Chapter 8

- LQG control
- Robustness of LQG control
- Loop transfer recovery (LTR)
- Introduction to Model Predictive Control

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Note:

LQG theory (Linear-Quadratic-Gaussian) means optimal (LQ) control with Gaussian noise disturbances present. The stochastic theory of continuous time systems is difficult.

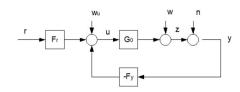
It is possible to present the theory in a "simplified" form. The important thing is to know that noise intensities (variance does not exist for continuous time stochastic signals) are mostly used as tuning parameters only. The optimal state estimator, Kalman filter, is used to estimate the states, which are fed back according to the LQ theory.

LQG = Kalman filter + LQ



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Chapter 8: LQG-control



$$z = Gu + w$$
 $u = F_r r - F_y y$ $e = z - r$ $y = z + n$

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- -how to describe, how "big" the signal is?
- -how to describe the frequency content of the signal?
- -how to describe the signal as the output of a dynamical system, driven by "white noise".

signal size (norm):

$$||z||_2^2 = \int_{-\infty}^{\infty} |z(t)|^2 dt$$
 ; $|z(t)|^2 = z^T(t)z(t)$; $z mx1$ vector

or the matrix measure

$$R_z = \int_{-\infty}^{\infty} z(t)z^T(t)dt$$
 "covariance" of $z(t)$ dimension mxm

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But let us look:

$$\left\|z\right\|_{2}^{2} = \int_{-\infty}^{\infty} \left|z(t)\right|^{2} dt = \int_{-\infty}^{\infty} z^{T}(t)z(t)dt = \underbrace{\int_{-\infty}^{\infty} \left[z_{1}^{2}(t) + z_{2}^{2}(t) + \dots + z_{m}^{2}(t)\right]}_{\operatorname{tr}(\mathbb{R}_{z})} dt$$

$$R_z = \int_{-\infty}^{\infty} z(t) z^T(t) dt$$

 $||z||_2^2 = \text{tr}(R_z)$ "trace" is the sum of the main diagonal elements of a matrix (see. 2.nd exercise set.)



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The spectral density is defined

$$\Phi_{u}(\omega) = U(i\omega)U^{*}(i\omega)$$

in which

$$U(i\omega) = \int_{-\infty}^{\infty} u(t)e^{-i\omega t}dt$$
 Fourier-transformation of the signal

$$R_{u} = \frac{1}{2\pi} \int_{-\infty}^{\infty} \Phi_{u}(\omega) d\omega = \frac{1}{2\pi} \int_{-\infty}^{\infty} U(i\omega) U^{*}(i\omega) d\omega = \int_{-\infty}^{\infty} u(t) u^{T}(t) dt$$

Covariance vs. signal size (Parseval's theorem)



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Spectral description of disturbances

To a *m*-dimensional u(t) a hermitian $m \times m$ -matrix $\Phi_u(\omega)$ is attached, (spectrum, spectral density)

If G is a linear and stable system, then

$$y(t) = G(p)u(t)$$

$$\Phi_{v}(\omega) = G(i\omega)\Phi_{u}(\omega)G^{*}(i\omega)$$



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m x m-dimensional matrix

$$R_u = \frac{1}{2\pi} \int_{-\infty}^{\infty} \Phi_u(\omega) d\omega$$

measures the size of signal \boldsymbol{u} by weighting the frequency components.

Cross-correlation spectral density:

$$z = \begin{bmatrix} y \\ u \end{bmatrix} \qquad \Phi_z(\omega) = \begin{bmatrix} \Phi_{yy}(\omega) & \Phi_{yu}(\omega) \\ \Phi_{uy}(\omega) & \Phi_{uu}(\omega) \end{bmatrix}$$

hermitian $\Phi_{vu}(\omega) = \Phi^*_{uy}(\omega)$



Two signals do not correlate, if their cross-correlation spectral density is identically zero.

The signal is called **white noise**, intensity *R*, if its spectral density is constant at the frequency range

$$\Phi_{\scriptscriptstyle e}(\omega) \equiv R$$

R is known as the **intensity** of the signal.

