

EEN-E2001 Computational Fluid Dynamics

# Lecture 2: Gauss' Theorem and Finite Volume Method

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January 22<sup>nd</sup> 2024

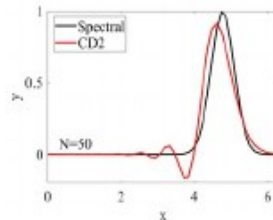
Aalto University, School of Engineering

**Lecture 1:** Linear PDEs and finite difference method

HW1

$$\frac{\partial T}{\partial t} + \nabla \cdot T \mathbf{u} = \alpha \nabla^2 T$$

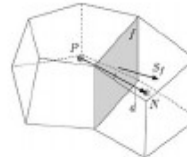
$$\frac{\partial T}{\partial x} \approx \frac{T_{i+1} - T_{i-1}}{2\Delta x}$$



**Lecture 2:** Gauss' theorem and finite volume method

$$\int_{\Omega} \nabla \cdot (T \mathbf{u}) d\Omega = \int_{\partial\Omega} (T \mathbf{u}) \cdot \mathbf{n} dS$$

$$\int_{\partial\Omega} \mathbf{u} \cdot \mathbf{n} dS \approx \sum_f \mathbf{u}_f \cdot \mathbf{n}_f dS_f$$

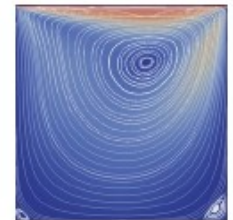


**Lecture 3:** Navier-Stokes equation and pressure

HW2

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla \cdot \mathbf{u} \mathbf{u} = -\nabla p + \nu \nabla^2 \mathbf{u}$$

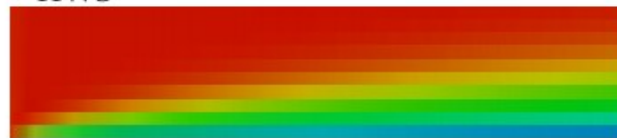
$$-\nabla^2 p = \nabla \cdot \nabla \cdot \mathbf{u} \mathbf{u}$$



**Lecture 4:** OpenFOAM code and structure

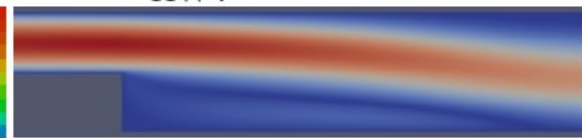
HW3

```
fvVectorMatrix UEqn
{
    fvm::ddt(U)
    + fvm::div(phi, U)
    - fvm::laplacian(nu, U)
};
```



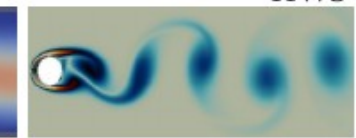
**Lecture 5:** Fluid physical phenomena: (laminar and turbulent flow)

HW4



**Lecture 6:** Matrix equations  $Ax=b$  and final assignment

HW5



# Intended learning objectives of the full lecture

## After the lecture the student:

- Can explain connection between Gauss' theorem and the finite volume method (fvm)
- Can write down & derive the fvm discretized 1d convection-diffusion problem (relevance: HW2)

In fact, Gauss (left) and Newton (right) developed much of the mathematics and physics tools & thinking that we use nowadays in our CFD simulations

[https://en.wikipedia.org/wiki/Carl\\_Friedrich\\_Gauss](https://en.wikipedia.org/wiki/Carl_Friedrich_Gauss)

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[https://en.wikipedia.org/wiki/Isaac\\_Newton](https://en.wikipedia.org/wiki/Isaac_Newton)

[https://en.wikipedia.org/wiki/File:Portrait\\_of\\_Sir\\_Isaac\\_Newton,\\_1689.jpg](https://en.wikipedia.org/wiki/File:Portrait_of_Sir_Isaac_Newton,_1689.jpg)



CFD simulation and PDE solution includes at least the following aspects covered on the course

- 1) **Physics** identification.
- 2) **Mathematical equations and physics interpretation.**  
Boundary/initial conditions.
- 3) **Objectives, feasibility, and time-constraints.**
- 4) **Numerical method and modeling assumptions.**
- 5) **Geometry and mesh generation.**
- 6) **Computing** i.e. running simulation.
- 7) **Visualization and post-processing.**
- 8) **Validation and verification, reference data.** Reporting, analysis and discussion of the results. Are the results sane?

