

EEN-E2001 Computational Fluid Dynamics

Lecture 5: Fluid physical phenomena

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February 12th 2024

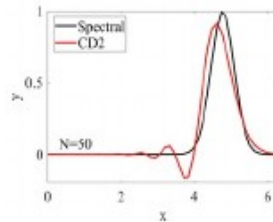
Aalto University, School of Engineering

Lecture 1: Linear PDEs and finite difference method

HW1

$$\frac{\partial T}{\partial t} + \nabla \cdot T \mathbf{u} = \alpha \nabla^2 T$$

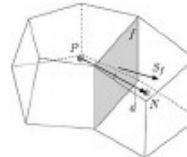
$$\frac{\partial T}{\partial x} \approx \frac{T_{i+1} - T_{i-1}}{2\Delta x}$$



Lecture 2: Gauss' theorem and finite volume method

$$\int_{\Omega} \nabla \cdot (T \mathbf{u}) d\Omega = \int_{\partial\Omega} (T \mathbf{u}) \cdot \mathbf{n} dS$$

$$\int_{\partial\Omega} \mathbf{u} \cdot \mathbf{n} dS \approx \sum_f \mathbf{u}_f \cdot \mathbf{n}_f dS_f$$

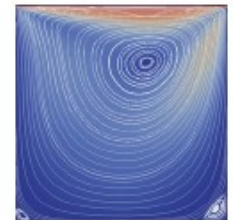


Lecture 3: Navier-Stokes equation and pressure

$$\frac{\partial \mathbf{u}}{\partial t} + \nabla \cdot \mathbf{u} \mathbf{u} = -\nabla p + \nu \nabla^2 \mathbf{u}$$

$$-\nabla^2 p = \nabla \cdot \nabla \cdot \mathbf{u} \mathbf{u}$$

HW2



Lecture 4: OpenFOAM code and structure

Lecture 5: Fluid physical phenomena: (laminar and turbulent flow)

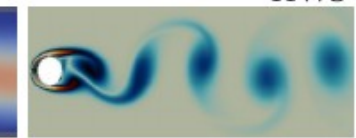
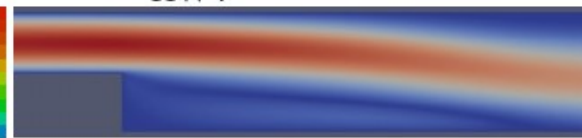
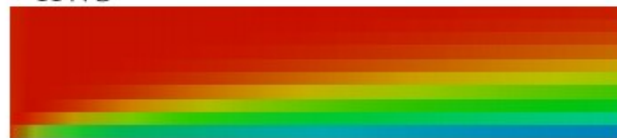
Lecture 6: Matrix equations $Ax=b$ and final assignment

HW3

HW4

HW5

```
fvVectorMatrix UEqn
(
    fvm::ddt(U)
    + fvm::div(phi, U)
    - fvm::laplacian(nu, U)
);
```



Intended learning objectives of the lecture

After the lecture the student:

- Can name basic fluid physical phenomena and connect them to HW3-HW5.

CFD simulation and PDE solution includes at least the following aspects covered on the course

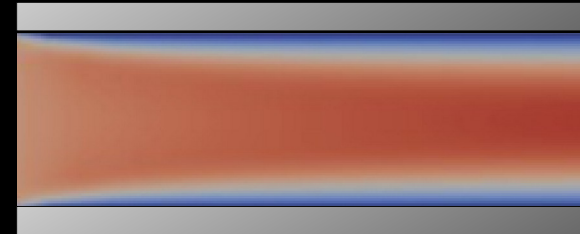
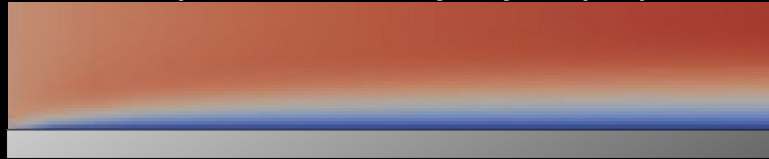
- 1) **Physics** identification.
- 2) **Mathematical equations and physics interpretation.**
Boundary/initial conditions.
- 3) **Objectives, feasibility, and time-constraints.**
- 4) **Numerical method and modeling assumptions.**
- 5) **Geometry and mesh generation.**
- 6) **Computing** i.e. running simulation.
- 7) **Visualization and post-processing.**
- 8) **Validation and verification, reference data.** Reporting, analysis and discussion of the results. Are the results sane?