The history of a white noise signal does not give any information of the future values of the signal.



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Note. The "stochastic" interpretation of stochastic systems has not been used above, e.g.

$$R_{u}(\tau) = \lim_{N \to \infty} \frac{1}{N} \int_{0}^{N} u(t)u^{T}(t-\tau)dt = E\left\{u(t)u^{T}(t-\tau)\right\}$$

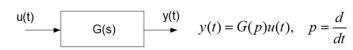
$$\Phi_u(\omega) = \int_0^\infty R_u(\tau) e^{-i\omega\tau} d\tau$$

$$R_{u} = \frac{1}{2\pi} \int_{-\infty}^{\infty} \Phi_{u}(\omega) d\omega = R_{u}(0) = \lim_{N \to \infty} \frac{1}{N} \int_{0}^{N} u(t) u^{T}(t) dt$$



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$$U(i\omega) = \int_{-\infty}^{\infty} u(t)e^{-i\omega t}dt$$
 Fourier transformation of the signal

$$\Phi_u(\omega) = U(i\omega)U^*(i\omega)$$
 Spectral density

$$R_{u} = \frac{1}{2\pi} \int_{-\infty}^{\infty} \Phi_{u}(\omega) d\omega = \frac{1}{2\pi} \int_{-\infty}^{\infty} U(i\omega) U^{*}(i\omega) d\omega = \int_{-\infty}^{\infty} u(t) u^{T}(t) dt$$

Covariance vs. signal size (Parseval's theorem)

$$Y(i\omega) = G(i\omega)U(i\omega)$$

$$\Phi_{y}(\omega) = Y(i\omega)Y^{*}(i\omega) = G(i\omega)U(i\omega)U^{*}(i\omega)G^{*}(i\omega)$$
$$= G(i\omega)\Phi_{y}(\omega)G^{*}(i\omega)$$



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When it is assumed that the stochastic process is *stationary* and *ergodic*, the modelling with the following formulas are adequate

$$y(t) = G(p)u(t)$$
 linear system

$$\Phi_{y}(\omega) = G(i\omega)\Phi_{u}(\omega)G^{*}(i\omega)$$
 spectral density

$$R_u = \frac{1}{2\pi} \int_{-\infty}^{\infty} \Phi_u(\omega) d\omega = Eu(t)u^T(t)$$
 covariance vs. signal size



But how do we manage with white noise?

$$\Phi_e(\omega) \equiv R$$
 R is the intensity

$$R_e = \frac{1}{2\pi} \int_{-\infty}^{\infty} \Phi_e(\omega) d\omega = \frac{1}{2\pi} \int_{-\infty}^{\infty} E(i\omega) E^*(i\omega) d\omega = \int_{-\infty}^{\infty} e(t) e^T(t) dt$$

The covariance of the white noise is intensity multiplied with the impulse function; note

$$\Phi_e(\omega) = \int_{-\infty}^{\infty} R_e(\tau) e^{-i\omega\tau} d\tau$$

The variance of white noise is infinite, so we are dealing with a mathematical idealization, which really does not exist.



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We obtain

$$\Phi_{y}(\omega) = |G(i\omega)|^{2} \Phi_{u}(\omega) + \lambda |H(i\omega)|^{2}$$

$$\Phi_{yu}(\omega) = G(i\omega)\Phi_{u}(\omega)$$

in which the basic equation

$$\Phi_{v}(\omega) = G(i\omega)\Phi_{u}(\omega)G^{*}(i\omega)$$

has been used.

