

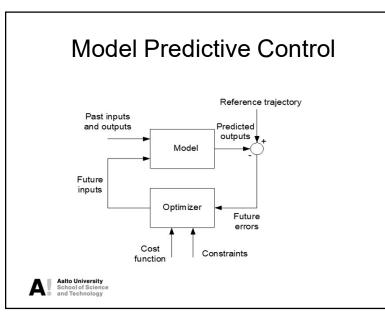


Model Predictive Control

- · Can deal with constraints in a natural way
- · The basic idea is easy to understand
- · It extends to multivariable plants naturally
- Generally more powerful than traditional PID control
- Integrates optimal control, stochastic control, control of processes with dead-time, multivariable control, control that can handle constraints.
- A practical methodology, which has numerous technical applications, especially in the process industry.
- It was earlier neglected and critisized by the control engineering community (lack of stability proofs, robustness etc.); this situation has changed due to progress in theory.



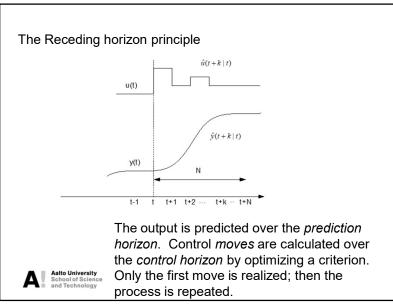
5



The main characteristics in MPC

- An *internal model* capable of fast simulation
- A *reference trajectory* which defines the desired closed-loop behaviour
- The *receding horizon* principle
- Future *input trajctory* by a finite number of *control moves*
- On-line optimization (possibly constrained)

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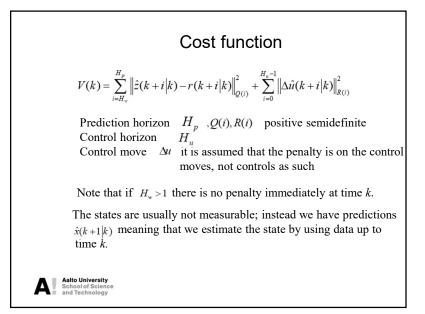


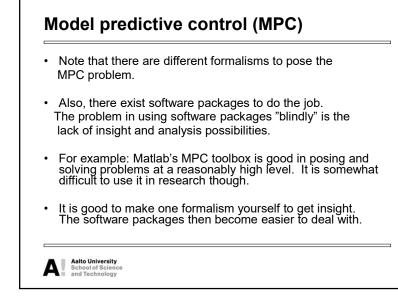
 A lot of different formulations can be found in the literature (MPHC, MAC, DMC, EHAC, EPSAC, GPC etc. etc.)

 Maciejowski's book has information on commercial MPC products, e.g. DMCPlus, RMPCT, Connoisseur, PFC, HIECON, 3dMPC, Process Perfecter.

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9





10

Features of constrained predictive control

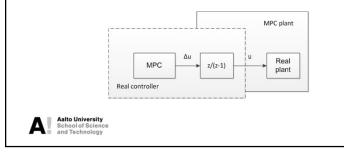
- Constraints cause MPC be *nonlinear*. But most of the time (when constraints are not near to be active) the controller operates in a linear way.
- In practice, meeting a hard constraint can be dangerous for the system. An MPC might do hazardous actions (in "panic"); usually a supervisory mode is used to prevent such actions.
- We consider only *time-invariant* MPC. The system has then constant coefficient matrices. In

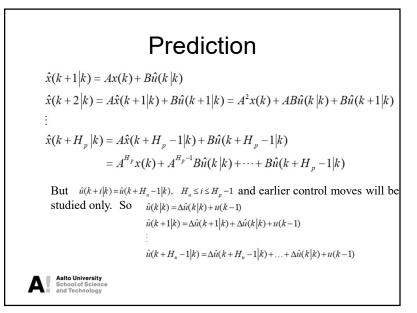
$$\mathcal{V}(k) = \sum_{i=H_{n}}^{H_{p}} \left\| \hat{z}(k+i|k) - r(k+i|k) \right\|_{\mathcal{Q}(i)}^{2} + \sum_{j=0}^{H_{n}-1} \left\| \Delta \hat{u}(k+i|k) \right\|_{\mathcal{R}(j)}^{2}$$

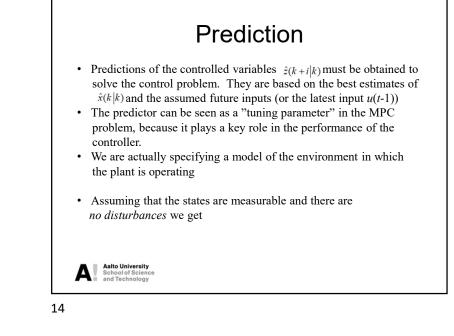
Q(i) and R(i) can vary with i , but they must not change with k Auto University School of Science and Technology

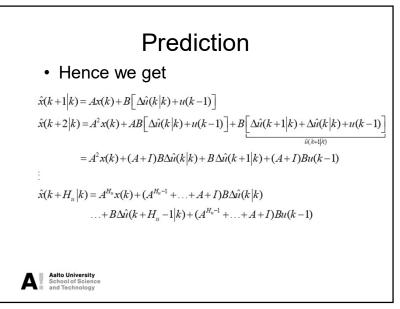
Alternative state variable choices

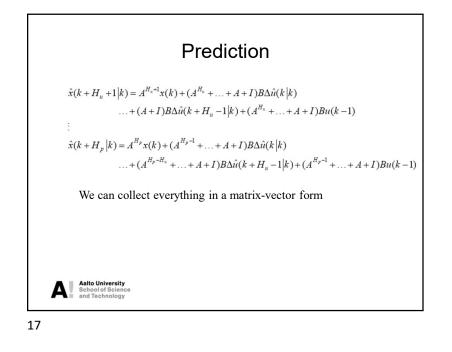
• Usually the MPC gives the *control move* as its output, whereas the project model uses absolute values. The *integration* in the state space model is then needed (to create *u* from Δu