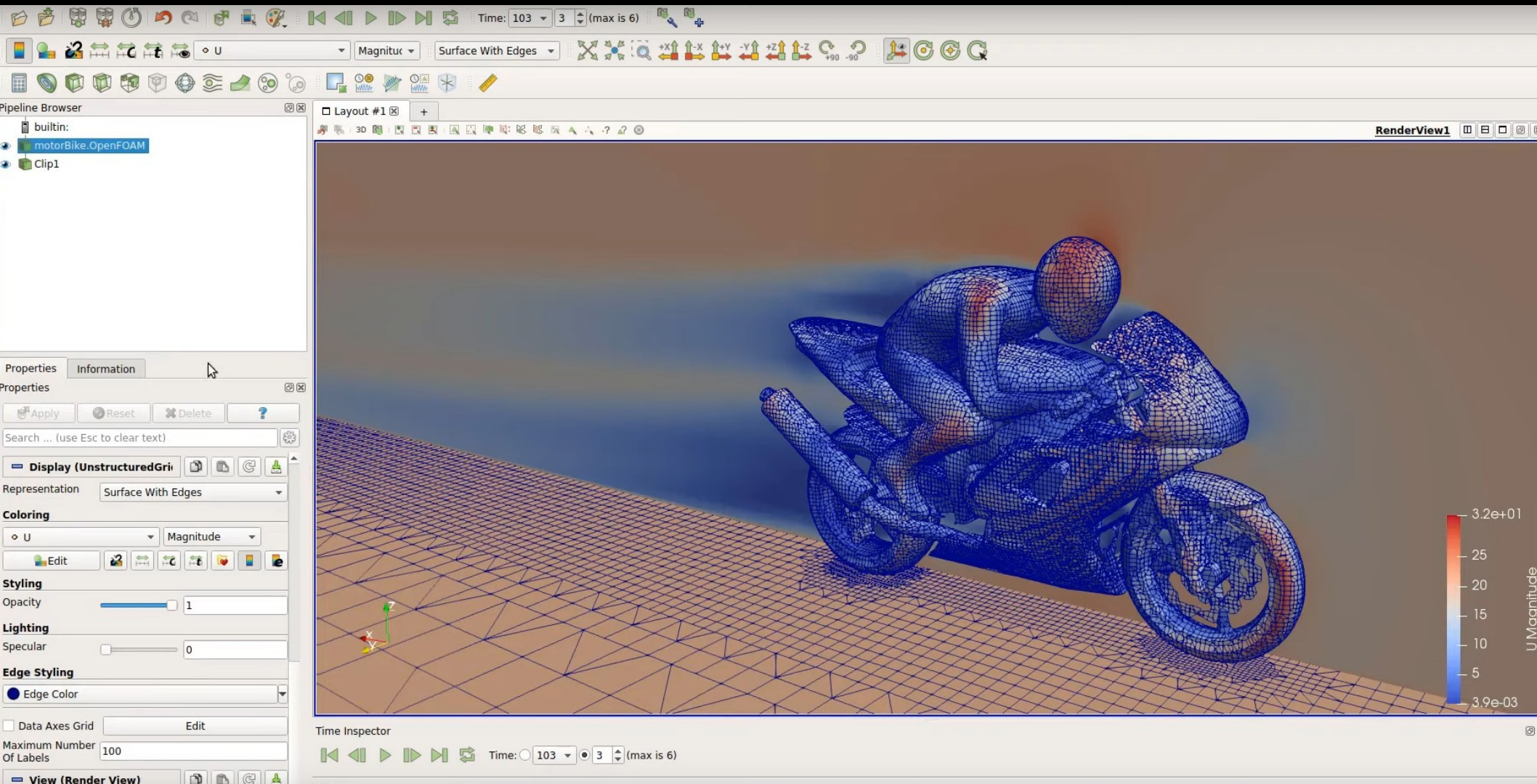
# **Example applications on finite volume method CFD simulations**



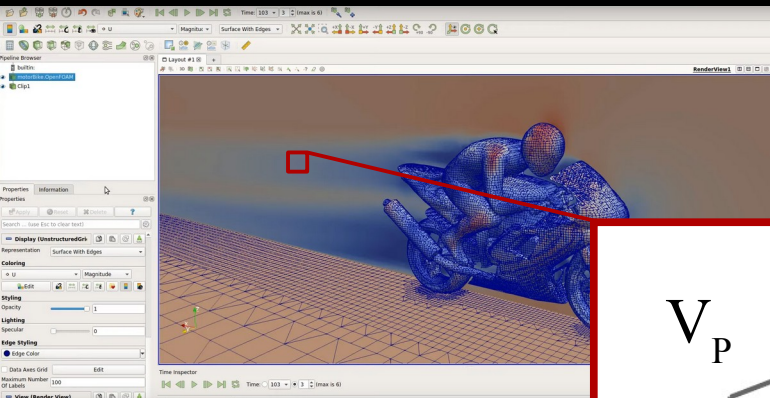
# Visual example: Aerodynamics CFD simulation using the finite volume method (OpenFOAM)

The Motorbike tutorial and steady state velocity field

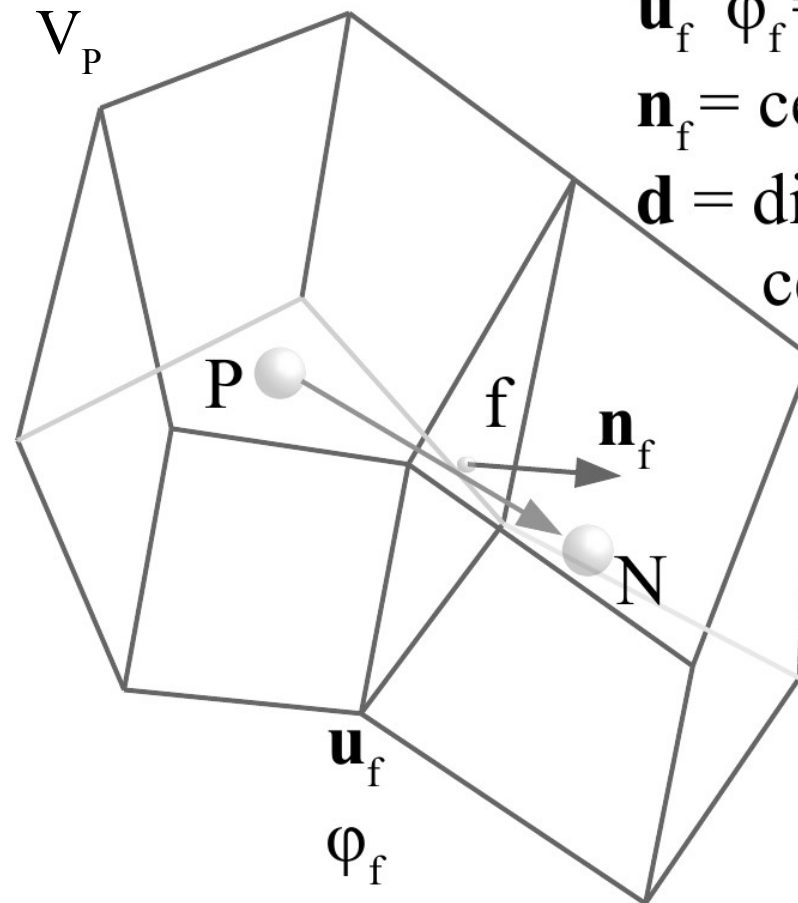
[https://www.youtube.com/watch?v=1C4Av\\_yCfpw&list=RDCMUCDuQsPzfqxcYKVp\\_uuKCzqw&start\\_radio=1&rv=1C4Av\\_yCfpw&t=6](https://www.youtube.com/watch?v=1C4Av_yCfpw&list=RDCMUCDuQsPzfqxcYKVp_uuKCzqw&start_radio=1&rv=1C4Av_yCfpw&t=6)