More generally for a linear filter:

let the input be white noise e with the intensity R



Example. Let

$$y(t) = G(p)u(t) + H(p)e(t)$$

where u and e are uncorrelated scalar signals with the spactral densities

$$\Phi_u(\omega)$$
 and $\Phi_e(\omega) = \lambda$

Use the variable $\varsigma(t) = \begin{bmatrix} u \\ e \end{bmatrix}$ which leads to

$$z(t) = \begin{bmatrix} y(t) \\ u(t) \end{bmatrix} = \begin{bmatrix} G(p) & H(p) \\ 1 & 0 \end{bmatrix} \varsigma(t) , \quad \Phi_{\varsigma} = \begin{bmatrix} \Phi_{u} & 0 \\ 0 & \lambda \end{bmatrix}$$

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$$v(t) = G(p)e(t)$$

The spectral density of the output is then

$$\Phi_{v}(\omega) = G(i\omega)RG^{*}(i\omega)$$

and in the scalar case

$$\Phi_{v}(\omega) = R \cdot |G(i\omega)|^{2}$$

Basic model for a disturbance signal: output of a linear time-invariant filter driven by white noise.



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General state-space realization of the process is

$$\dot{x} = Ax + Bu + Nv_1$$

$$z = Mx$$

$$y = Cx + v_2$$

and the criterion

$$\min \left(\left\| e \right\|_{Q_{1}}^{2} + \left\| u \right\|_{Q_{2}}^{2} \right) = \min \int \left[e^{T}(t)Q_{1}e(t) + u^{T}(t)Q_{2}u(t) \right] dt$$

$$e = z - r$$

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Solution (without proof): Let (A,B) be stabilizable and (A,C) detectable.

The optimal control law is

$$u(t) = -L\hat{x}(t)$$

$$\dot{\hat{x}}(t) = A\hat{x}(t) + Bu(t) + K[y(t) - C\hat{x}(t)]$$

in which the Kalman gain K is obtained by the Riccati equation

$$AP + PA^{T} + NR_{1}N^{T} - (PC^{T} + NR_{12})R_{2}^{-1}(PC^{T} + NR_{12})^{T} = 0$$

$$K = (PC^{T} + NR_{12})R_{2}^{-1}$$



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Consider the regulator problem (r = 0)

$$\dot{x} = Ax + Bu + Nv_1$$

$$z = Mx$$

$$y = Cx + v_2$$

white noise
$$\begin{bmatrix} v_1 \\ v_2 \end{bmatrix}$$
 with intensity $\begin{bmatrix} R_1 & R_{12} \\ R_{12}^T & R_2 \end{bmatrix}$

Determine

$$u(t) = -F_v(p)y(t)$$
 such that

$$V = ||z||_{Q_1}^2 + ||u||_{Q_2}^2$$
 is minimized

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and the state feedback coefficient L

$$L = Q_2^{-1} B^T S$$

where S is the solution to the stationary Riccati equation (LQ)

$$A^{T}S + SA + M^{T}Q_{1}M - SBQ_{2}^{-1}B^{T}S = 0$$

(symmetric and positive semidefinite solution)

(Note that only infinite optimization horizons are considered here, so that the stationary Riccati equations can be used.)



The solution has the *separation property*: the optimal state observer and optimal state feedback can be designed independent of each other. The whole solution is then the "combination" of these.

If the states are measurable, y = x, the Kalman-filter is not needed and the state feedback is formed directly from the state.

The theory guarantees that the resulting closed-loop system is stable.

Terms: LQ (linear quadratic)

LQG (linear quadratic gaussian) ARE (algebraic Riccati equation)

(Separation principle)



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But how about the robustness of the LQ(LQG) – controller?

$$e = (I - G_c)r - Sw + Tn$$

$$u = G_{vv}r + G_{vvv}(w + n)$$

Not necessarily very good!

The weight matrices and noise intensities can be thought to be *tuning parameters* in control design.

After design the frequency domain analysis and simulations must be carried out to verify the performance of the controller. Next, consider robustness a bit closer.