Examples on physics phenomena in fluid dynamics

Steady, laminar flow. Key physics: diffusion builds up the BL structure

Channel flow

Free flat plate boundary layer (BL)

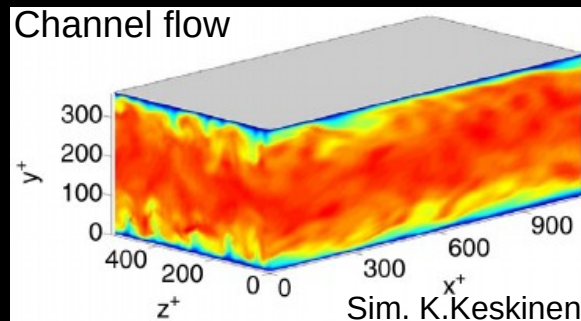


Unsteady, laminar flow. Key physics: von Karman instability and vortex shedding

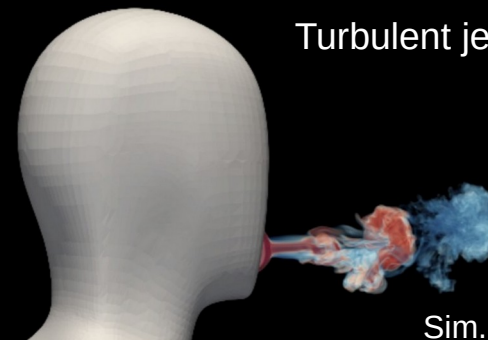


Unsteady, turbulent flow. Key physics: turbulence production at walls and shear layers

Channel flow



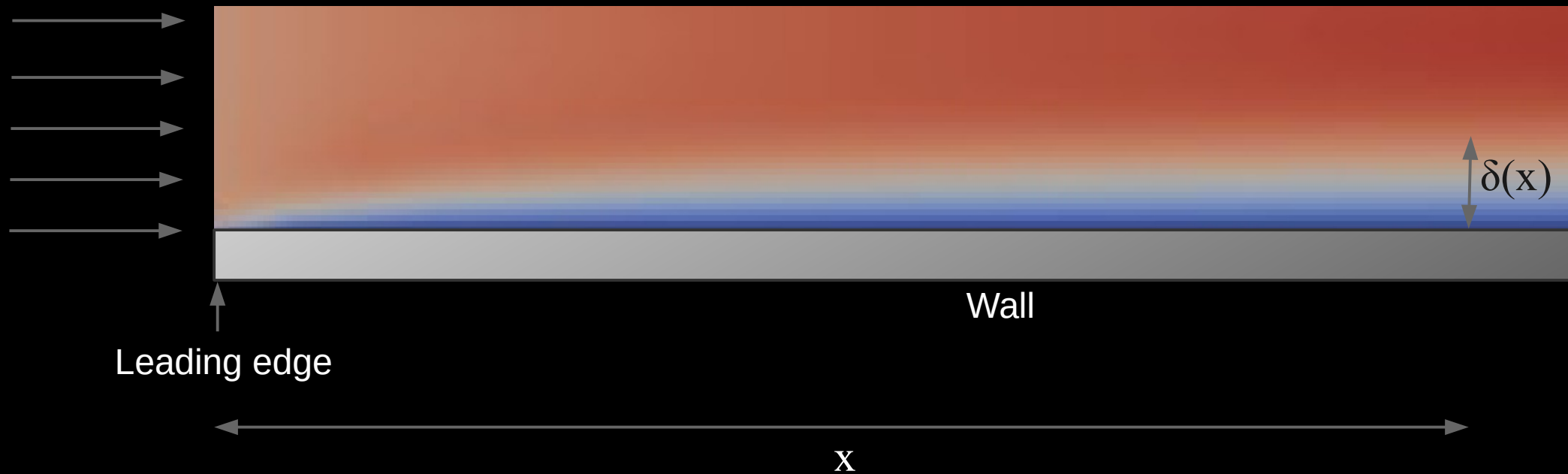
Turbulent jet



Free boundary layer

Relevance: HW3

Free boundary layer (relevance: HW3)



Recall: free boundary layer thickness grows as

$$\delta \approx 5.0 \sqrt{\frac{\nu x}{U_\infty}} = 5.0 x / \sqrt{\text{Re}_x}$$

