

SOLUTION 4

The required output power of the hydraulic motor

$$P_m = T_2 \cdot \omega_2 = T_2 \cdot 2 \cdot \pi \cdot n_2 = 300 \text{ Nm} \cdot 2 \cdot \pi \cdot 400/60 \text{ s} = 12.6 \text{ kW}$$

Due to losses, the input power to the motor has to be larger than the output power. From the input power, flow requirement can be calculated.

$$P_{m,\text{hydr}} = \frac{P_m}{\eta_{t2}} = \frac{12.6 \text{ kW}}{0.83} = 15.1 \text{ kW}$$

$$P_{m,\text{hydr}} = \Delta p \cdot q_{v,m}$$

$$\Rightarrow q_{v,m} = \frac{P_{m,\text{hydr}}}{\Delta p} = \frac{15.1 \text{ kW}}{14 \cdot 10^6 \text{ Pa}} = 1.08 \cdot 10^{-3} \text{ m}^3/\text{s} \quad (= 64.91/\text{min})$$

With non-ideal pump, its output flow is lesser than with ideal one; which is expressed with volumetric efficiency factor η_v .

$$q_{v,p} = \eta_v \cdot V_g \cdot n_1 = \eta_v \cdot V_{\text{rad}} \cdot \omega_1$$

The inlet flow to the hydraulic motor is equal to pump's outlet flow

$$q_{v,p} = q_{v,m}$$

$$\Rightarrow V_g = \frac{q_{v,p}}{\eta_v \cdot n_1} = \frac{1.08 \cdot 10^{-3} \text{ m}^3/\text{s}}{0.95 \cdot 1000/60 \text{ s}} = 68.3 \cdot 10^{-6} \frac{\text{m}^3}{\text{r}} = 68.3 \frac{\text{cm}^3}{\text{r}}$$

Pump's hydraulic power (outlet power)

$$P_1 = q_{v,p} \cdot \Delta p = 1.08 \cdot 10^{-3} \cdot 14 \cdot 10^6 = 15 \text{ kW}$$

Which can be seen being equal to (calculated above) motors inlet power (Pipes assumed to be lossless)

Pumps mechanical inlet power (electric motors output power)

$$P_{\text{pm}} = \frac{P_{m,\text{hydr}}}{\eta_{t1}} = \frac{15.1 \text{ kW}}{0.82} = 18.4 \text{ kW}$$

SOLUTION 5

a) Flow requirement to cylinder $q_{v,s}$

$$q_{v,s} = \frac{v \cdot A_1}{\eta_{v,s}} = \frac{0.02 \cdot 20 \cdot 10^{-4}}{1} = 40 \cdot 10^{-6} \frac{\text{m}^3}{\text{s}}$$

Flow produced by pump $q_{v,p}$.

$$q_{v,p} = \varepsilon \cdot \omega \cdot V_{\text{rad,max}} \cdot \eta_{v,p} \Rightarrow \varepsilon = \frac{q_{v,p}}{\omega \cdot V_{\text{rad,max}} \cdot \eta_{v,p}}$$

Flows have to be equal $q_{v,p} = q_{v,s}$ (assuming that the pressure relief valve remains closed).

$$\Rightarrow \varepsilon = \frac{q_{v,s}}{\omega \cdot V_{\text{rad,max}} \cdot \eta_{v,p}} = \frac{40 \cdot 10^{-6}}{1460 \cdot \frac{2\pi}{60} \cdot 0.6 \cdot 10^{-6} \cdot 0.87} = 0.5$$

Pumps displacement has to be set to 50% of its maximum value.

b) Let's calculate the pressure in the piston side chamber of cylinder while assuming the pressure in rod side chamber being zero.

$$p_p = \frac{F}{A_1 \cdot \eta_{hm,s}} = \frac{18600}{20 \cdot 10^{-4} \cdot 0.93} = 10 \text{ MPa}$$

Calculating the driving torque of the pump T_p

$$T_p = p_p \cdot \frac{\varepsilon \cdot V_{\text{rad,max}}}{\eta_{hm,p}} = 10 \cdot 10^6 \cdot \frac{0.5 \cdot 0.6 \cdot 10^{-6}}{0.94} = 3.2 \text{ Nm}$$

The power required to drive the pump P_{in}

$$P_{in} = T_p \cdot \omega = 3.2 \cdot 1460 \cdot \frac{2\pi}{60} = 489 \text{ W}$$

Mechanical output power of cylinder P_{out}

$$P_{out} = F \cdot v = 18600 \cdot 0.02 = 372 \text{ W}$$

Overall system efficiency η_t

$$\eta_t = \frac{P_{out}}{P_{in}} = \frac{372}{489} = 0.76$$

SOLUTION 6

a) Magnet a is energized

$$\begin{aligned} q_{V3} &= v \cdot A_3 \\ q_{V,p} &= v \cdot A_1 \end{aligned} \Rightarrow q_{V3} = \frac{q_{V,p} \cdot A_3}{A_1} = \frac{421/\text{min} \cdot 25 \text{ cm}^2}{31.2 \text{ cm}^2} = 33.71/\text{min}$$