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Matlab:

kalman, estim lqgreg

lqr, dlqr

lqe, dlqe lqrd

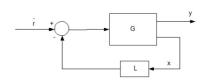
sigma, dsigma



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Robustness of LQ/LQG-controllers

LQ: u(t) = -Lx(t) $\dot{x}(t) = Ax(t) + Bu(t)$



The loop transfer function (gain in control signal)

$$G_k(s) = L(sI - A)^{-1}B$$

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But in that transfer function

$$H(s) = L(sI - A)^{-1} B$$

L is determined from the equations

$$L = Q_2^{-1}B^T S$$

 $A^T S + SA + Q_1 - SBQ_2^{-1}B^T S = 0$

and now it holds (apply the lemma 5.2 in the textbook)

$$\left[I + H(-i\omega)\right]^T Q_2 \left[I + H(i\omega)\right] \ge Q_2$$

which in SISO-case is

$$|1+H(i\omega)|\geq 1$$



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LQG:
$$u(t) = -L\hat{x}(t) + \tilde{r}(t)$$
$$p\hat{x}(t) = A\hat{x}(t) + Bu(t) + K[y(t) - C\hat{x}(t)]$$

It follows

$$u(t) = -F_y(p)y(t) + F_r(p)\tilde{r}(t)$$

$$F_y(p) = L(pI - A + BL + KC)^{-1}K$$

$$F_r(p) = I - L(pI - A + BL + KC)^{-1}B$$

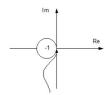
and the loop gains are

$$GF_y = C(sI - A)^{-1}BL(sI - A + BL + KC)^{-1}K$$

 $F_yG = L(sI - A + BL + KC)^{-1}KC(sI - A)^{-1}B$



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That means that the Nyquist curve will never go inside the circle shown in the figure:

- -phase margin at least 60 degrees
- -gain margin infinite
- -the magnitude of the sensitivity function is less than one
- -the magnitude of the complementary sensitivity function is smaller than two.



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looked from the output or input side of the process . (For SISO-systems the functions are the same.)

But now the good robustness properties do not necessarily hold, even though K and L have been chosen according to the LQG-formulas (the phase margin can even be arbitrarily small).

An idea to fix that problem: let L be chosen as above. Can K be chosen such that

$$F_{y}G = L(sI - A + BL + KC)^{-1}KC(sI - A)^{-1}B \approx L(sI - A)^{-1}B$$

which would make it possible to enjoy the "ideal" loop transfer function again.



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Result: Yes, it is possible by choosing

$$K = \rho B$$

where ρ is large enough. That holds generally and also in MIMO case; the number of inputs and outputs must be the same.

This technique is called the **loop transfer recovery** (*LTR*).

The idea is to calculate L as the solution to the optimal control problem and then change K as described above. (To increase ρ until the desired sensitivity functions are obtained.) But there is no guarantee that the filter remains stable.



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where the last two terms dominate, as α grows. Hence

$$K \approx \sqrt{\alpha}B$$

holds, and also the Kalman-filter remains Ok.

Now the tuning parameters were N, R_1 and R_2 .

Note. The presented method was *input-LTR*, because the loop transfer function was F_yG (gain of the input signal)

There exists also an *output-LTR* method based on GF_y In *SISO*-case the two methods are the same.



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Use another procedure to aim at $K = \rho B$

$$\dot{x} = Ax + Bu + Nv_1$$

$$z = Mx$$

$$y = Cx + v_2$$

$$K = PC^T R_2^{-1}$$

$$PA^T + AP - PC^T R_2^{-1} CP + NR_1 N^T = 0$$
(Kalman)

Choose

$$R_1 = \alpha R_2$$
, $N = B$ α being "large". Then
$$PA^T + AP - KR_2K^T + \alpha BR_2B^T = 0$$



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Model Predictive Control (MPC)

Literature:

- Wang, L, Model Predictive Control System Design and Implementation Using MATLAB, Springer, 2009.
- Maciejowski, J. M., Predictive Control, with Constraints, Pearson Education, 2002.
- Rawlings, J. B., and Mayne, D. Q., Model Predictive Control, Theory and Design, Nob Hill, 2009.





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Model Predictive Control

- · Can deal with constraints in a natural way
- · The basic idea is easy to understand
- It extends to multivariable plants naturally
- · Generally more powerful than traditional PID control
- Integrates optimal control, stochastic control, control of processes with dead-time, multivariable control, control that can handle constraints.
- A practical methodology, which has numerous technical applications, especially in the process industry.
- It was earlier neglected and critisized by the control engineering community (lack of stability proofs, robustness etc.); this situation has changed due to progress in theory.

