## SOLUTION 4

The required output power of the hydraulic motor

$$
P_{\mathrm{m}}=T_{2} \cdot \omega_{2}=T_{2} \cdot 2 \cdot \pi \cdot n_{2}=300 \mathrm{Nm} \cdot 2 \cdot \pi \cdot 400 / 60 \mathrm{~s}=12.6 \mathrm{~kW}
$$

Due to losses, the input power to the motor has to be larger than the output power. From the input power, flow requirement can be calculated.

$$
\begin{aligned}
& P_{\mathrm{m}, \mathrm{hydr}}=\frac{P_{\mathrm{m}}}{\eta_{t 2}}=\frac{12.6 \mathrm{~kW}}{0.83}=15.1 \mathrm{~kW} \\
& P_{\mathrm{m}, \mathrm{hydr}}=\Delta p \cdot q_{\mathrm{v}, \mathrm{~m}} \\
\Rightarrow & q_{\mathrm{V}, \mathrm{~m}}=\frac{P_{\mathrm{m}, \mathrm{hydr}}}{\Delta p}=\frac{15.1 \mathrm{~kW}}{14 \cdot 10^{6} \mathrm{~Pa}}=1.08 \cdot 10^{-3} \mathrm{~m}^{3} / \mathrm{s} \quad(=64.91 / \mathrm{min})
\end{aligned}
$$

With non-ideal pump, its output flow is lesser than with ideal one; which is expressed with volumetric efficiency factor $\eta_{\mathrm{v}}$.

$$
q_{\mathrm{v}, \mathrm{p}}=\eta_{\mathrm{v}} \cdot V_{\mathrm{g}} \cdot n_{1}=\eta_{\mathrm{v}} \cdot V_{\mathrm{rad}} \cdot \omega_{1}
$$

The inlet flow to the hydraulic motor is equal to pump's outlet flow

$$
\begin{aligned}
& q_{\mathrm{V}, \mathrm{p}}=q_{\mathrm{v}, \mathrm{~m}} \\
\Rightarrow \quad & V_{\mathrm{g}}=\frac{q_{\mathrm{v}, \mathrm{p}}}{\eta_{\mathrm{v}} \cdot n_{1}}=\frac{1.08 \cdot 10^{-3} \mathrm{~m}^{3} / \mathrm{s}}{0.95 \cdot 1000 / 60 \mathrm{~s}}=68.3 \cdot 10^{-6} \frac{\mathrm{~m}^{3}}{\mathrm{r}}=68.3 \frac{\mathrm{~cm}^{3}}{\mathrm{r}}
\end{aligned}
$$

Pump's hydraulic power (outlet power)

$$
P_{1}=q_{\mathrm{V}, \mathrm{p}} \cdot \Delta p=1.08 \cdot 10^{-3} \cdot 14 \cdot 10^{6}=15 \mathrm{~kW}
$$

Which can be seen being equal to (calculated above) motors inlet power (Pipes assumed to be lossless)

Pumps mechanical inlet power (electric motors output power)

$$
P_{\mathrm{pm}}=\frac{P_{\mathrm{m}, \mathrm{hydr}}}{\eta_{t 1}}=\frac{15.1 \mathrm{~kW}}{0.82}=18.4 \mathrm{~kW}
$$

## SOLUTION 5

a) Flow requirement to cylinder $q_{\mathrm{V}, \mathrm{s}}$

$$
q_{\mathrm{v}, \mathrm{~s}}=\frac{v \cdot A_{1}}{\eta_{\mathrm{v}, \mathrm{~s}}}=\frac{0.02 \cdot 20 \cdot 10^{-4}}{1}=40 \cdot 10^{-6} \frac{\mathrm{~m}^{3}}{\mathrm{~s}}
$$

Flow produced by pump $q_{\mathrm{v}, \mathrm{p}}$.
$q_{\mathrm{V}, \mathrm{p}}=\varepsilon \cdot \omega \cdot V_{\mathrm{rad}, \text { max }} \cdot \eta_{\mathrm{v}, \mathrm{p}} \Rightarrow \varepsilon=\frac{q_{\mathrm{V}, \mathrm{p}}}{\omega \cdot V_{\mathrm{rad}, \text { max }} \cdot \eta_{\mathrm{v}, \mathrm{p}}}$
Flows have to be equal $q_{\mathrm{V}, \mathrm{p}}=q_{\mathrm{V}, \mathrm{s}}$ (assuming that the pressure relief valve remains closed).
$\Rightarrow \varepsilon=\frac{q_{\mathrm{V}, \mathrm{s}}}{\omega \cdot V_{\mathrm{rad}, \text { max }} \cdot \eta_{\mathrm{v}, \mathrm{p}}}=\frac{40 \cdot 10^{-6}}{1460 \cdot \frac{2 \pi}{60} \cdot 0.6 \cdot 10^{-6} \cdot 0.87}=0.5$
Pumps displacement has to be set to $50 \%$ of its maximum value.
b) Let's calculate the pressure in the piston side chamber of cylinder while assuming the pressure in rod side chamber being zero.

