


Figure 2.3: Velocity distribution and shear rate in the shear gap of a Two-Plates-Model

**Controlled shear rate (CSR):**  
Shear rate (velocity) is set and controlled and shear stress is measured

**Controlled shear stress (CSS):**  
Shear stress is set and controlled and shear rate is measured





# Shear test – Continuous rotation

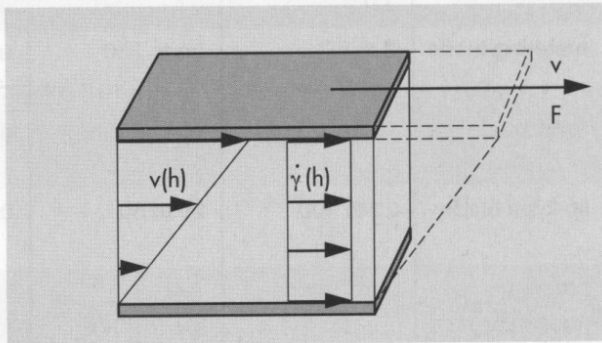


Figure 2.3: Velocity distribution and shear rate in the shear gap of a Two-Plates-Model

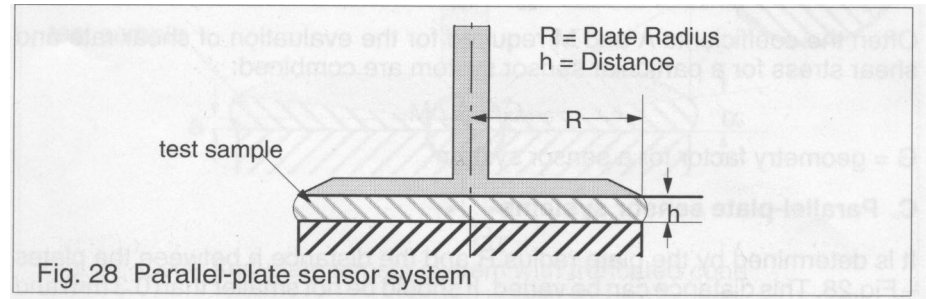
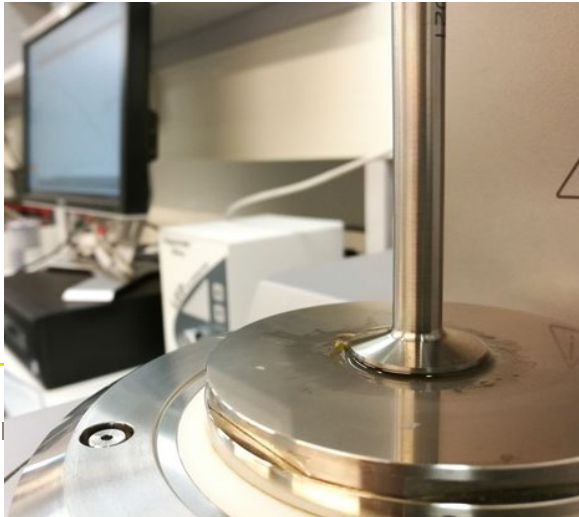


Fig. 28 Parallel-plate sensor system

$$\tau = \frac{2}{\pi R^2} M = C_1 \mathbf{M} \quad \text{M...torque [Nm]}$$

$$\dot{\gamma} = \frac{v}{h} = \frac{\omega R}{h} = \frac{2\pi R}{60h} n = C_2 n$$

$$\eta = \frac{\tau}{\dot{\gamma}} = \frac{2\mathbf{M}h}{\pi R^4 \omega}$$

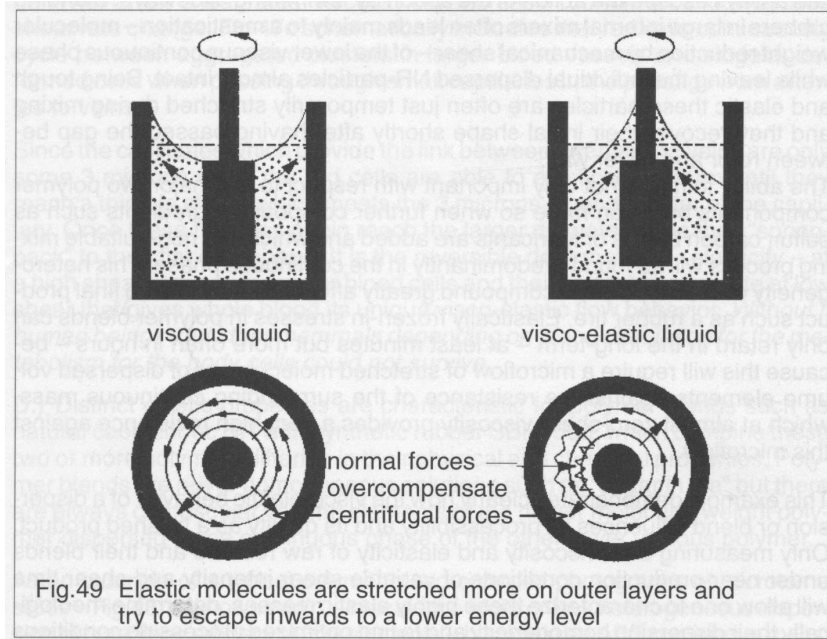


$\omega$ ...angular frequency [rad s<sup>-1</sup>]  
 $n$ ...rotational speed [min<sup>-1</sup>]

# Shear test



# Weissenberg effect



Rotational velocity increases with the radius ( $v = \omega r$ ). Hence, polymer chains are subjected to higher shear stress at the outer layers. To "escape" this stress they try to move inwards and, subsequently, upwards. This generate a "normal (perpendicular) stress"