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Remark 1.1. Note that a number of control methods which have gained popularity in industry, such as fuzzy control and neural control, do not explicitly address any of the fundamental control issues in a quantitative way at all. This is the main reason why control people do not usually take these methods seriously. Naturally, these methods will still often work at least in not too demanding applications. They also appeal to many people with a non-control background and their functioning can more easily be explained to process operators and the media.

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The main characteristics in MPC

- An internal model capable of fast simulation
- A reference trajectory which defines the desired closed-loop behaviour
- The *receding horizon* principle
- Future input trajctory by a finite number of control moves
- On-line optimization (possibly constrained)

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Model Predictive Control Reference trajectory Predicted outputs Model Predicted outputs Optimizer Future errors Cost function Constraints

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- A lot of different formulations can be found in the literature (MPHC, MAC, DMC, EHAC, EPSAC, GPC etc. etc.)
- Maciejowski's book has information on commercial MPC products, e.g. DMCPlus, RMPCT, Connoisseur, PFC, HIECON, 3dMPC, Process Perfecter.

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The Receding horizon principle

\[
\begin{align*}
\text{u(t)} & \text{u(t)} & \text{u(t)} & \text{v(t+k+t)} & \text{v(t+k+t)} & \text{v(t+k+t)} & \text{The output is predicted over the prediction horizon. Control moves are calculated over the control horizon by optimizing a criterion. Only the first move is realized; then the process is repeated.}

\[
\begin{align*}
\text{Alto University School of Science and Technology} & \text{only the first move is realized; then the process is repeated.} \]

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Model predictive control (MPC)

- Note that there are different formalisms to pose the MPC problem.
- Also, there exist software packages to do the job.
 The problem in using software packages "blindly" is the lack of insight and analysis possibilities.
- For example: Matlab's MPC toolbox is good in posing and solving problems at a reasonably high level. It is somewhat difficult to use it in research though.
- It is good to make one formalism yourself to get insight.
 The software packages then become easier to deal with.

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Cost function

$$V(k) = \sum_{i=H_{-}}^{H_{p}} \left\| \hat{z}(k+i|k) - r(k+i|k) \right\|_{Q(i)}^{2} + \sum_{i=0}^{H_{g}-1} \left\| \Delta \hat{u}(k+i|k) \right\|_{R(i)}^{2}$$

Prediction horizon H_p , Q(i), R(i) positive semidefinite Control horizon H

Control move Δu it is assumed that the penalty is on the control moves, not controls as such

Note that if $H_w > 1$ there is no penalty immediately at time k.

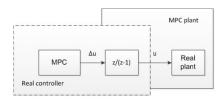
The states are usually not measurable; instead we have predictions $\hat{x}(k+1|k)$ meaning that we estimate the state by using data up to time k.



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Alternative state variable choices

• Usually the MPC gives the *control move* as its output, whereas the project model uses absolute values. The *integration* in the state space model is then needed (to create u from Δu



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Features of constrained predictive control

- Constraints cause MPC be nonlinear. But most of the time (when constraints are not near to be active) the controller operates in a linear way.
- In practice, meeting a hard constraint can be dangerous for the system. An MPC might do hazardous actions (in "panic"); usually a supervisory mode is used to prevent such actions.
- We consider only time-invariant MPC. The system has then constant coefficient matrices. In

$$V(k) = \sum_{i=H_{\varphi}}^{H_{p}} \left\| \hat{z}(k+i | k) - r(k+i | k) \right\|_{\mathcal{Q}(i)}^{2} + \sum_{i=0}^{H_{u}-1} \left\| \Delta \hat{u}(k+i | k) \right\|_{\mathcal{Z}(i)}^{2}$$