**Basic idea of finite volume method:** divide geometry into small volumes and update numerical solution at **volume centroids** by estimating e.g. **mass & momentum fluxes** through the **faces** of the **control volumes** during small time intervals



## Control volume



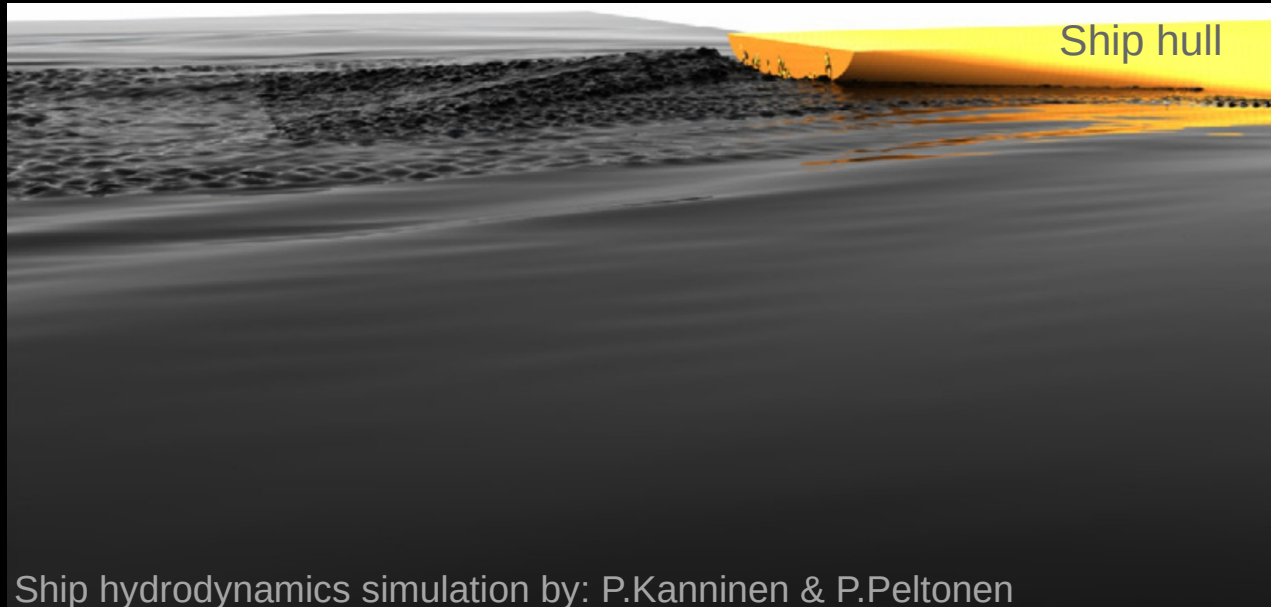
$\mathbf{u}_f$   $\phi_f$  = cell face interpolants

$\mathbf{n}_f$  = cell face normal vector

$\mathbf{d}$  = distance vector between cell centroids  $P$  and  $N$

# Visual research examples: recent high-performance computing applications using finite volume method (OpenFOAM) in my team

<https://www.sciencedirect.com/science/article/abs/pii/S0029801821017194?via%3Dihub>



Velocity

$$\vec{u} = \vec{u}(x, y, z, t)$$

Concentration

$$c = c(x, y, z, t)$$

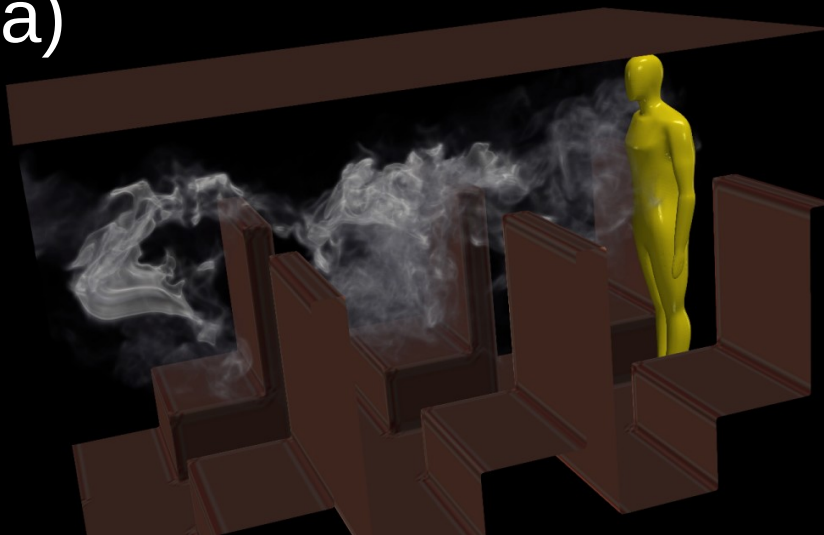
Convection-Diffusion eqn

$$\frac{\partial c}{\partial t} + \vec{u} \cdot \nabla c = \alpha \nabla^2 c$$

Navier-Stokes (Newton's 2<sup>nd</sup> law)