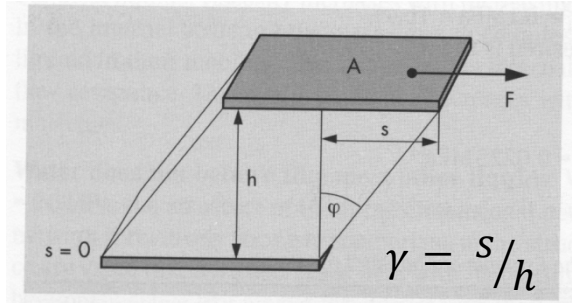
# Weissenberg effect



# Visco-elasticity



# Elastic behavior and shear modulus

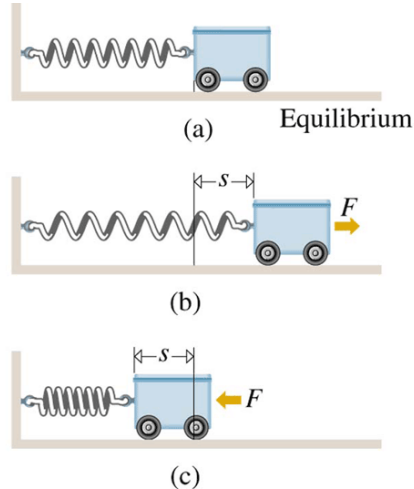


within the linear-elastic range

$$\tau = G * \gamma$$

$G$ ... shear modulus [Pa]

Hooke's law:



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within the Hookean range

$$F = -k * s$$

$k$ ... spring constant [N m<sup>-1</sup>]



Robert Hooke (1635 to 1703); in 1676 he describes **for solids proportionality of force and deformation.**

However, the laterly so-called “**Elasticity Law of Hooke**” was formulated not before the 19. century (e.g. by T. Young in 1807, or A.L. Cauchy in 1827).

# Elastic behavior and shear modulus



Material	Shear modulus $G / \text{Pa}$ (20 °C)
salad dressing	$\approx 10$
cosmetics	$\approx 500$
puddings	$\approx 5\,000$
gummi bears	$\approx 100\,000$
PE-LD	$\approx 100\,000\,000$
PE-HD	$\approx 500\,000\,000$
window glass	$\approx 30\,000\,000\,000$
steel	$\approx 80\,000\,000\,000$

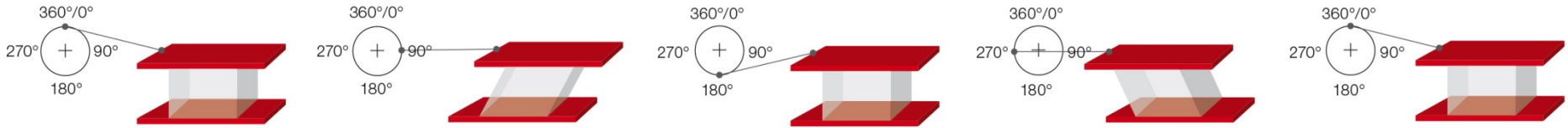
# Elastic behavior and shear modulus

Cheese type	Example	Shear modulus (around)
1 cream	Philadelphia	1 kPa
2 soft	French Camembert	10 kPa
3 semi-hard	Holland Gouda (young)	0.1 MPa
4 hard	Swiss Emmentaler	0.5 MPa
5 extra hard	Italian Parmigiano	1 MPa





# Oscillatory tests

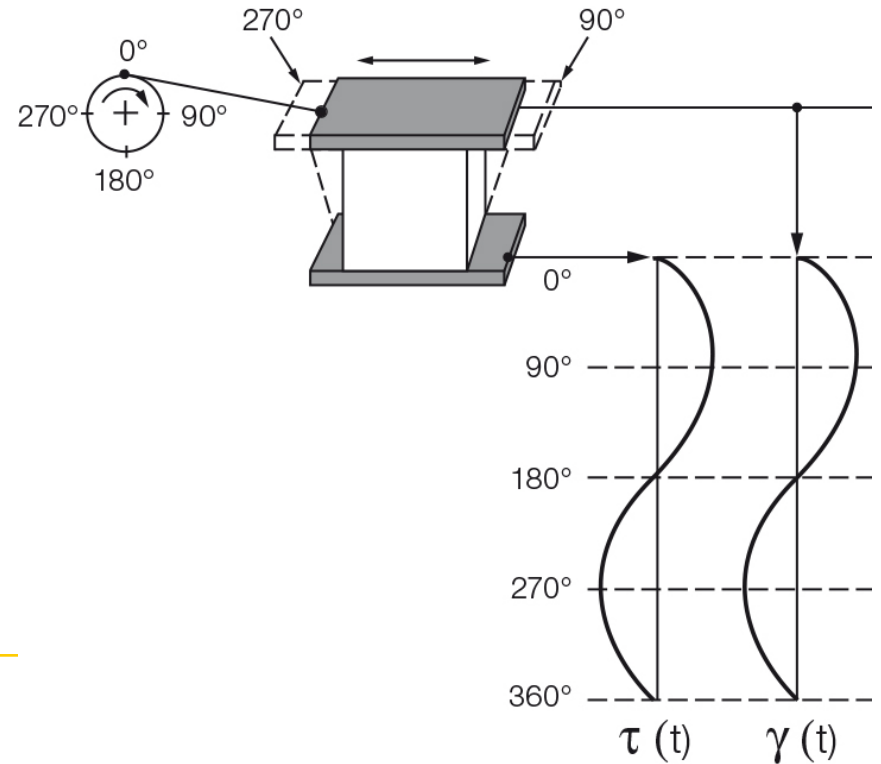


Two plates model, equipped with two sensors, on top:  
preset of deflection path (strain or deformation) bottom:  
measurement of resulting force (shear stress)