Q(i) and R(i) can vary with i , but they must not change with k

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Prediction

- Predictions of the controlled variables
 \$\hat{z}(k+i|k)\$ must be obtained to solve the control problem. They are based on the best estimates of
 \$\hat{x}(k|k)\$ and the assumed future inputs (or the latest input \$u(t-1)\$)
- The predictor can be seen as a "tuning parameter" in the MPC problem, because it plays a key role in the performance of the controller.
- We are actually specifying a model of the environment in which the plant is operating
- Assuming that the states are measurable and there are *no disturbances* we get



Prediction

$$\begin{split} \hat{x}(k+1|k) &= Ax(k) + B\hat{u}(k|k) \\ \hat{x}(k+2|k) &= A\hat{x}(k+1|k) + B\hat{u}(k+1|k) = A^2x(k) + AB\hat{u}(k|k) + B\hat{u}(k+1|k) \\ \vdots \\ \hat{x}(k+H_p|k) &= A\hat{x}(k+H_p-1|k) + B\hat{u}(k+H_p-1|k) \\ &= A^{H_p}x(k) + A^{H_p-1}B\hat{u}(k|k) + \dots + B\hat{u}(k+H_p-1|k) \end{split}$$

But $\hat{u}(k+i|k) = \hat{u}(k+H_u-1|k)$, $H_u \le i \le H_p-1$ and earlier control moves will be studied only. So $\hat{u}(k|k) = \Delta \hat{u}(k|k) + u(k-1)$

$$\begin{split} \hat{u}(k+1\big|k) = & \Delta \hat{u}(k+1\big|k) + \Delta \hat{u}(k\big|k) + u(k-1) \\ \vdots \end{split}$$

 $\hat{u}(k+H_u-1|k) = \Delta \hat{u}(k+H_u-1|k) + ... + \Delta \hat{u}(k|k) + u(k-1)$

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Prediction

$$\begin{split} \hat{x}(k+H_u+1\big|k) &= A^{H_u+1}x(k) + (A^{H_u}+\ldots+A+I)B\Delta\hat{u}(k\big|k) \\ &\qquad \ldots + (A+I)B\Delta\hat{u}(k+H_u-1\big|k) + (A^{H_u}+\ldots+A+I)Bu(k-1) \\ \vdots \\ \hat{x}(k+H_p\big|k) &= A^{H_p}x(k) + (A^{H_p-1}+\ldots+A+I)B\Delta\hat{u}(k\big|k) \\ &\qquad \ldots + (A^{H_p-H_u}+\ldots+A+I)B\Delta\hat{u}(k+H_u-1\big|k) + (A^{H_p-1}+\ldots+A+I)Bu(k-1) \end{split}$$

We can collect everything in a matrix-vector form



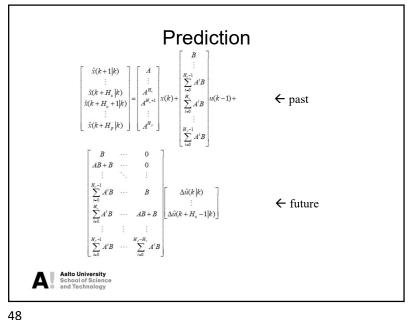
Prediction

• Hence we get

$$\begin{split} \hat{x}(k+1|k) &= Ax(k) + B\Big[\Delta \hat{u}(k|k) + u(k-1)\Big] \\ \hat{x}(k+2|k) &= A^2x(k) + AB\Big[\Delta \hat{u}(k|k) + u(k-1)\Big] + B\Big[\Delta \hat{u}(k+1|k) + \Delta \hat{u}(k|k) + u(k-1)\Big] \\ &= A^2x(k) + (A+I)B\Delta \hat{u}(k|k) + B\Delta \hat{u}(k+1|k) + (A+I)Bu(k-1) \\ &\vdots \\ \hat{x}(k+H_u|k) &= A^{H_u}x(k) + (A^{H_u-1} + \ldots + A+I)B\Delta \hat{u}(k|k) \\ & \ldots + B\Delta \hat{u}(k+H_u-1|k) + (A^{H_u-1} + \ldots + A+I)Bu(k-1) \end{split}$$