$$\text{Re}_x = \frac{U_\infty x}{\nu}$$

Backward facing step flow

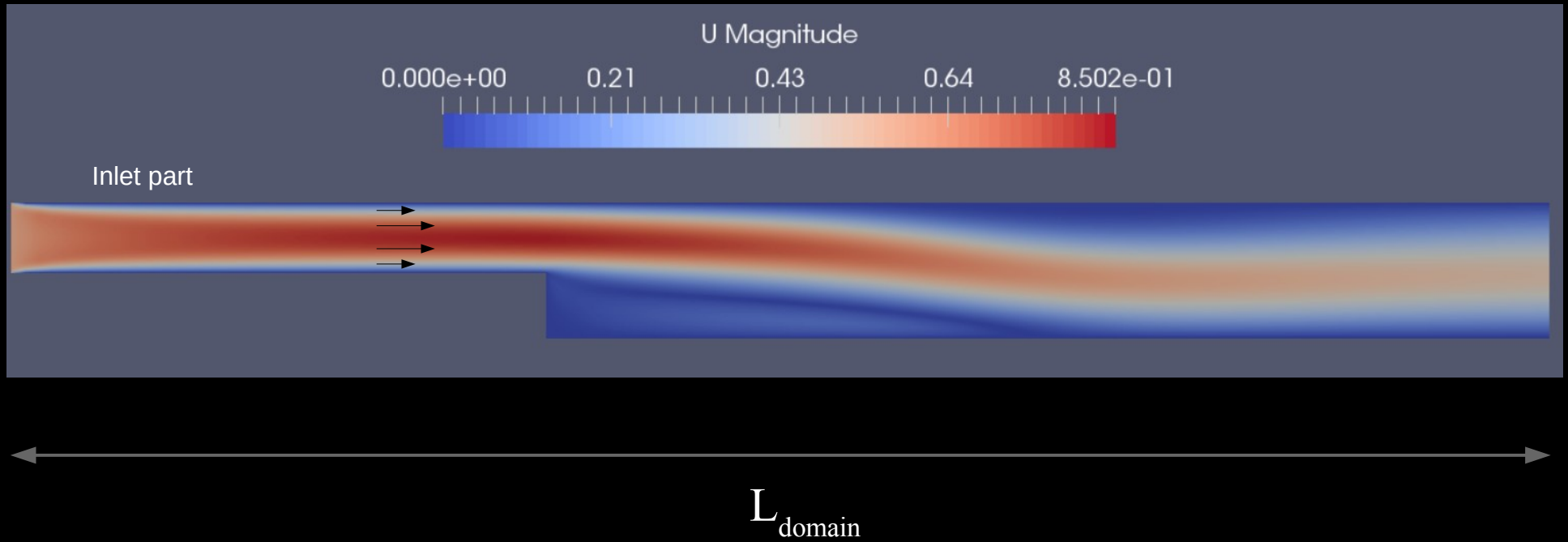
Relevance: HW3-HW4

Real world “Backward facing step”

By Ralf Roletschek (talk) - Fahrradtechnik auf fahrradmonteur.de - Own work, FAL, <https://commons.wikimedia.org/w/index.php?curid=15>



Backward facing step



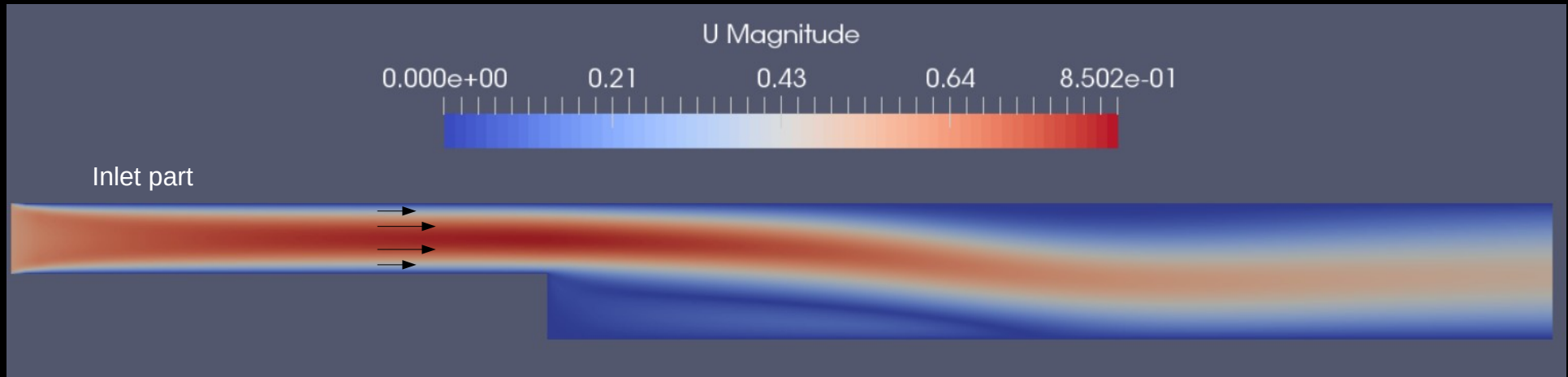
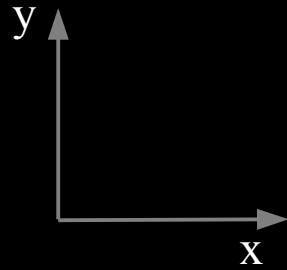
Backward facing step

Reynolds number:

$$Re = \frac{UD}{\nu}$$

Viscous entry length after which laminar channel flow fully developed:

$$L/D = 0.05 Re$$



1 2 3

Comment 1: constant velocity at inlet.

Comment 2: laminar boundary layer growth by viscous diffusion.

Comment 3: after viscous entry length, expect close to parabolic velocity profile $U=U(y)$.