$$
p_{\mathrm{P}}=\frac{F}{A_{1} \cdot \eta_{\mathrm{hm}, \mathrm{~s}}}=\frac{18600}{20 \cdot 10^{-4} \cdot 0.93}=10 \mathrm{MPa}
$$

Calculating the driving torque of the pump $T_{\mathrm{P}}$

$$
T_{\mathrm{P}}=p_{\mathrm{P}} \cdot \frac{\varepsilon \cdot V_{\mathrm{rad}, \text { max }}}{\eta_{\mathrm{hm}, \mathrm{p}}}=10 \cdot 10^{6} \cdot \frac{0.5 \cdot 0.6 \cdot 10^{-6}}{0.94}=3.2 \mathrm{Nm}
$$

The power required to drive the pump $P_{\text {in }}$
$P_{\mathrm{in}}=T_{\mathrm{P}} \cdot \omega=3.2 \cdot 1460 \cdot \frac{2 \pi}{60}=489 \mathrm{~W}$
Mechanical output power of cylinder $P_{\text {out }}$

$$
P_{\text {out }}=F \cdot v=18600 \cdot 0.02=372 \mathrm{~W}
$$

Overall system efficiency $\eta_{t}$
$\eta_{t}=\frac{P_{\text {out }}}{P_{\text {in }}}=\frac{372}{489}=0.76$

## SOLUTION 6

a) Magnet a is energized

$$
\begin{aligned}
& q_{V 3}=v \cdot A_{3} \\
& q_{\mathrm{V}, \mathrm{p}}=v \cdot A_{1}
\end{aligned} \quad \Rightarrow q_{V 3}=\frac{q_{\mathrm{V}, \mathrm{p}} \cdot A_{3}}{A_{1}}=\frac{421 / \mathrm{min} \cdot 25 \mathrm{~cm}^{2}}{31.2 \mathrm{~cm}^{2}}=33.71 / \mathrm{min}
$$

The pressure losses in both control edges (from chart)

$$
\begin{array}{ll}
q_{V 3}=33.71 / \mathrm{min} & \Rightarrow \Delta p_{\mathrm{B} \rightarrow \mathrm{~T}} \approx 4 \mathrm{bar} \\
q_{\mathrm{V}, \mathrm{p}}=421 / \mathrm{min} & \Rightarrow \Delta p_{\mathrm{P} \rightarrow \mathrm{~A}} \approx 8 \mathrm{bar}
\end{array}
$$

Resolving $p_{1}$ (from force balance equation)

$$
\begin{aligned}
& p_{1} \cdot A_{1}-p_{3} \cdot A_{3}=F \\
& p_{1}=\frac{p_{3} \cdot A_{3}+F}{A_{1}} \\
& p_{1}=\frac{30 \mathrm{kN}+4 \cdot 10^{5} \mathrm{~N} / \mathrm{m}^{2} \cdot 25 \cdot 10^{-4} \mathrm{~m}^{2}}{31.2 \cdot 10^{-4} \mathrm{~m}^{2}}=9.9 \mathrm{MPa} \\
& p_{\mathrm{p}}=p_{1}+\Delta p_{\mathrm{P} \rightarrow \mathrm{~A}}=9.9 \mathrm{MPa}+0.8 \mathrm{MPa}=10.7 \mathrm{MPa}
\end{aligned}
$$

b)

$$
\begin{aligned}
& q_{\mathrm{V}, \mathrm{p}}=v \cdot A_{3} \\
& q_{V 1}=v \cdot A_{1}
\end{aligned} \quad \Rightarrow q_{V 1}=\frac{q_{\mathrm{v}, \mathrm{p}} \cdot A_{1}}{A_{3}}=\frac{421 / \mathrm{min} \cdot 31.2 \mathrm{~cm}^{2}}{25 \mathrm{~cm}^{2}}=52.41 / \mathrm{min}
$$

The pressure losses (from chart)

$$
\begin{array}{ll}
q_{V 1}=52.41 / \mathrm{min} & \Rightarrow \Delta p_{\mathrm{A} \rightarrow \mathrm{~T}} \approx 10 \mathrm{bar} \\
q_{\mathrm{V}, \mathrm{p}}=421 / \mathrm{min} & \Rightarrow \Delta p_{\mathrm{P} \rightarrow \mathrm{~B}} \approx 8 \mathrm{bar}
\end{array}
$$