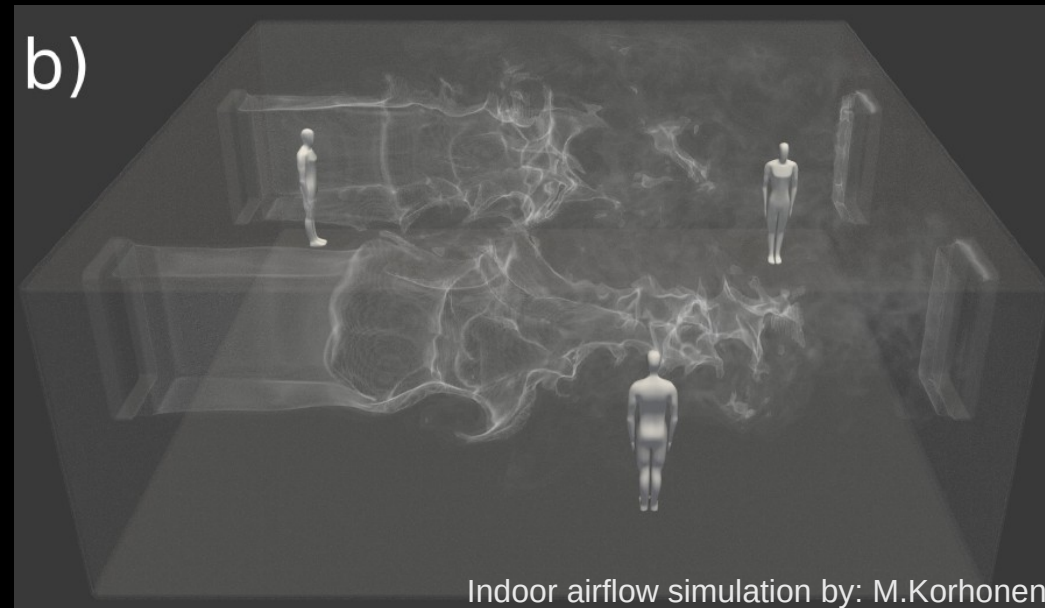
$$\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} = -\nabla p + \nu \nabla^2 \vec{u}$$

a)



Indoor airflow simulation by: V.Vuorinen. Visualization: M.Gadalla

b)



Indoor airflow simulation by: M.Korhonen



# “Computational cost” depends on numerous aspects:

Type of software, computing infrastructure, how long can you wait, method, resolution, how long we need to simulate physical time, steady vs transient, physics (e.g. refinement need at boundary layers/wakes), what is the intention of the simulation (e.g. visualization of known physics, quick design insight, exact matching of an experiment with publication quality) etc

Case	Resolution	Computational cost	Method	Comment
<b>Motorbike</b>	Very coarse ~0.1M cells	~ <b>1 min</b> (Laptop CPU)	Steady state RANS - method	A basic tutorial. Intention: demo
<b>Airflow in a room</b>	Medium ~30M cells	~ <b>2 days</b> (GPU)	Transient LES method	To be submitted to a journal.
<b>Ship hydro</b>	Medium ~60M cells	~ <b>10 days</b> (Supercomputer)	Transient LES method	Published in a journal.

# Finite volume method in a nutshell

**The core problem in solving convection-diffusion type equations (PDE's):**

In CFD, we would like to find a  $\Delta\phi = \Delta t(-C+D)$  to update solution as  $\phi_{n+1} = \phi_n + \Delta\phi$ .

→ Need to numerically calculate divergence terms i.e. convection  $C=C(x,y,z,t)$  & diffusion  $D=D(x,y,z,t)$  ( $t=n\Delta t$ ).

$$C = \nabla \cdot (\mathbf{u}\phi)$$

$$D = \alpha \nabla \cdot \nabla \phi$$

**Gauss' theorem:** enables converting volume integrals into surface integrals (B.Sc. math)

$$\int_V \nabla \cdot (\mathbf{u}\phi) dV = \int_A (\mathbf{u}\phi) \cdot \mathbf{n} dA$$

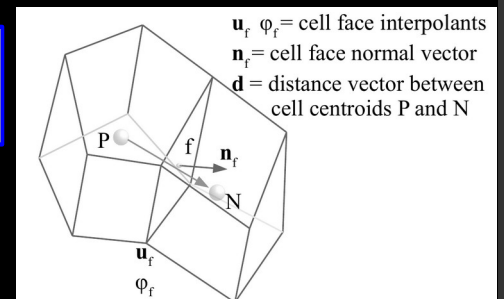
$dA$  = differential area element on the outer surface  $A$  of volume  $V$