## Sinusoidal preset

For ideally elastic behavior of a totally stiff  
sample (e.g. a stone or steel):

- There is no time shift between the sine curves of preset strain and resulting shear stress:
- The curves of  $\gamma$  and  $\tau$  are “in phase”



$$G^* = \frac{\tau(t)}{\square t}$$

$$G^* = G' + iG''$$

$$G' = \frac{\tau_A}{\gamma_A} * \cos(\delta)$$

$$G'' = \frac{\tau_A}{\gamma_A} * \sin(\delta)$$

$$|G^*| = \sqrt{(G')^2 + (G'')^2}$$

$i = \sqrt{-1}$ ...imaginary unit

$G'$ ...**storage modulus** [Pa]: refers to stress energy that is stored upon deformation and completely recovered after removal of the external stress

$G''$ ...**loss modulus** [Pa]: refers to energy that is lost during shear induced flow (energy dissipation)

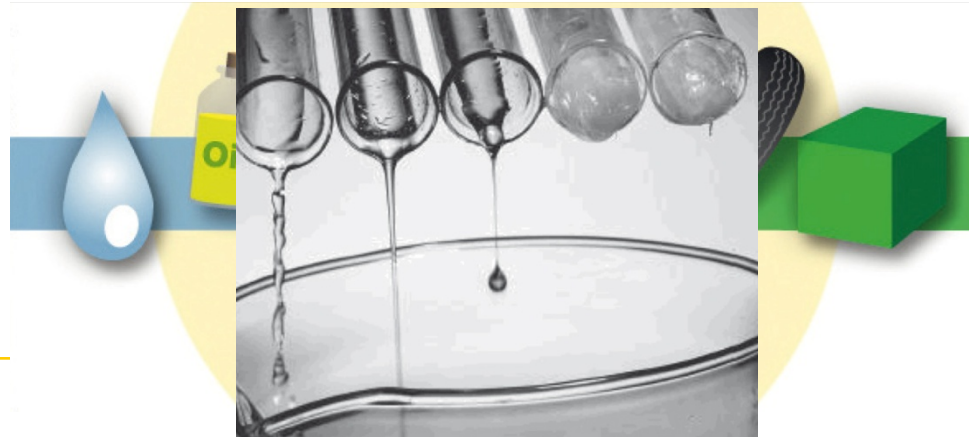
$$\frac{G''}{G'} = \frac{\sin(\delta)}{\cos(\delta)} = \tan(\delta)$$

$$|G^*| = \omega * |\eta^*|$$

$|\eta^*|$ ...**complex (dynamic) viscosity**

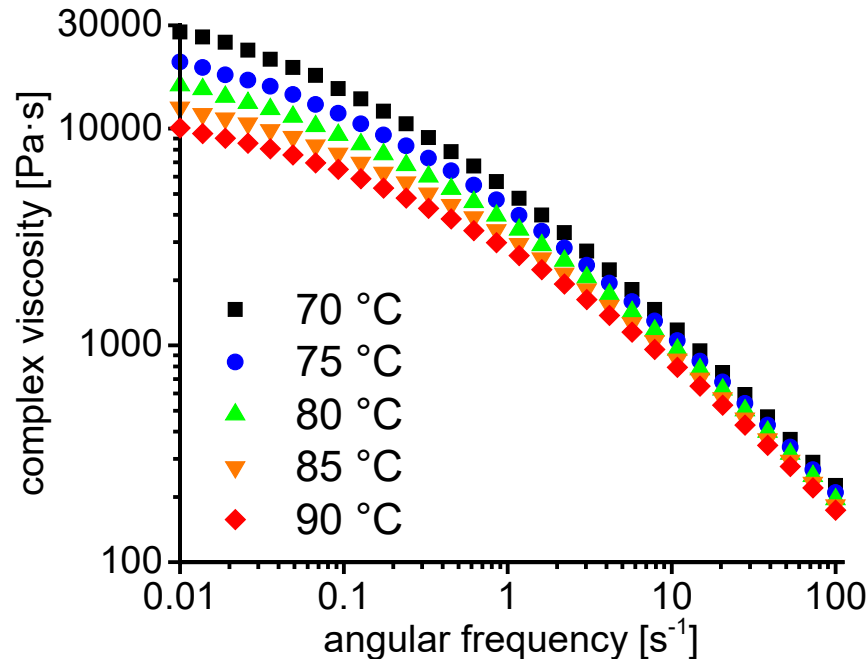
# Viscoelasticity: summary

Ideal viscous flow behavior	Behavior of a viscoelastic liquid (sol)	Sol/gel transition point	Behavior of a viscoelastic solid (gel)	Idealelastic deformation behavior
$\delta = 90^\circ$	$90^\circ > \delta > 45^\circ$	$\delta = 45^\circ$	$45^\circ > \delta > 0^\circ$	$\delta = 0^\circ$
$\tan(\delta) \rightarrow \infty$	$\tan(\delta) > 1$	$\tan(\delta) = 1$	$\tan(\delta) < 1$	$\tan(\delta) \rightarrow 0$
$G' \rightarrow 0$	$G'' > G'$	$G' = G''$	$G' > G''$	$G'' \rightarrow 0$