Resolving $p_{3}$ (from force balance equation)

$$
\begin{aligned}
& p_{3}=\frac{F+p_{1} \cdot A_{1}}{A_{3}} \\
& p_{3}=\frac{30 \mathrm{kN}+10 \cdot 10^{5} \mathrm{~N} / \mathrm{m}^{2} \cdot 31.2 \cdot 10^{-4} \mathrm{~m}^{2}}{25 \cdot 10^{-4} \mathrm{~m}^{2}}=13.2 \mathrm{MPa}
\end{aligned}
$$



$$
p_{\mathrm{p}}=p_{3}+\Delta p_{\mathrm{P} \rightarrow \mathrm{~B}}=13.2 \mathrm{MPa}+0.8 \mathrm{MPa}=14 \mathrm{MPa}
$$

## Additional information 1:

Should all the losses in the transfer line be included, one method for solving the pumps output ports pressure would is to:

Solve volume flows in pipes
Find out the (inside) diameters of pipes


Calculate the flow velocities in the pipes
$\downarrow$


Find out loss coefficients
of pipe bendings (see literature)

$$
\begin{aligned}
\Delta p_{\text {bend }}= & \xi_{90^{\circ}} \cdot \frac{\rho \cdot v^{2}}{2} \\
& \downarrow
\end{aligned}
$$

Calculate losses in each bending Calculate $R e$ at each pipe

Find out the surface roughness of the pipes $\downarrow$
Find out friction factor $\lambda$, e.g. Moody's chart $\downarrow$

$$
\begin{gathered}
\Delta p_{\mathrm{pipe}}=\lambda \cdot \frac{l}{d} \cdot \frac{\rho \cdot v^{2}}{2} \\
\downarrow
\end{gathered}
$$

## Calculate pressure loss at each pipe

Sum the pressure losses starting from tank and return line and ending to the rod side chamber of the cylinder
$\downarrow$
$\Delta p_{\text {IT }}+\Delta p_{\text {bends }, 4}+\Delta p_{\mathrm{B} \rightarrow \mathrm{T}}+\Delta p_{\mathrm{IB}}+\Delta p_{\text {bends }, 2}$


Resolve the pressure in the piston side chamber of the cylinder by using the force equilibrium equation of the cylinder $\downarrow$
To this value add the remaining pressure losses between the piston side chamber and pump output port (pipe bendings, valve, pipes)

$$
\begin{gathered}
\downarrow \\
\Delta p_{\mathrm{IA}}+\Delta p_{\mathrm{bends}, 66} \\
\downarrow
\end{gathered}
$$

The pressure at the pump outlet port $p_{p}$ is resolved!

## Additional information 2:

Sometimes flow loss curves are not given, but only a flow rate value with a given pressure loss. In such cases, the losses with any other given flow rate can be estimated as in the following example.

## EXAMPLE ASSIGNMENT

Let's assume that pressure loss-curves are not available. The pressure loss $(\mathrm{P} \rightarrow \mathrm{B})$ with flow of $q_{\mathrm{V}}=40 \mathrm{l} / \mathrm{min}$ is known to be $\Delta p=4$ bar. Calculate the pressure loss, when the flow is $q_{\mathrm{v}}=30 \mathrm{l} / \mathrm{min}$ and the opening of the valve (and therefore the flow cross section area) remains constant.

## SOLUTION

Flow through a turbulent choke (as in the case of a flow control valve) is

$$
q_{\mathrm{v}}=C_{\mathrm{q}} \cdot A \cdot \sqrt{\frac{2 \cdot \Delta p}{\rho}}
$$

where
$C_{\mathrm{q}}=$ flow coefficient ( depends on flow velocity and of the geometry of the choke orifice)
$A=\pi \cdot d \cdot h$
$h=$ opening of the slide
$d=$ diameter of the slide
$\Delta p=$ pressure difference over a control edge
$\rho=$ density of the fluid

Using previous

$$
\begin{aligned}
& \frac{q_{V 1}}{q_{V 2}}= \\
& C_{q} \cdot A_{1} \cdot \sqrt{\frac{2 \cdot \Delta p_{1}}{\rho}} \\
& C_{q} \cdot A_{2} \cdot \sqrt{\frac{2 \cdot \Delta p_{2}}{\rho}}=\frac{\sqrt{\Delta p_{1}}}{\sqrt{\Delta p_{2}}} \text { when } A_{1}=A_{2} \text { ja } \rho=\mathrm{constant} \\
& \Rightarrow \Delta p_{2}=\Delta p_{1} \cdot\left(\frac{q_{V 2}}{q_{V 1}}\right)^{2}=4 \mathrm{bar} \cdot\left(\frac{301 / \mathrm{min}}{401 / \mathrm{min}}\right)^{2}=2.25 \mathrm{bar}
\end{aligned}
$$