$\mathbf{n}$  = the surface outer normal vector

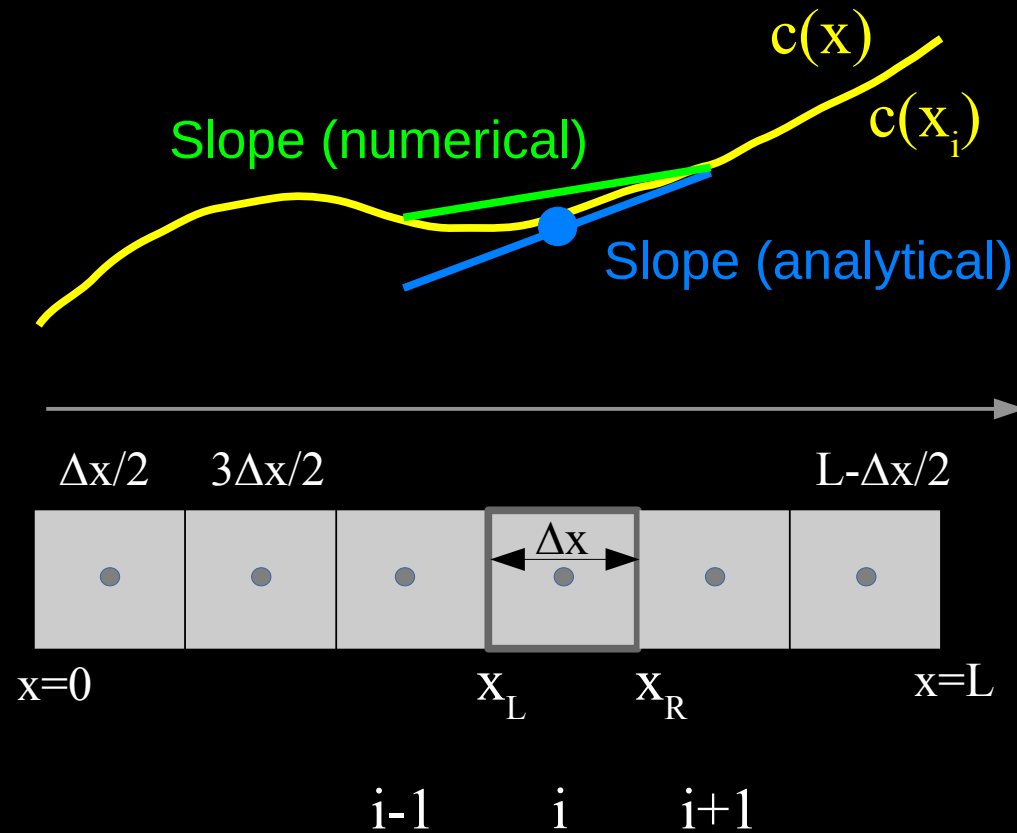
**Gauss' theorem + volume averaging:** divergence terms  $C$  and  $D$  can be converted into surface integrals which can be numerically computed via summations.

$$C_{ave} = \frac{1}{V} \int_V \nabla \cdot (\mathbf{u}\phi) dV = \frac{1}{V} \int_A (\mathbf{u}\phi) \cdot \mathbf{n} dA \approx \frac{1}{V} \sum_{faces} (\mathbf{u}_f \phi_f) \cdot \mathbf{n}_f dA_f$$

$$D_{ave} = \frac{1}{V} \int_V \alpha \nabla \cdot \nabla \phi dV = \frac{1}{V} \int_A \nabla \phi \cdot \mathbf{n} dA \approx \frac{1}{V} \sum_{faces} \nabla \phi_f \cdot \mathbf{n}_f dA_f$$



**Recall:** discretization methods (FDM, FVM, FEM) needed to numerically calculate space derivatives appearing in PDE's  
 (derivative = slope of the function)



E.g. with CD2/FD:  $c'(x_i) = \frac{\partial c}{\partial x} \approx \frac{c_{i+1} - c_{i-1}}{2\Delta x}$

Next, we derive fvm discretization for the derivative  $c'(x)$ .

Keywords: "volume averaging & Gauss' theorem"

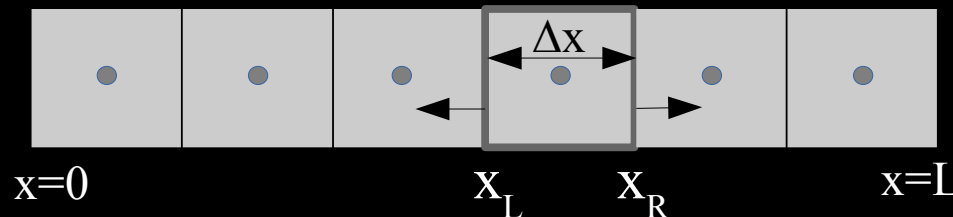
Let us integrate  $c'(x)$  over  $x_L < x < x_R$  ( $\Delta x = x_R - x_L$ ):

$$\int_{x_L}^{x_R} c'(x) dx = +c(x_R) - c(x_L)$$

To obtain "volume average" of  $c'(x)$ , divide both sides by  $\Delta x$ :

$$\frac{1}{\Delta x} \int_{x_L}^{x_R} c'(x) dx = \frac{+c(x_R) - c(x_L)}{\Delta x}$$

Volume average of  $c'(x)$  over  $\Delta x$       Looks essentially like CD2/FD



**Note:**

Cell face outer normal vectors point to  $(+1,0)$  and  $(-1,0)$  directions so actually the  $+/-$  signs in 1d integration originate from the Gauss' theorem.



This leads to a finite volume discretization formula for  $c'(x)$

Interpolating fluxes linearly  $c(x_L) = 0.5(c_i + c_{i-1})$  and  $c(x_R) = 0.5(c_i + c_{i+1})$  yields the fvm discretization:

$$\left(\frac{\partial c}{\partial x}\right)_{fvm} = \frac{1}{\Delta x} \int_{x_L}^{x_R} c'(x) dx = \frac{c(x_R) - c(x_L)}{\Delta x} = \frac{c_{i+1} - c_{i-1}}{2 \Delta x}$$

... being exactly the CD2/FD formula (week 1).

## Notes:

→ Averaging derivative over an interval (1d) or volume (3d) we can find finite volume discretization formulae. On uniform grids, and linear interpolation, FVM and FDM give exactly the same 2<sup>nd</sup> order central difference (CD2) formula (see: Week 1).

→ **Face interpolation** of  $c(x_L)$  and  $c(x_R)$  is **one of the most essential parts to pay attention on in CFD** (the numerical uncertainty and error contained in the interpolation details). In HW1 you will compare three interpolation procedures: linear (CD2) vs upwind (UW1) vs a flux limiter. Flux limiters “try” to be as close to CD2 but still diffusive enough to stabilize the numerical solution.