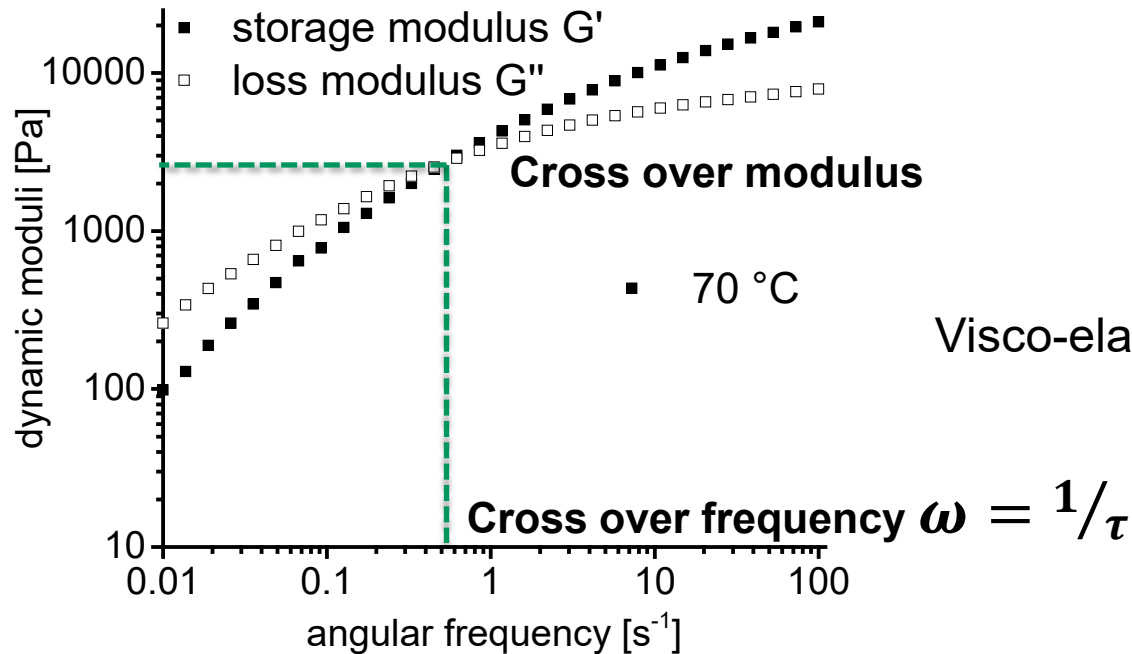
# Solutions with direct solvents

# Frequency sweep



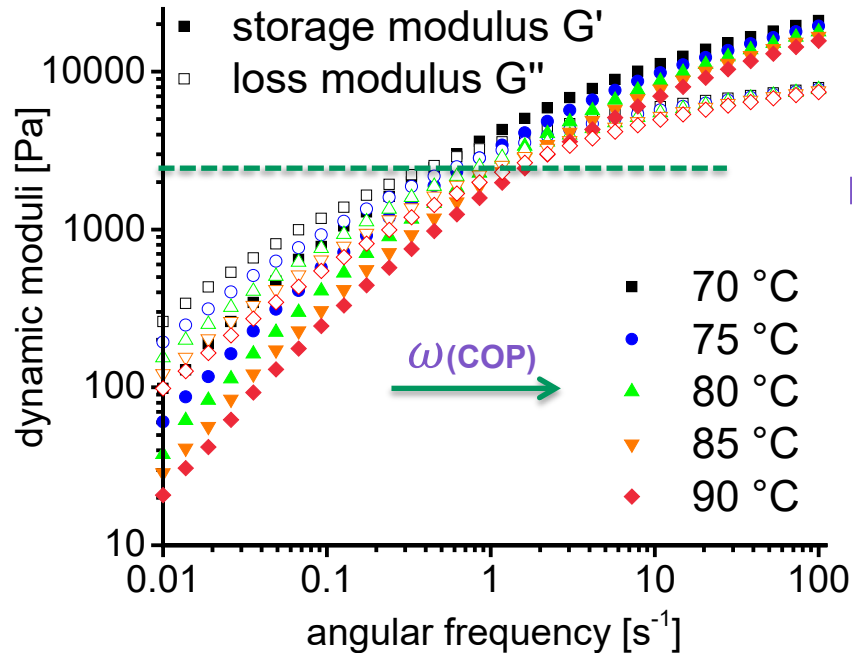
Oscillatory frequency sweep measurements provides complex viscosity as function of angular frequency