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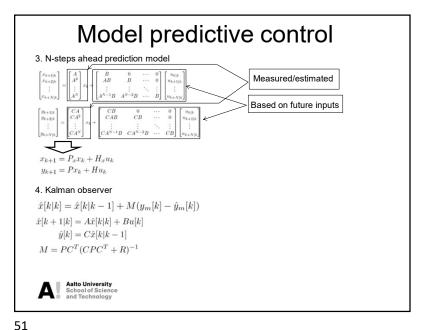
Prediction

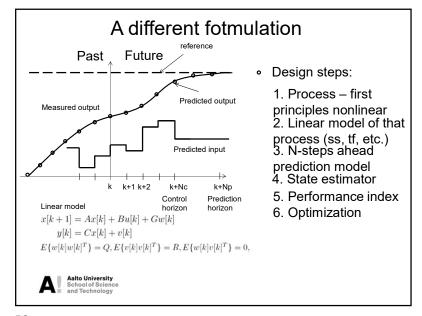
• The predictions are now obtained simply as

$$\begin{bmatrix} \hat{z}(k+1\big|k) \\ \vdots \\ \hat{z}(k+H_{_{P}}\big|k) \end{bmatrix} = \begin{bmatrix} C_z & 0 & \cdots & 0 \\ 0 & C_z & \cdots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & 0 & \cdots & C_z \end{bmatrix} \begin{bmatrix} \hat{x}(k+1\big|k) \\ \vdots \\ \hat{x}(k+H_{_{P}}\big|k) \end{bmatrix}$$

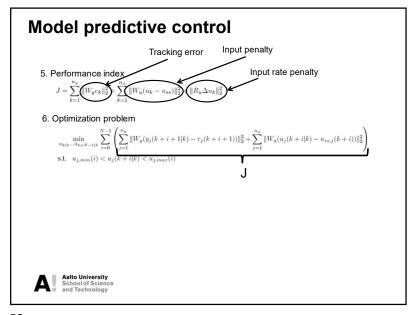
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The formalism in Wang's book

Process model

$$\dot{x}_m(t) = Ax_m(t) + Bu(t)$$
$$y(t) = Cx_m(t)$$

Discretized form

$$x_m(k+1) = A_m x_m(k) + B_m u(k)$$
$$y(k) = C_m x_m(k)$$

Form the difference

$$x_m(k+1) - x_m(k) = A_m \left[x_m(k) - x_m(k-1) \right] + B_m \left[u(k) - u(k-1) \right]$$



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and finally to

$$\begin{bmatrix} \Delta x_m^{x(k+1)} \\ y(k+1) \end{bmatrix} = \begin{bmatrix} A_m & o_m^T \\ C_m A_m & 1 \end{bmatrix} \begin{bmatrix} \Delta x_m^{x(k)} \\ y(k) \end{bmatrix} + \begin{bmatrix} B_m \\ C_m B_m \end{bmatrix} \Delta u(k)$$

$$y(k) = \begin{bmatrix} o_m^c & 1 \end{bmatrix} \begin{bmatrix} \Delta x_m(k) \\ y(k) \end{bmatrix}; \quad o_m = \begin{bmatrix} 0 & 0 \end{bmatrix}^{m_1} \cdots 0$$

Now, remember

$$\begin{bmatrix} y_{k+1|k} \\ y_{k+2|k} \\ \vdots \\ y_{k+N|k} \end{bmatrix} = \begin{bmatrix} CA \\ CA^2 \\ \vdots \\ CA^N \end{bmatrix} x_k + \begin{bmatrix} CB & 0 & \cdots & 0 \\ CAB & CB & \cdots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ CA^{N-1}B & CA^{N-2}B & \cdots & CB \end{bmatrix} \begin{bmatrix} u_{k|k} \\ u_{k+1|k} \\ \vdots \\ u_{k+N|k} \end{bmatrix}$$

or

$$Y = Fx(k_i) + \Phi \Delta U$$



and define the variables

$$\Delta x_m(k+1) = x_m(k+1) - x_m(k) \Delta x_m(k) = x_m(k) - x_m(k-1) \Delta u(k) = u(k) - u(k-1)$$