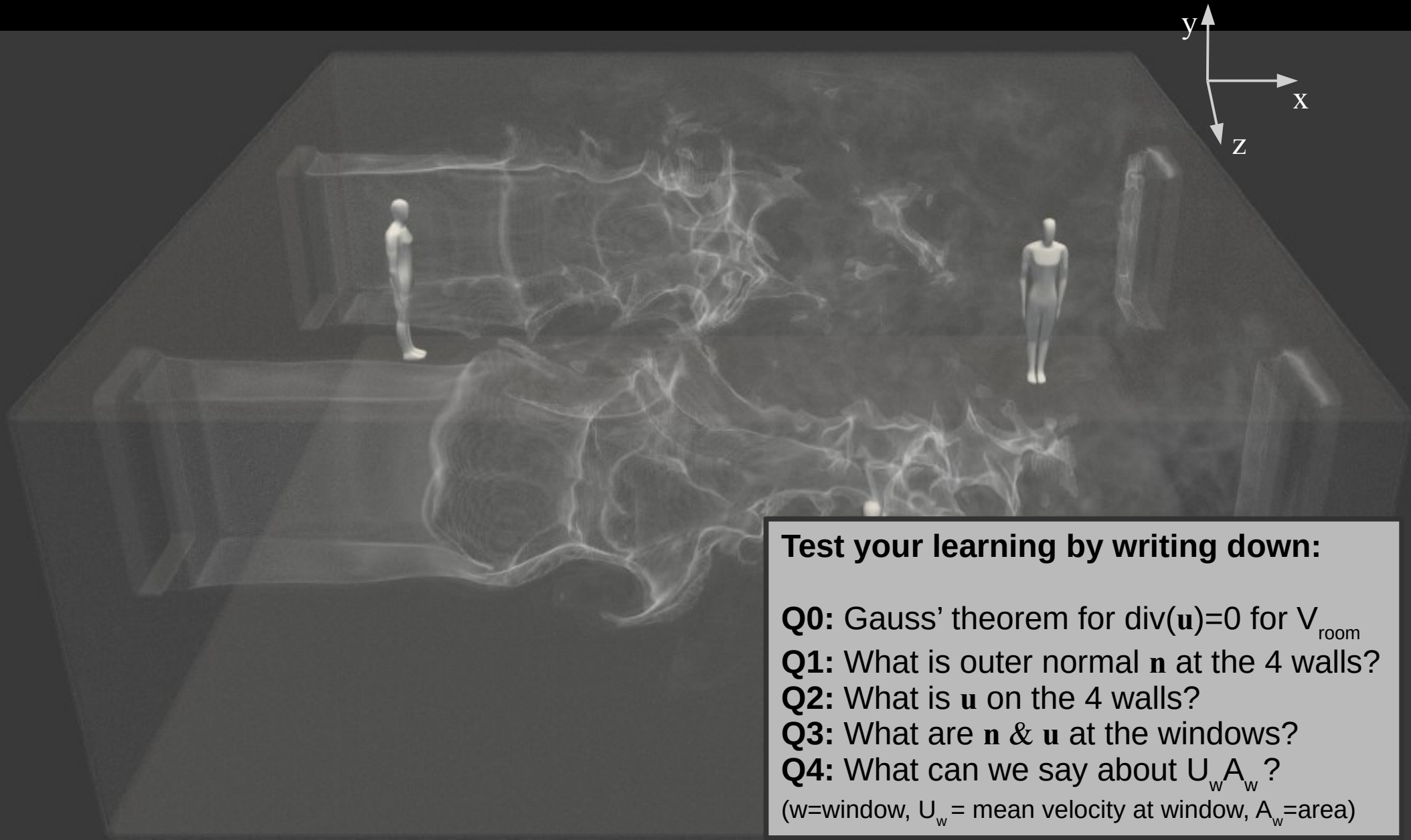
**Recap discussions:** Gauss' theorem, conservation of mass and a room with cross-draught. Flow enters 1m/s from the left windows and exits from right. Window area = constant.

[https://www.youtube.com/watch?v=Pf7hgOkjd\\_w](https://www.youtube.com/watch?v=Pf7hgOkjd_w)



**Basic fluid dynamics (M.Sc.):** Velocity field of incompressible fluids, such as low speed air and water, satisfies the mass conservation equation:

$$\nabla \cdot \vec{u} = 0$$



**Test your learning by writing down:**

- Q0:** Gauss' theorem for  $\text{div}(\mathbf{u})=0$  for  $V_{\text{room}}$   
**Q1:** What is outer normal  $\mathbf{n}$  at the 4 walls?  
**Q2:** What is  $\mathbf{u}$  on the 4 walls?  
**Q3:** What are  $\mathbf{n}$  &  $\mathbf{u}$  at the windows?  
**Q4:** What can we say about  $U_w A_w$ ?  
( $w$ =window,  $U_w$  = mean velocity at window,  $A_w$ =area)

Gauss theorem + mass conservation:

$$\int_{V_{\text{room}}} \nabla \cdot \vec{u} dV = \int_{A_{\text{room}}} \vec{u} \cdot \vec{n} dA = 0$$