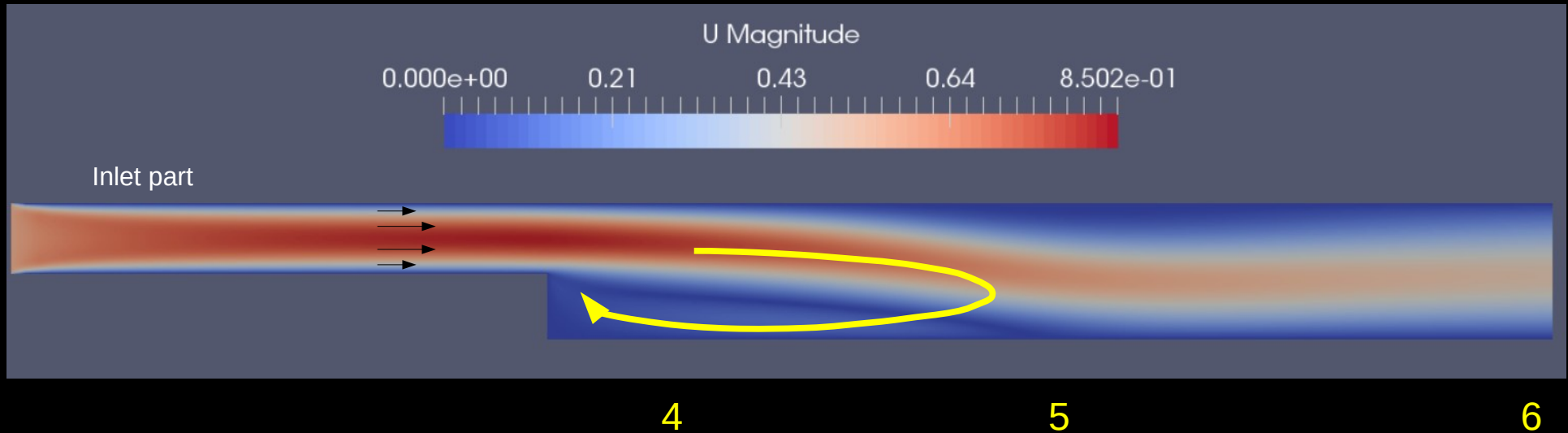
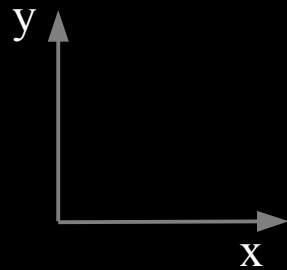
Backward facing step

Reynolds number:

$$Re = \frac{UD}{\nu}$$

Viscous entry length after which laminar channel flow fully developed:

$$L/D = 0.05 Re$$



Comment 4: flow recirculation zone (negative x-velocity).

Comment 5: stagnation point (x-velocity=0)

Comment 6: outlet (modeled commonly using `zeroGradient` or `InletOutlet bc` in OpenFOAM)

Important considerations

“Resolve”:

Space: put enough grid points to resolve the length scales (we can not take photos with 5*5 pixels).

Time: make timestep small enough. (Courant number, CFL number).

Resolve all the geometrical length scales:

channel height, step height, channel length, main chamber length/height.

Identify physics and refine grid accordingly:

- Laminar or turbulent.
- Turbulent flow: stricter space resolution requirement to resolve vortices of different size.
- Boundary layer thickness and near wall resolution (y^+ value) → necessary to understand in order to capture the wall shear stress (friction).
- Is there unsteady behavior e.g. vortex shedding? What is the oscillation frequency?

How long time should we simulate?

→ **Depends on the case but rough guidelines to start with:**

- Identify vortex turnaround time scale and simulate “at least tens of those time scales”
- Identify “flow through time scale” and simulate “at least a few of them”