# Frequency sweep



Visco-elasticity described by storage and loss moduli

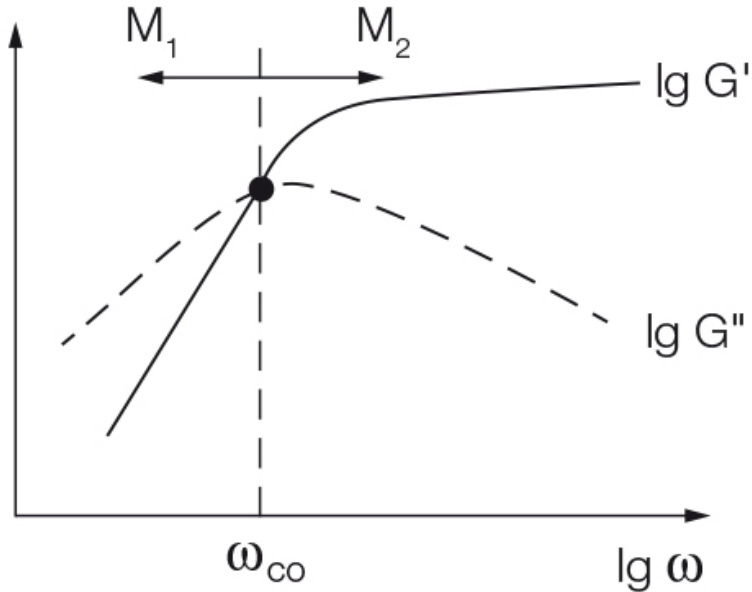
# Frequency sweep



$G_{COP}$  does not change much

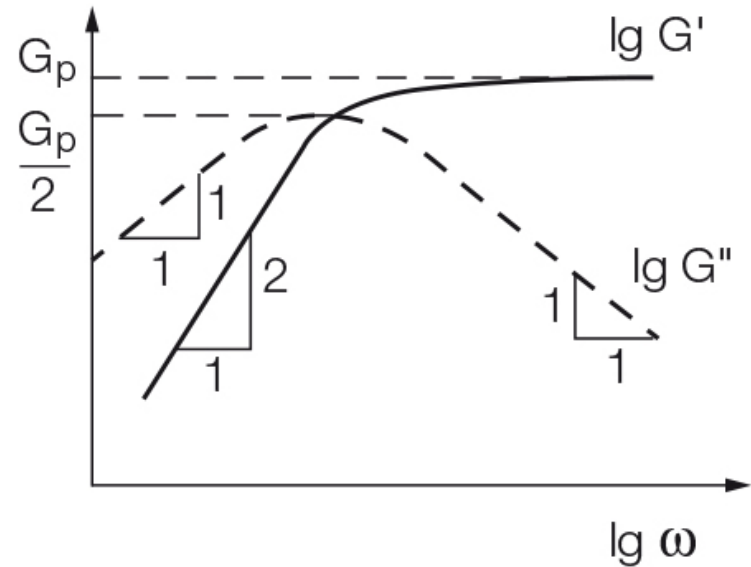
Visco-elasticity affected by the temperature

# Frequency sweep



## Average molar mass $M$

Position of the crossover point  $G' = G''$ , depends on  $M$  (here:  $M_1 > M_2$ )

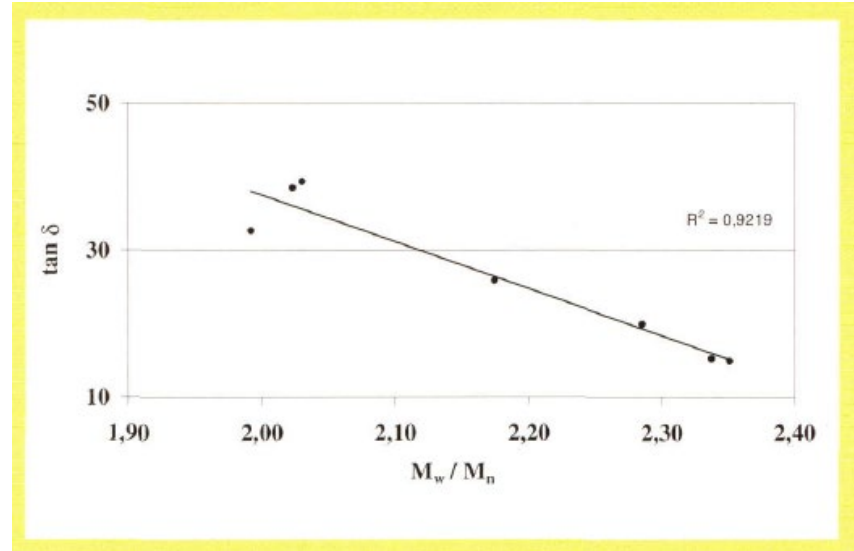
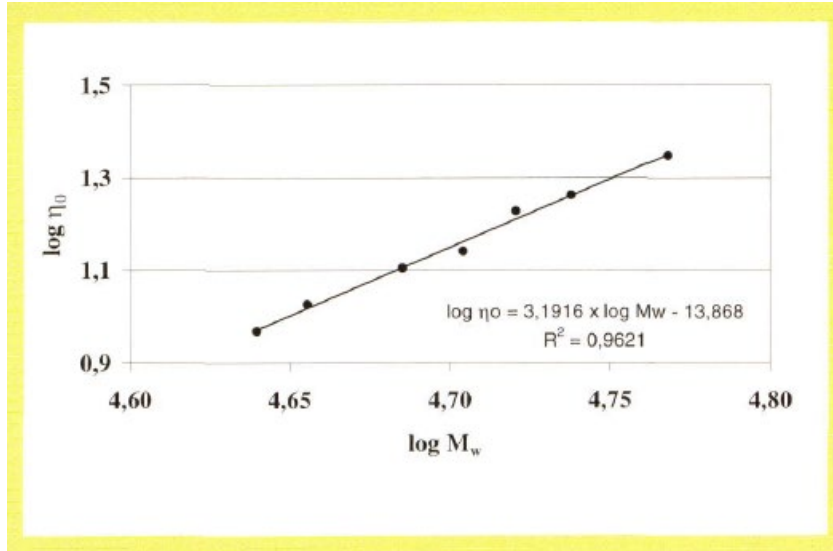


## Maxwellian behavior

In the range of low frequencies  $G''(\omega)$  and  $G'(\omega)$  show the slopes of 1:1 and 2:1