# **Finite volume method for the 1d convection-diffusion equation**

**(relevance: small theory question in HW2)**

$$\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} = -\nabla p + \nu \nabla^2 \vec{u}$$

$$\frac{\partial c}{\partial t} + \vec{u} \cdot \nabla c = \alpha \nabla^2 c$$

$$\vec{u} = \vec{u}(x, y, z, t)$$

$$c = c(x, y, z, t)$$

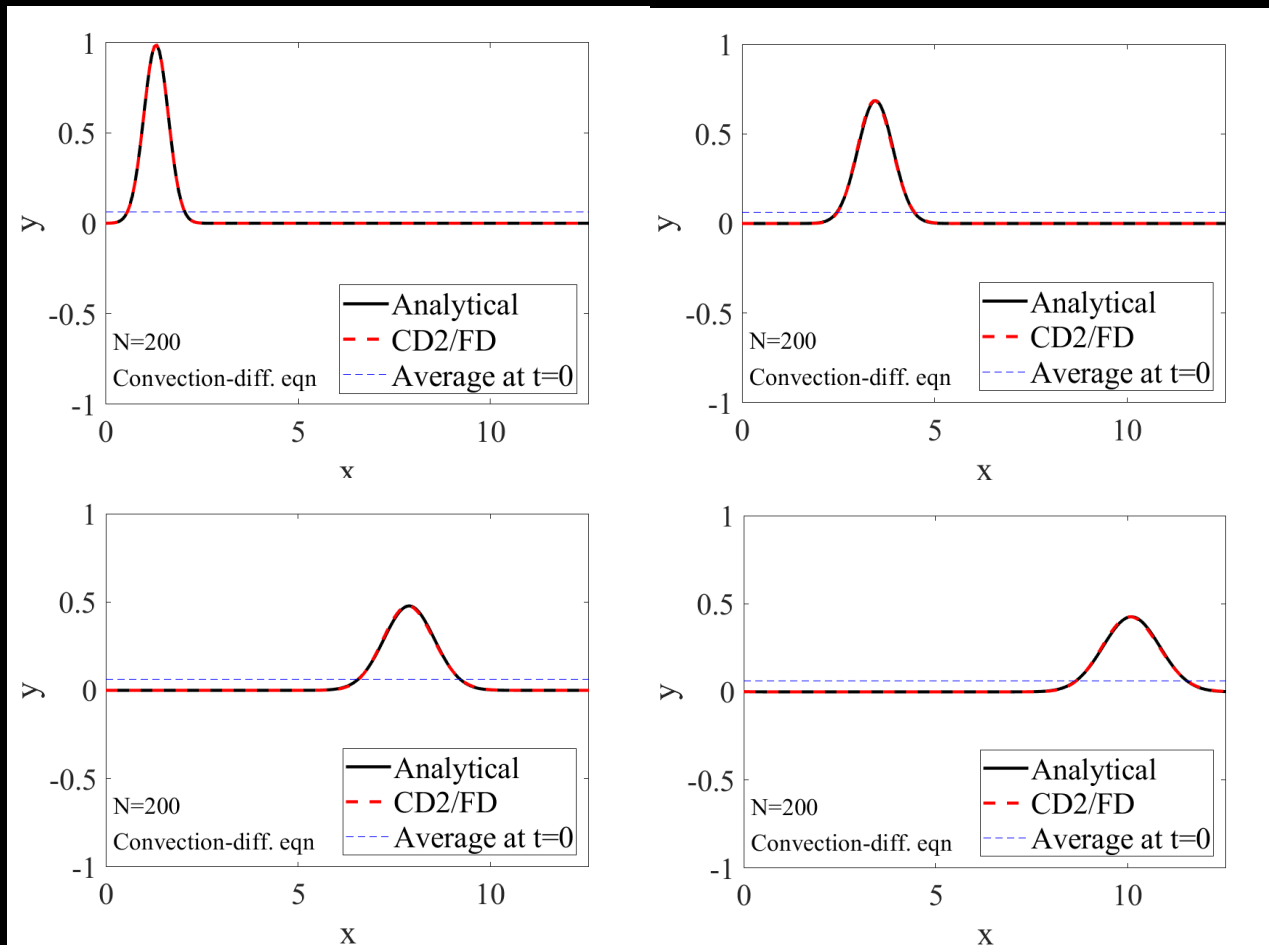
# 3D smoke cloud moving in air



Let us model the smoke cloud motion in a simple way using the 1D convection-diffusion equation ( $u=\text{constant}$ )

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = \alpha \frac{\partial^2 c}{\partial x^2}$$

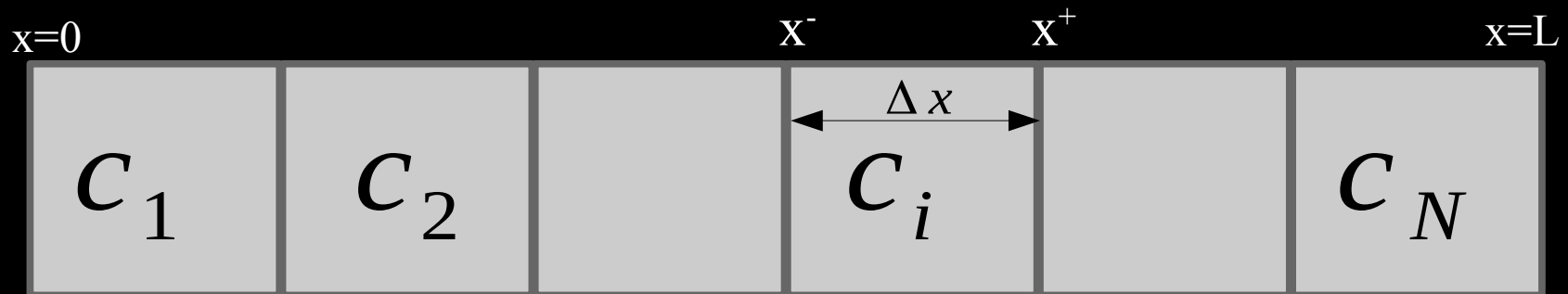
$c$ =smoke concentration  
 $\alpha$ =diffusivity [ $\text{m}^2/\text{s}$ ]  
 $u$ =mean wind velocity [ $\text{m}/\text{s}$ ]



We average the 1d CD-eqn over finite intervals of length  $\Delta x$ .