Vortex turn-around time scale

$$\tau_{\text{vortex}} = \frac{d_{\text{vortex}}}{U_{\text{vortex}}}$$

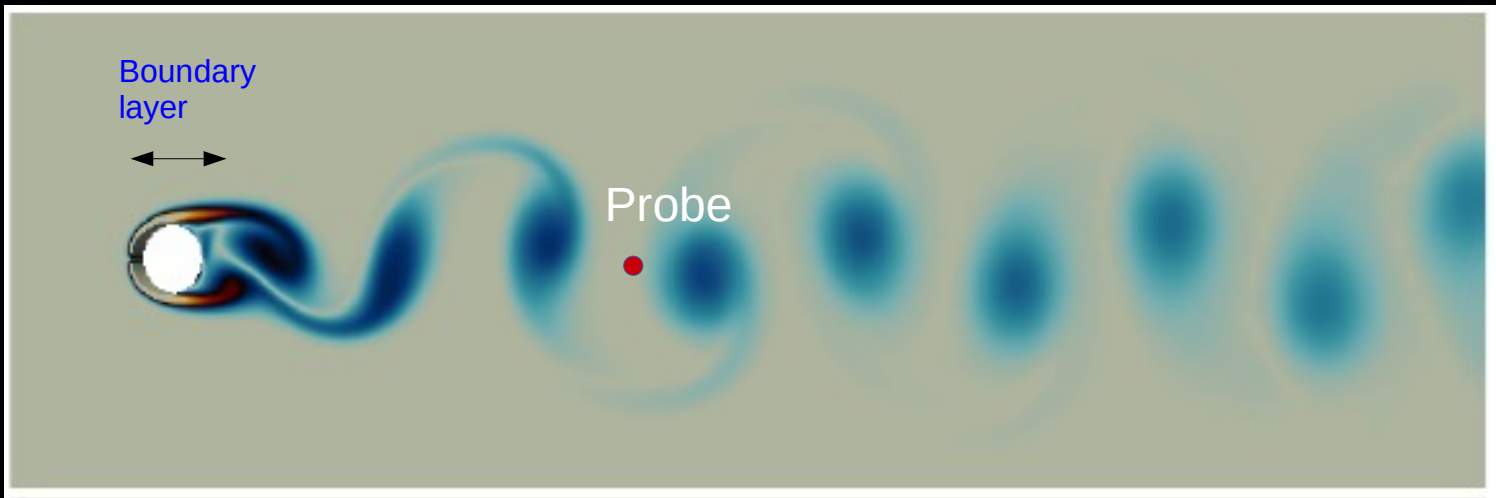
Flow through time scale

$$\tau_{\text{flow}} = \frac{L_{\text{domain}}}{U}$$

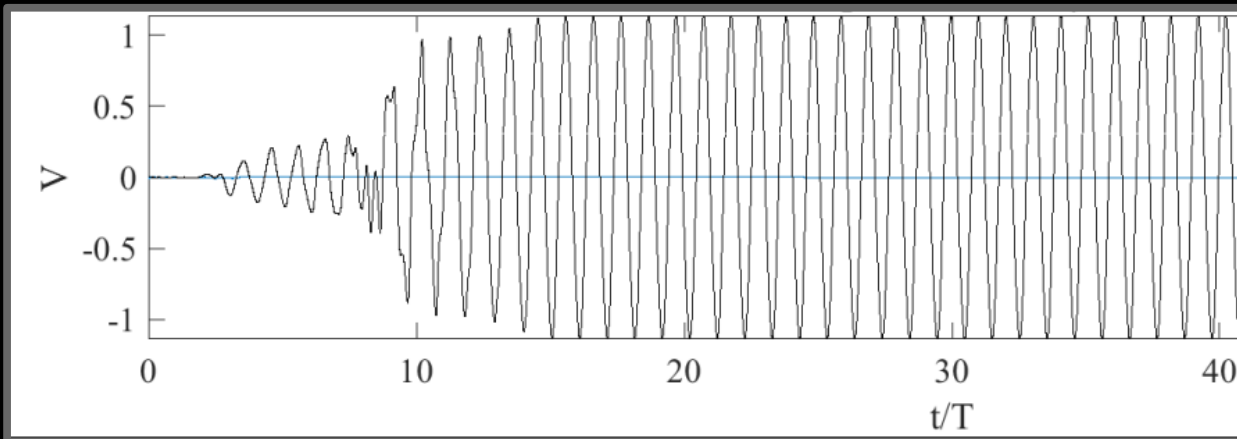
Flow over a cylinder

Relevance: HW5

Flow over a cylinder



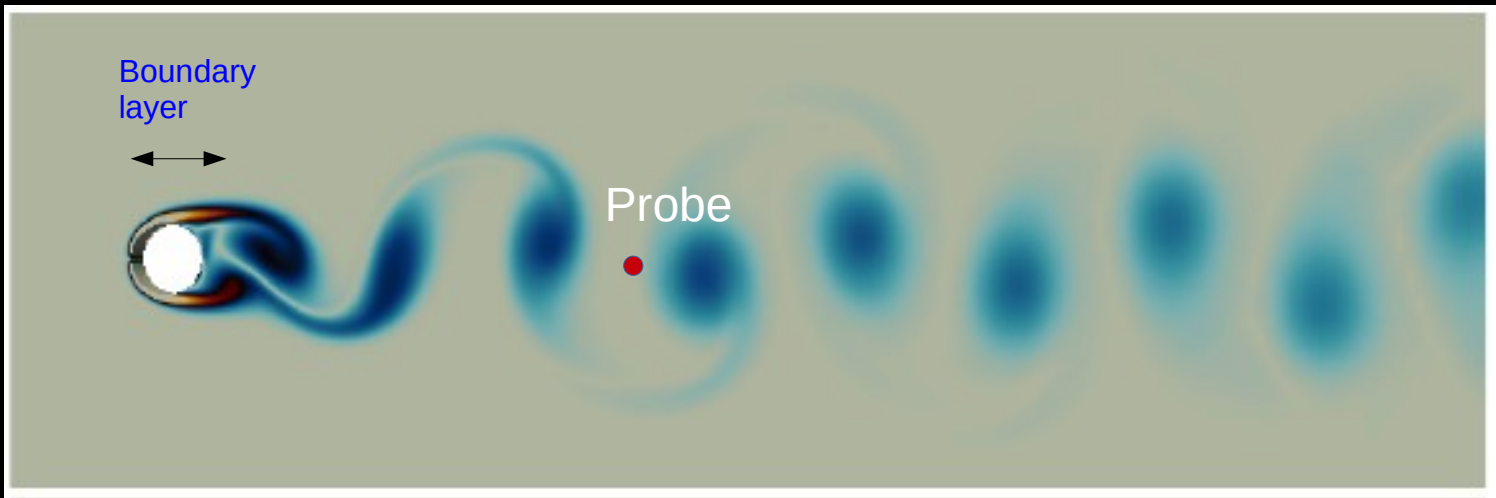
Probe



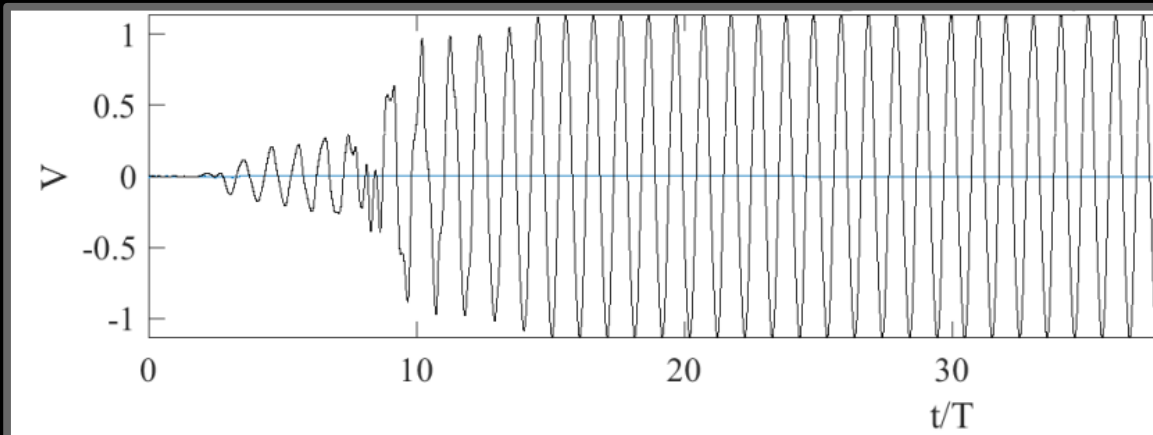
Typical scenario:

After initial transients flow enters a periodic shedding mode with a distinct frequency (Strouhal number) observed from the spanwise velocity component by downstream probing or lift-coefficient variation.

Flow over a cylinder



Probe



Very, very important in numerics to minimize numerical diffusion (but typically it is not possible to get fully rid of it). Pay attention to:

- Discretize convection term $\text{div}(\phi, \mathbf{U})$ preferably with "Gauss linear" (CD2)
- Second best option TVD/NVD limiter: e.g. GammaV 0.1
- Discretize time with "backward" (2nd order)