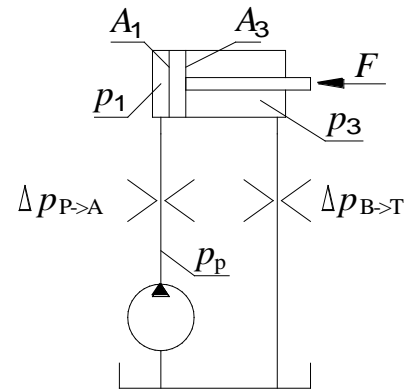
The pressure losses in both control edges (from chart)

$$\begin{aligned} q_{V3} = 33.71/\text{min} &\Rightarrow \Delta p_{B \rightarrow T} \approx 4 \text{ bar} \\ q_{V,p} = 421/\text{min} &\Rightarrow \Delta p_{P \rightarrow A} \approx 8 \text{ bar} \end{aligned}$$

Resolving p_1 (from force balance equation)

$$\begin{aligned} p_1 \cdot A_1 - p_3 \cdot A_3 &= F \\ p_1 &= \frac{p_3 \cdot A_3 + F}{A_1} \\ p_1 &= \frac{30 \text{ kN} + 4 \cdot 10^5 \text{ N/m}^2 \cdot 25 \cdot 10^{-4} \text{ m}^2}{31.2 \cdot 10^{-4} \text{ m}^2} = 9.9 \text{ MPa} \end{aligned}$$

$$p_p = p_1 + \Delta p_{P \rightarrow A} = 9.9 \text{ MPa} + 0.8 \text{ MPa} = 10.7 \text{ MPa}$$



b)

$$\begin{aligned} q_{V,p} &= v \cdot A_3 \\ q_{V1} &= v \cdot A_1 \end{aligned} \Rightarrow q_{V1} = \frac{q_{V,p} \cdot A_1}{A_3} = \frac{421/\text{min} \cdot 31.2 \text{ cm}^2}{25 \text{ cm}^2} = 52.41/\text{min}$$

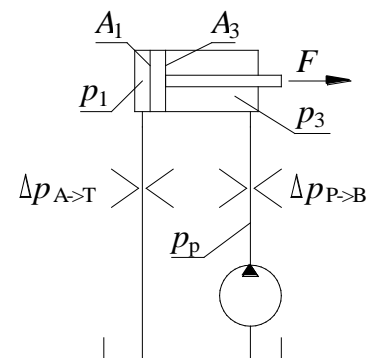
The pressure losses (from chart)

$$\begin{aligned} q_{V1} = 52.41/\text{min} &\Rightarrow \Delta p_{A \rightarrow T} \approx 10 \text{ bar} \\ q_{V,p} = 421/\text{min} &\Rightarrow \Delta p_{P \rightarrow B} \approx 8 \text{ bar} \end{aligned}$$

Resolving p_3 (from force balance equation)

$$\begin{aligned} p_3 &= \frac{F + p_1 \cdot A_1}{A_3} \\ p_3 &= \frac{30 \text{ kN} + 10 \cdot 10^5 \text{ N/m}^2 \cdot 31.2 \cdot 10^{-4} \text{ m}^2}{25 \cdot 10^{-4} \text{ m}^2} = 13.2 \text{ MPa} \end{aligned}$$

$$p_p = p_3 + \Delta p_{P \rightarrow B} = 13.2 \text{ MPa} + 0.8 \text{ MPa} = 14 \text{ MPa}$$



Additional information 2:

Sometimes flow loss curves are not given, but only a flow rate value with a given pressure loss. In such cases, the losses with any other given flow rate can be estimated as in the following example.

EXAMPLE ASSIGNMENT

Let's assume that pressure loss-curves are not available. The pressure loss (P→B) with flow of $q_V = 40$ l/min is known to be $\Delta p = 4$ bar. Calculate the pressure loss, when the flow is $q_V = 30$ l/min and the opening of the valve (and therefore the flow cross section area) remains constant.

SOLUTION

Flow through a turbulent choke (as in the case of a flow control valve) is

$$q_V = C_q \cdot A \cdot \sqrt{\frac{2 \cdot \Delta p}{\rho}}$$

where

C_q = flow coefficient (depends on flow velocity and of the geometry of the choke orifice)

$$A = \pi \cdot d \cdot h$$

h = opening of the slide

d = diameter of the slide

Δp = pressure difference over a control edge

ρ = density of the fluid

Using previous

$$\frac{q_{V1}}{q_{V2}} = \frac{C_q \cdot A_1 \cdot \sqrt{\frac{2 \cdot \Delta p_1}{\rho}}}{C_q \cdot A_2 \cdot \sqrt{\frac{2 \cdot \Delta p_2}{\rho}}} = \frac{\sqrt{\Delta p_1}}{\sqrt{\Delta p_2}} \quad \text{when } A_1 = A_2 \text{ ja } \rho = \text{constant}$$

$$\Rightarrow \Delta p_2 = \Delta p_1 \cdot \left(\frac{q_{V2}}{q_{V1}} \right)^2 = 4 \text{ bar} \cdot \left(\frac{30 \text{ l/min}}{40 \text{ l/min}} \right)^2 = 2.25 \text{ bar}$$

This derived equation can be found in the equation collection-document.