**Definition:** average of a function in 1d over the interval  $\Delta x$

$$f_{ave} = \frac{1}{\Delta x} \int_{\Delta x} f dx$$



Averaged CD-eqn over the interval  $\Delta x$

$$\frac{1}{\Delta x} \int_{x^-}^{x^+} \frac{\partial c}{\partial t} dx + \frac{1}{\Delta x} \int_{x^-}^{x^+} u \frac{\partial c}{\partial x} dx = \frac{1}{\Delta x} \int_{x^-}^{x^+} \alpha \frac{\partial^2 c}{\partial x^2} dx$$



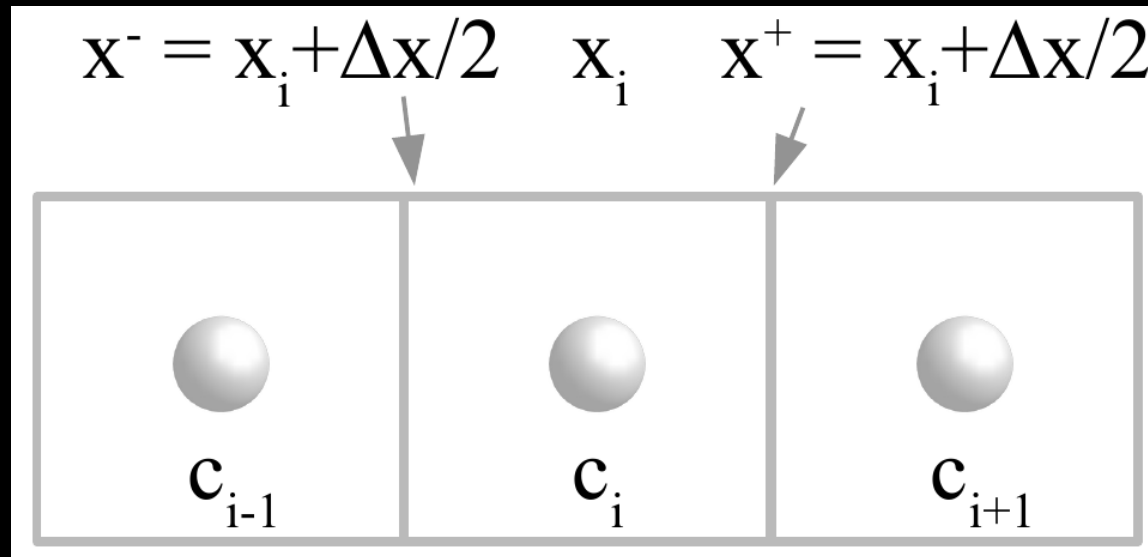
We average the 1d CD-eqn over a finite interval of length  $\Delta x$ .

Assuming  $\Delta x$  is small, we assume:

$$c \approx \frac{1}{\Delta x} \int_{x^-}^{x^+} c dx$$

The resulting form:

$$\frac{\partial c}{\partial t} + u \frac{c(x^+, t) - c(x^-, t)}{\Delta x} = \alpha \left[ \frac{\partial c(x^+, t)}{\partial x} - \frac{\partial c(x^-, t)}{\partial x} \right] \frac{1}{\Delta x}$$



# Estimation of quantities at the cell face

The terms below require **interpolation** of  $c$  to the cell face from adjacent cells

$$c(x^+), c(x^-)$$

The terms below require **estimation of the gradients** of  $c$  on the cell face

$$\alpha \frac{\partial c(x^+)}{\partial x}, \alpha \frac{\partial c(x^-)}{\partial x}$$

**How could we get those values ?**

→ On uniform grid one could simply linearly **interpolate**

$$c(x^+) \approx 0.5(c_{i+1} + c_i)$$

$$c(x^-) \approx 0.5(c_i + c_{i-1})$$

$$\alpha \frac{\partial c(x^+)}{\partial x} \approx \alpha \frac{c_{i+1} - c_i}{\Delta x}$$

$$\alpha \frac{\partial c(x^-)}{\partial x} \approx \alpha \frac{c_i - c_{i-1}}{\Delta x}$$

Gathering the interpolants into the cell averaged equations and discretizing time with Euler method gives...

$$\frac{\partial c}{\partial t} + u \frac{c(x^+, t) - c(x^-, t)}{\Delta x} = \alpha \left[ \frac{\partial c(x^+, t)}{\partial x} - \frac{\partial c(x^-, t)}{\partial x} \right] \frac{1}{\Delta x}$$



$$\frac{c_i^{n+1} - c_i^n}{\Delta t} + u \frac{c_{i+1}^n - c_{i-1}^n}{2 \Delta x} = \alpha \frac{c_{i+1}^n - 2c_i^n + c_{i-1}^n}{\Delta x^2}$$



$$c_i^{n+1} = c_i^n - \Delta t u \frac{c_{i+1}^n - c_{i-1}^n}{2 \Delta x} + \alpha \Delta t \frac{c_{i+1}^n - 2c_i^n + c_{i-1}^n}{\Delta x^2}$$

**Observation:** Finite volume method boils down to the finite difference method (week 1) on uniform grids.

**Numerical stability:** Courant number (Co) and Courant-Friedrichs-Lewy (CFL) number should be below one.

Co is relevant to the stability of the convection term (e.g. velocity is not allowed to transport over distances larger than grid spacing during timestep)

$$Co = \frac{\Delta t u}{\Delta x} < 1$$

CFL is relevant to the stability of the diffusion term (e.g. concentration is not allowed to diffuse over distances larger than grid spacing during timestep)

$$CFL = \frac{\Delta t \alpha}{\Delta x^2} < 1$$