Turbulent flow

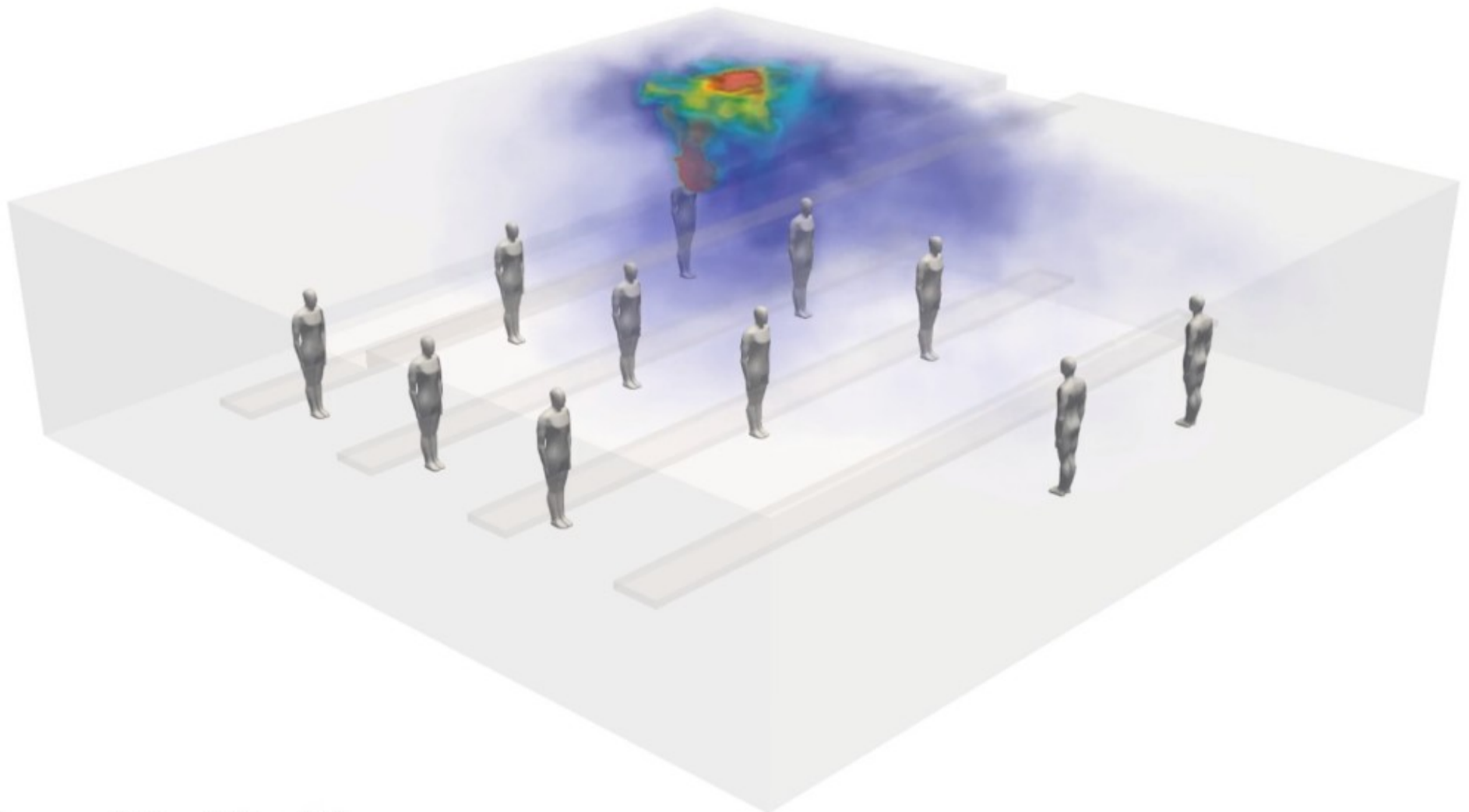
Insight to turbulent flow

- 1) CFD course: we directly solve Navier-Stokes eqn under laminar conditions
- 2) CFD course OpenFOAM solvers: directly applicable for turbulent flows as well under moderate Reynolds # (e.g. $Re < 5000$) without turbulence modeling on very fine grid resolution $\Delta x \approx \eta$. This is called: “**direct numerical simulation**” or “**DNS**”
- 3) In practice, for turbulent conditions, it is not feasible to refine the grid all the way to the smallest **Kolmogorov length scale** η (“eta”) where **kinetic energy dissipates to heat**. DNS is computationally expensive although possible.
- 4) In turbulent flow, energy flows from large scales to η . **Think:** pour milk to coffee and what happens? What is “large scale” and what are the “medium scales”?
- 5) In practice, for turbulent flows, in CFD we can “afford” to resolve until $\Delta x > \eta$. Turbulence modeling needed to compensate the “missing” kinetic energy dissipation on scale Δx . Physics: there are “subgrid eddies” of size $< \Delta x$.
- 6) **Large-eddy simulation (LES turbulence model):** fine resolution CFD, only model the “subgrid” scales. Offers space-time dependent transient information.
- 7) **Reynolds averaged Navier-Stokes simulation (RANS turbulence model):** Offers time-averaged solution.

Large-eddy simulation of buoyant airflow in an airborne pathogen transmission scenario publication (Laitinen, Vuorinen et al. 2023)