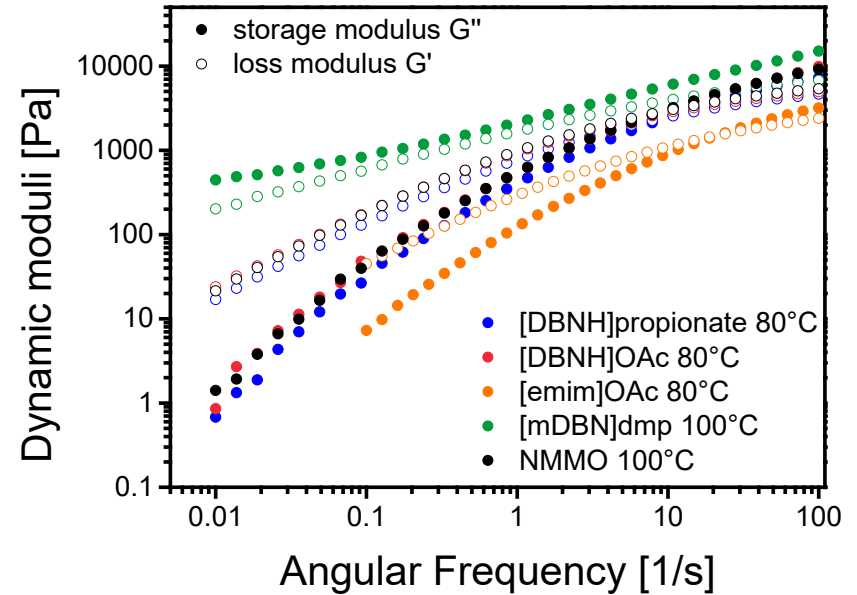
# Determination of molar mass



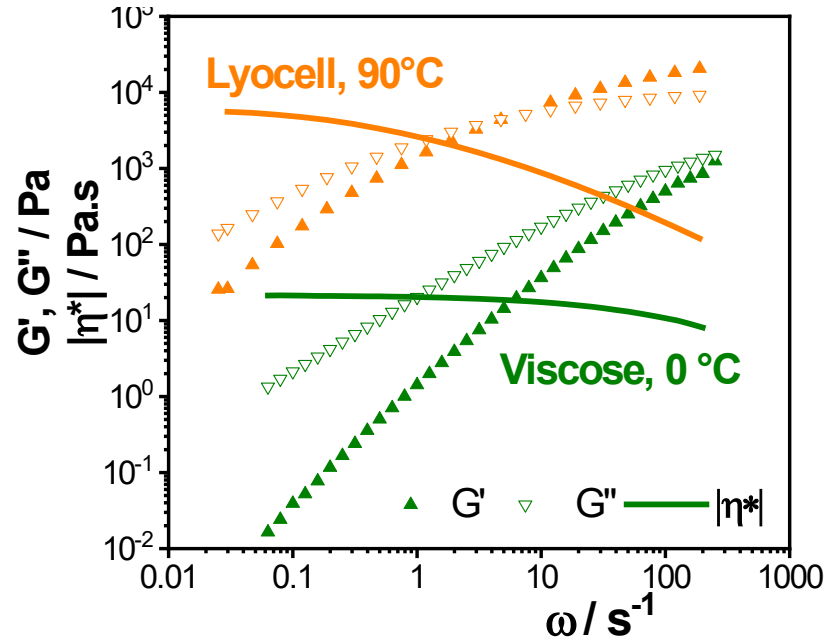
Correlation between zero shear viscosity  $\eta_0$  and weight average molar mass  $M_w$