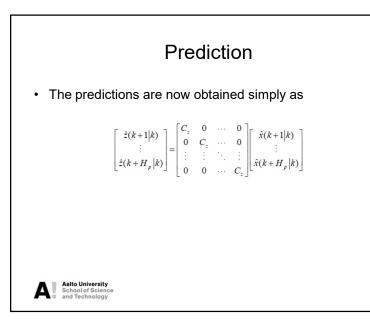


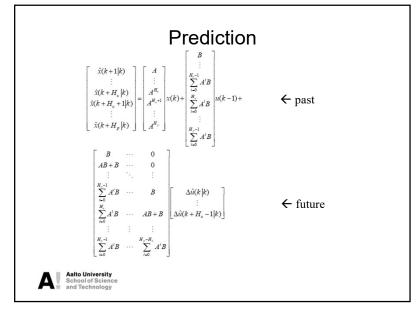


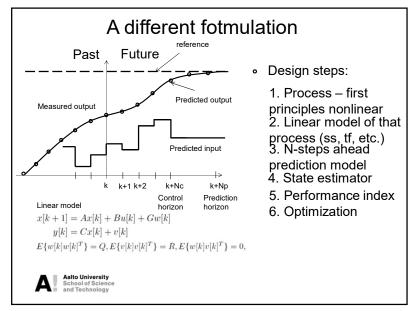


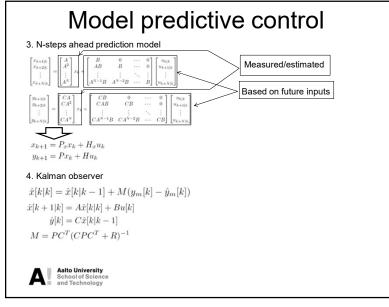


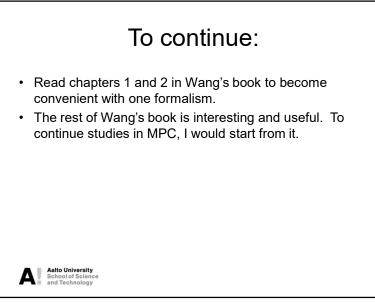


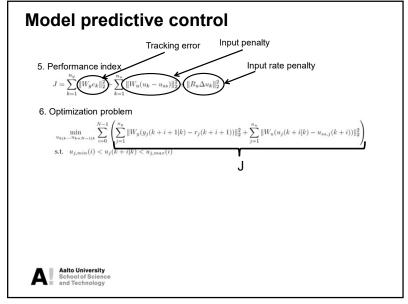












22

The formalism in Wang's book

Process model

 $\dot{x}_m(t) = Ax_m(t) + Bu(t)$ $y(t) = Cx_m(t)$

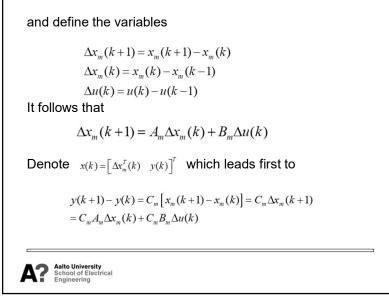
Discretized form

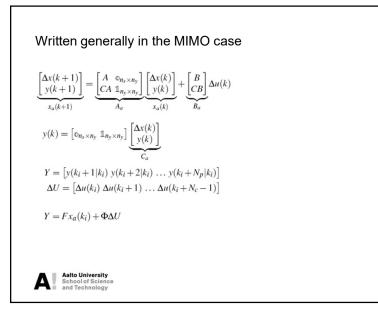
 $x_m(k+1) = A_m x_m(k) + B_m u(k)$ $y(k) = C_m x_m(k)$

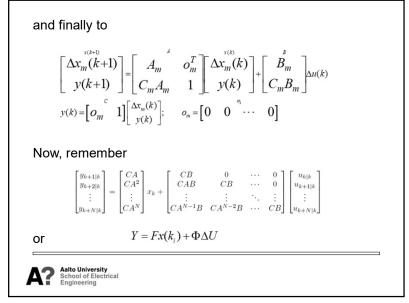
Form the difference

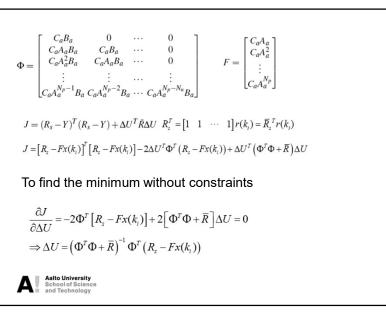
$$x_m(k+1) - x_m(k) = A_m[x_m(k) - x_m(k-1)] + B_m[u(k) - u(k-1)]$$

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• Generally (with constraints)

```
\min_{\substack{\Delta u_{k|k}...\Delta u_{k+N_{u}|k}}} J,
s.t. A_{ineq}\Delta U \leq b_{ineq}
```

leads to a numerical optimization problem, for which efficient algorithms exist.

Note that the idea has been to formulate the whole MPC problem such that it can be solved by general optimization software. See e.g. the command *quadprog* in Matlab. Using a special MPC toolbox is possible of course, but it is impossible to see "inside" what it really does.



29