<https://www.sciencedirect.com/science/article/pii/S0360132323004894>

https://www.youtube.com/watch?v=f7MLFW_QJLo

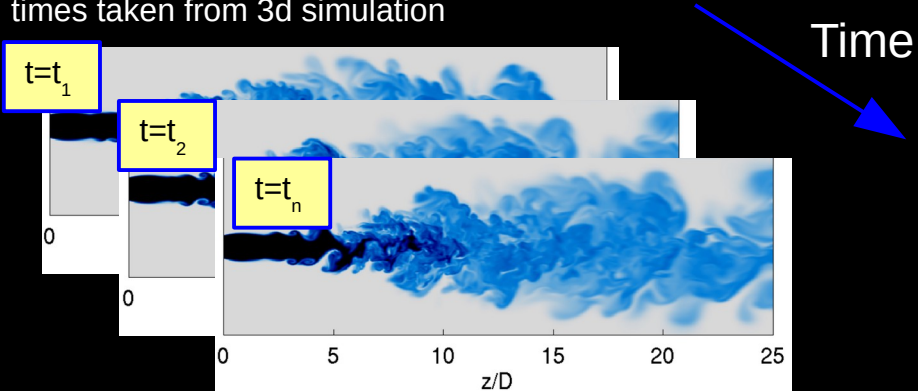


Time 00:02:41

Turbulent jets

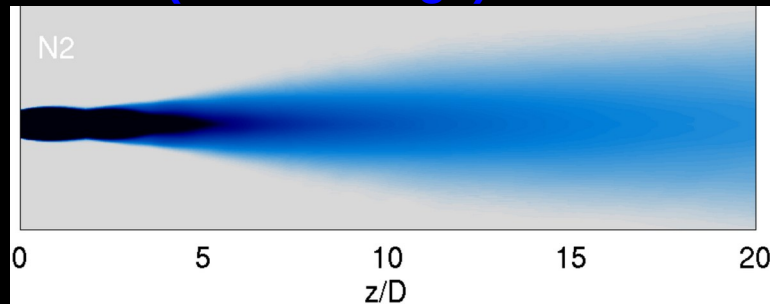
Below: we inject a concentration field in the jet flow to study mixing.

Example: 2d cutplanes from different times taken from 3d simulation



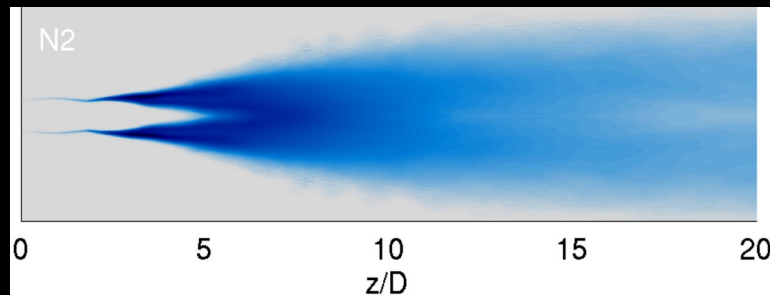
Here: passive scalar field averaged in time over several thousand cutplanes (time snapshots)

Mean (time average)



$$\langle P \rangle = \frac{1}{N} \sum_{i=1}^N P_i$$

Standard Deviation



$$\sigma_P = \frac{\sqrt{\sum_{i=1}^N (P_i - \langle P \rangle)^2}}{\sqrt{N}}$$

Turbulent channel flows

Here is a Matlab code to do turbulent channel flow. OpenFOAM also has respective channel flow case.
<https://www.sciencedirect.com/science/article/abs/pii/S0010465516300388>

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \nu \frac{\partial^2 u_i}{\partial x_j^2} + g_i$$

Domain size

$$2\pi \times 2 \times \pi$$

$$\frac{\partial u_i}{\partial x_i} = 0$$

Vuorinen et al., Com.in Comp.Physics (2016)

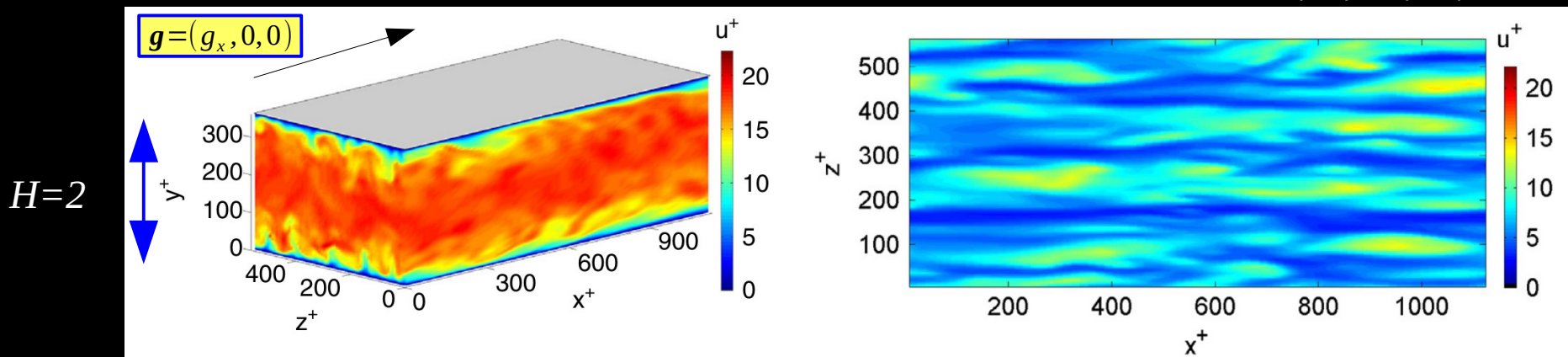


Fig. 5. Matlab simulations of instantaneous velocity in the channel (left), and visualization of the near-wall streaks at $y^+ \approx 10$ (right).

Note:

- Channel flows are very much studied configurations in understanding near-wall turbulence
- The “standard” for LES/DNS code benchmarking
- Steady flow maintained with the external force \mathbf{g}
- Periodic boundary conditions

Turbulent channel flows – Mean velocity profiles