Correlation between  $\tan(\delta)$  and polydispersity index  $M_w/M_n$

# Pulp solutions

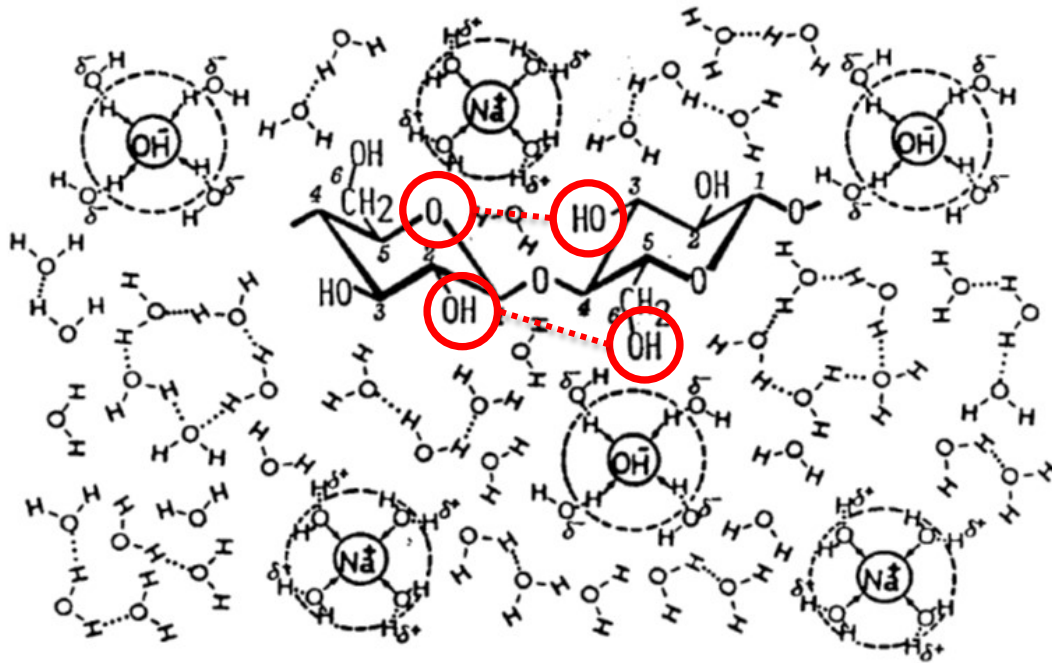


# Viscose vs Lyocell vs Ionic liquids



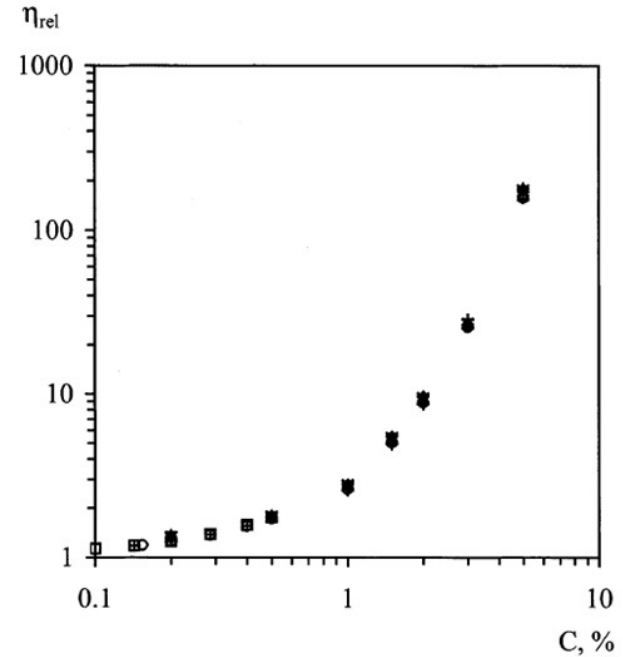
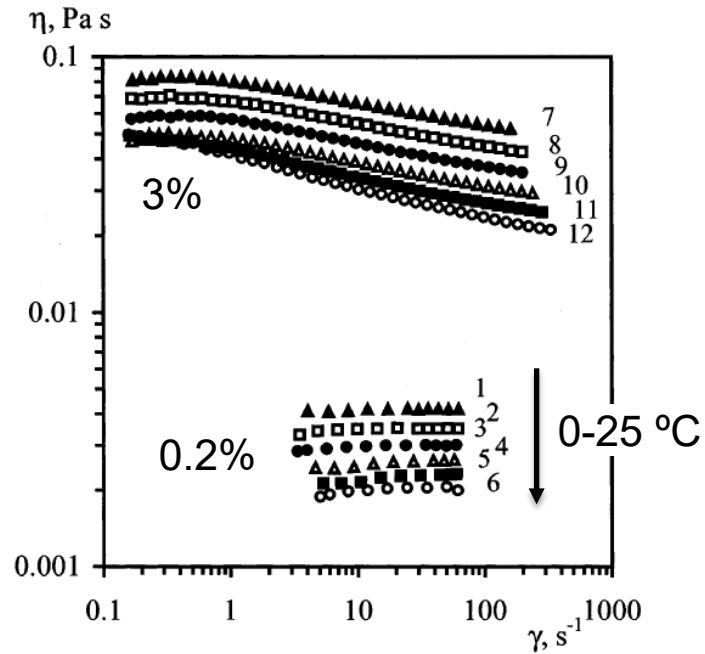
# Aqueous solutions

# NaOH solutions

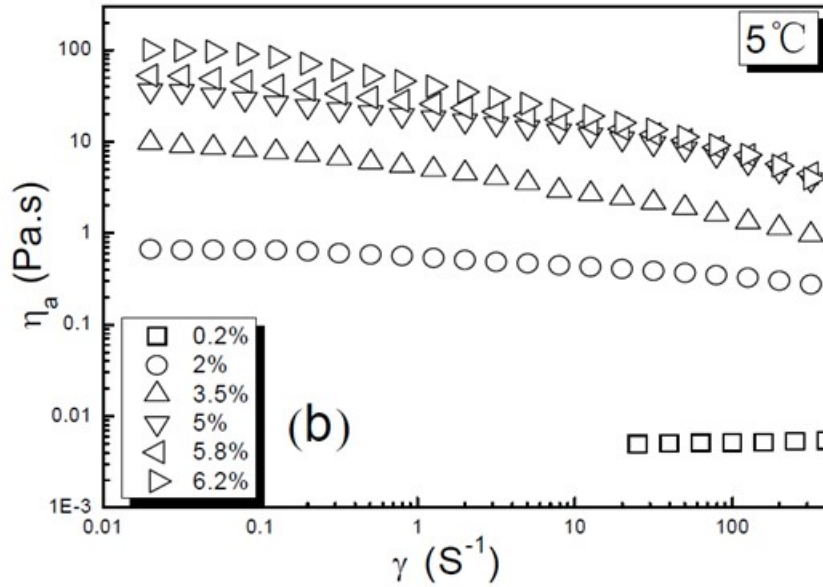


Deconstruction of intramolecular  
 $O_3-H...O_5'$  and  $O_2-H...O_6'$   
H-bonds