It follows that

$$\Delta x_m(k+1) = A_m \Delta x_m(k) + B_m \Delta u(k)$$

Denote $x(k) = \begin{bmatrix} \Delta x_m^T(k) & y(k) \end{bmatrix}^T$ which leads first to

$$y(k+1) - y(k) = C_m \left[x_m(k+1) - x_m(k) \right] = C_m \Delta x_m(k+1)$$

= $C_m A_m \Delta x_m(k) + C_m B_m \Delta u(k)$

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Written generally in the MIMO case

$$\underbrace{\begin{bmatrix} \Delta x (k+1) \\ y (k+1) \end{bmatrix}}_{x_a(k+1)} = \underbrace{\begin{bmatrix} A & \odot_{n_s \times n_y} \\ CA & \mathbb{1}_{n_y \times n_y} \end{bmatrix}}_{A_a} \underbrace{\begin{bmatrix} \Delta x (k) \\ y (k) \end{bmatrix}}_{x_a(k)} + \underbrace{\begin{bmatrix} B \\ CB \end{bmatrix}}_{B_a} \Delta u(k)$$

$$y(k) = \left[o_{n_s \times n_y} \, \mathbb{1}_{n_y \times n_y} \right] \underbrace{\left[\underbrace{o_{x}(k)}_{y(k)} \right]}_{C_x}$$

$$Y = [y(k_i + 1|k_i) \ y(k_i + 2|k_i) \dots y(k_i + N_p|k_i)]$$

$$\Delta U = [\Delta u(k_i) \ \Delta u(k_i + 1) \dots \Delta u(k_i + N_c - 1)]$$

$$Y = Fx_a(k_i) + \Phi \Delta U$$

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$$\Phi = \begin{bmatrix} C_a B_a & 0 & \cdots & 0 \\ C_a A_a B_a & C_a B_a & \cdots & 0 \\ C_a A_a^2 B_a & C_a A_a B_a & \cdots & 0 \\ \vdots & \vdots & \cdots & \vdots \\ C_a A_a^{N_p-1} B_a & C_a A_a^{N_p-2} B_a & \cdots & C_a A_a^{N_p-N_u} B_a \end{bmatrix} \qquad F = \begin{bmatrix} C_a A_a \\ C_a A_a^2 \\ \vdots \\ C_a A_a^{N_p} \end{bmatrix}$$

$$J = (R_s - Y)^T (R_s - Y) + \Delta U^T \overline{R} \Delta U \qquad R_z^T = \begin{bmatrix} 1 & 1 & \cdots & 1 \end{bmatrix} r(k_i)$$

$$J = \begin{bmatrix} R_z - Fx(k_i) \end{bmatrix}^T \begin{bmatrix} R_z - Fx(k_i) \end{bmatrix} - 2\Delta U^T \Phi^T (R_z - Fx(k_i)) + \Delta U^T (\Phi^T \Phi + \overline{R}) \Delta U$$

To find the minimum without constraints

$$\begin{split} &\frac{\partial J}{\partial \Delta U} = -2\Phi^T \left[R_z - Fx(k_i) \right] + 2 \left[\Phi^T \Phi + \overline{R} \right] \Delta U = 0 \\ \Rightarrow \Delta U = \left(\Phi^T \Phi + \overline{R} \right)^{-1} \Phi^T \left(R_z - Fx(k_i) \right) \end{split}$$

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To continue:

- Read chapters 1 and 2 in Wang's book to become convenient with one formalism.
- The rest of Wang's book is interesting and useful. To continue studies in MPC, I would start from it.

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$$\min_{\Delta u_{k|k}...\Delta u_{k+N_{u}|k}} J,$$
s.t. $A_{ineq}\Delta U \leq b_{ineq}$

leads to a numerical optimization problem, for which efficient algorithms exist.

Note that the idea has been to formulate the whole MPC problem such that it can be solved by general optimization software. See e.g. the command *quadprog* in Matlab. Using a special MPC toolbox is possible of course, but it is impossible to see "inside" what it really does.