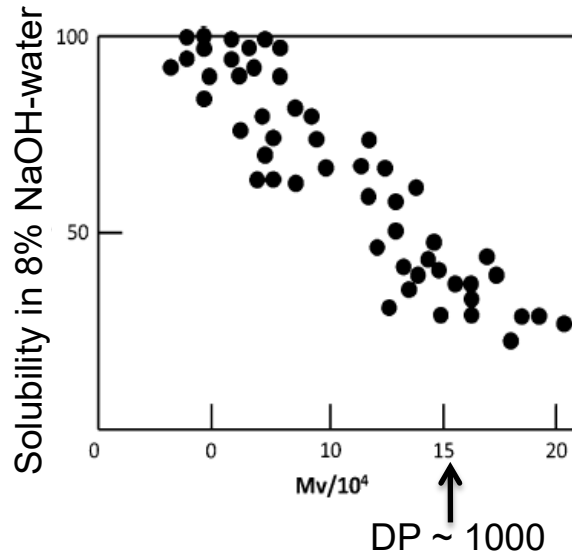
# NaOH solutions



# NaOH solutions



# NaOH solutions

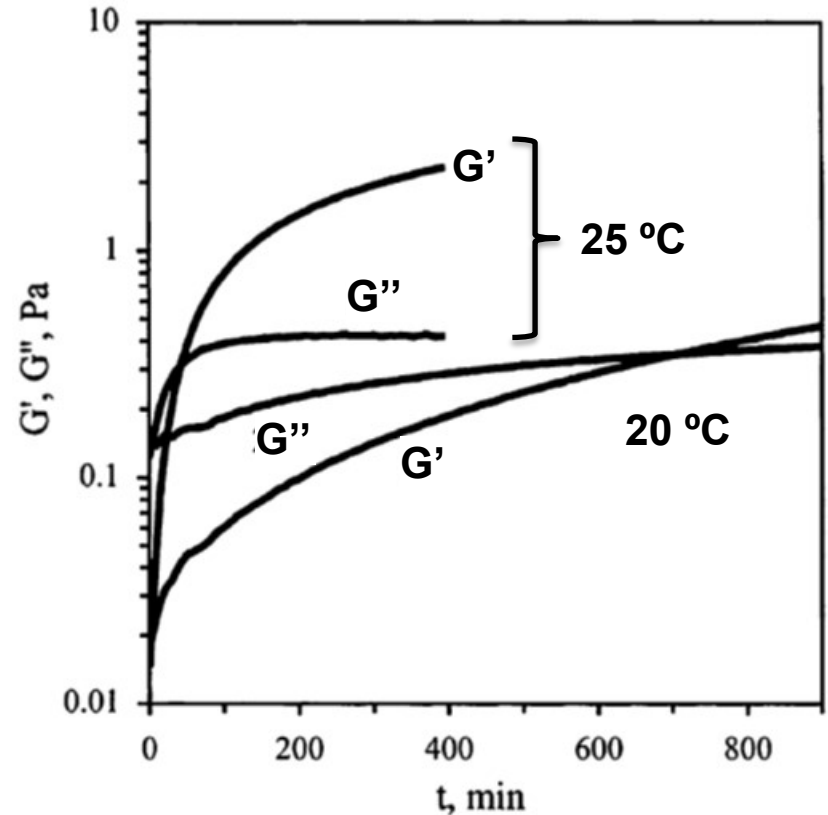


- Major limitation of NaOH as solvent: solubility of cellulose strongly dependent on DP
- Upper limit for cellulose concentration;
- Limited mechanical properties of regenerated products



# NaOH solutions

- tendency of solutions to gel irreversibly
- Gelling over time
- Pronounced gelling upon temperature increase

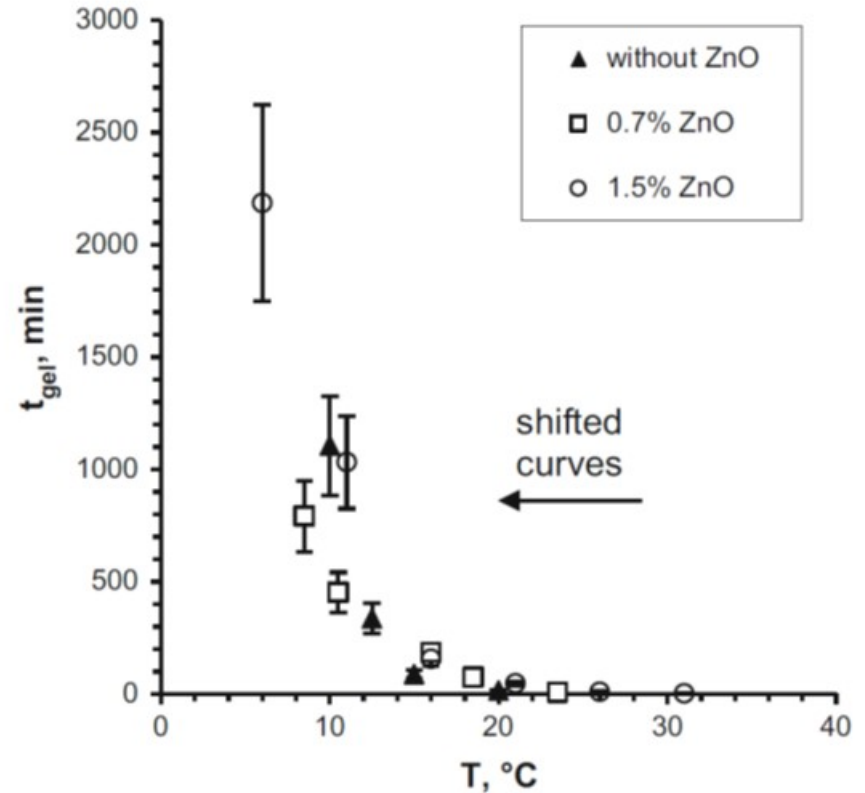


# NaOH solutions – additives

Various additives tested:

- amongst longest know: ZnO
- also urea and thiourea

No confirmed effect on solubility maximum; but stabilization of solution state and hampering of gelation



# Summary questions

- **What is viscoelasticity?**
- **How does the temperature affect viscoelasticity?**
- **How does the polymer molecular weight affect viscoelasticity?**
- **Compare aqueous and direct cellulose solutions in terms of their viscoelastic properties**